



Photoelectrocatalytic Treatment and By-Product Formantion

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Istanbul University at a Glance

The Oldest University of Turkiye (Established in 145

Academics

Faculties: 20

Schools: 3

Vocational Higher Schools: 6

**Students:** 

Associate Degree: 9000 Students

Undergraduate: 65000 Students

Graduate: 14500 Students Total: 88500 Students

Nobel Prizes: (Orhan Pamuk)

1 Nobel Prize in Literature

Campuses:

12 Campuses

# Coloboration with Industry

- ENTA Treatment Coop.(SMEs), Istanbul
- Sunholding Research Center Inc. (Textile) Izmir.
- Yunsa Inc. (Textile Industry) Cerkezkoy, Istanbul
- Akin Textile Inc. Luleburgaz
- TISAN Inc. Izmir. <a href="www.tisan.net">www.tisan.net</a>, the garbage container Truck" (SMEs)
- GUMUSSU Treatment Camp. (Denizli, Turkiye)
- Karboy Textile, Kahramanmaras, Turkiye
- 5 Other Textile Industries



#### Organization

http://rr.istanbul.edu.tr/



Homepage

Main Topics

Committees

Keynote Speakers

Important Dates

Instructions NEW

Conference Programme NEW

Registration UPDATE

Submission

Venue UPDATE

Accommodation

Sponsore



Dear Colleagues,

After a great success of the first conference which brought together over 200 of the world's leading thinkers and practitioners from science, policy and enterprise communities, we are pleased to inform you that the 2nd "International Conference on Recycling and Reuse, 2014" (R&R, 2014) will be organized in 4-6 June 2014 in Istanbul, Turkiye.

The purpose of the conference is to provide an excellent platform for researchers and



### International Projects

**TUBITAK** "Deposition of TiO<sub>2</sub> ve Metal Doped TiO<sub>2</sub> Nanoparticles for the self-cleaning and antibacterial cotton textile; Funded by TUBITAK 260.000\$

**LEONARDO DA VINCI,** Community Vocational Training Action Program, WASTE TRAIN: Vocational Training, Education, Conveying Information on up to data Waste Management Practices Makers/Staff Involved Waste Management. *Partner 550.000* €

MIUR Italy Collobration Project, -Evaluation of Advanced Oxidation Processes for Wastewater Treatment and Disinfection, and Reuse. MRCR Project (Italy, Greece, Turkey, Morocco), *Partner 80.000* €

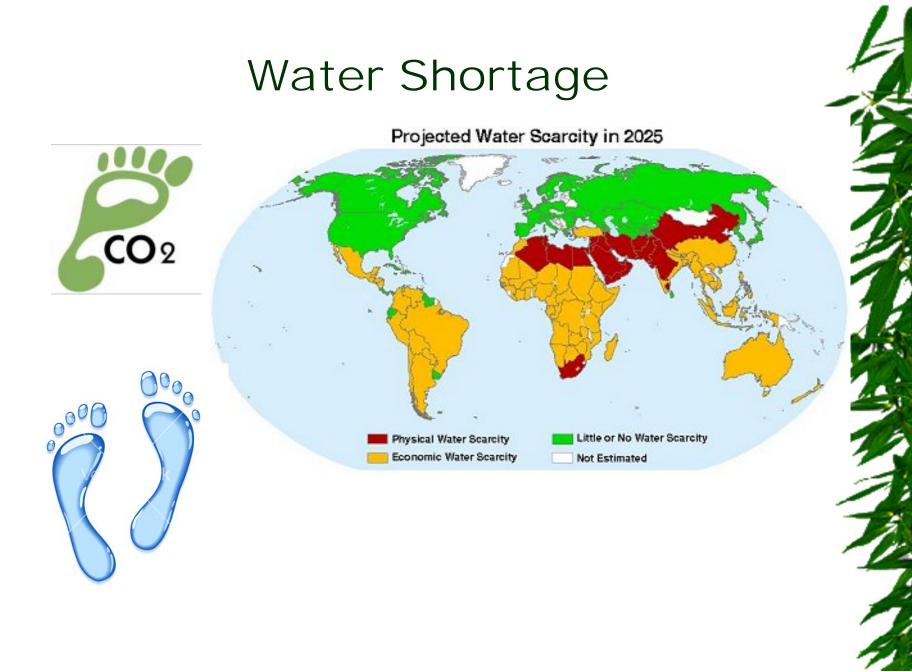
*NATO Collaborative Linkage Grant*, (€ 15.400, # EST.CLG.980506), "Evaluation of alternative water treatment systems for obtaining safe

drinking water in three countries"

Cost action, ICTAG C-075, "Environmental Pollution Effects and Best Available Integrated Technologies for Textile Industry Preparation," Dyeing and Finishing Process Chemicals", 80.000 \$

### Industrial Projects

- SERTAS Alaminium INC., EPA Treatment Company (SME), "Recovery of liquors and metals from Aluminum Industry for zero discharge".
- Sunholding Research Center Inc. Izmir. "Application of Advanced Oxidation and Membrane Separation Treatments for the Reuse of Salt and Textile Process Wastewater: 480.000\$.
- <u>Yunsa Textile Inc.</u> Cerkezkoy, Istanbul, "Development of Selfcleaning Properties on the wool textile" 84.000\$.
- Akin Textile Inc. Luleburgaz. "Integrated Membrane Treatment for treatment and reuse of the segregated dyeing and mercerizing process waters" 850.000\$.
- Gumussu Treatment Inc. (SME) "Integrated Membrane Treatment for the Advanced Treatment of the Biologically Treated Wastewaters and Reuse of Membrane Brine in Textile Processes" 240.000\$
- TISAN Inc. Izmir (SME) "Development of wastewater treatment and reuse system for the garbage container washing truck" 240.000\$.



New water resources: Polluted water and treated wastewaters

- Remaining refractory organics
- High TDS level is not suitable for potable, industrial and agricultural uses.
- Still not safe (due to the pathogens, micropollutans, many different toxic chemicals)
- Hazardous By-Products (Bromate, THM, HAAs.....)
- The cost of advanced treatment system is high

#### Solutions??

Today, it is critical:

to reduce salinity (Desalination)

to decrease refractory organic levels of waters/wastewaters (advanced treatment)

to reduce treatment cost

to develope energy free treatment and disinfection Tech. (Solar Systems)

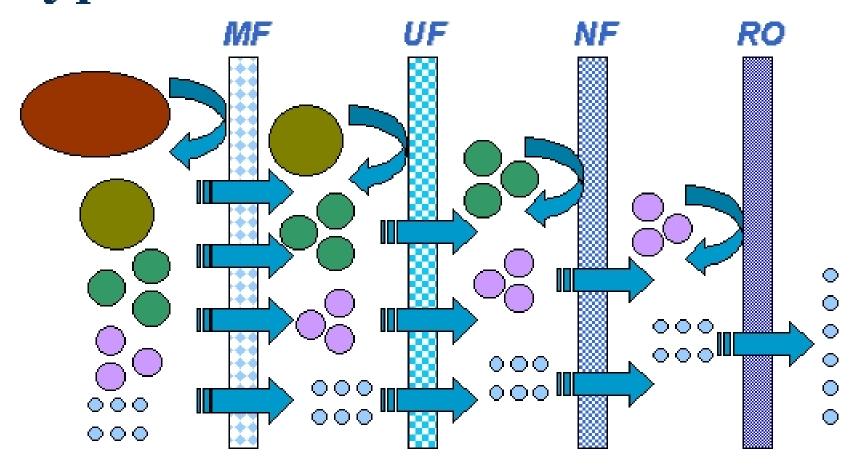


#### Desalination

- •Membrane Based Processes
- Solar Desalination Systems



#### Types of Membrane



- Suspended Solids 🔵 Multivalent Ions
- Macromolecules Monovalent lons Water

# Membrane processes for solution

- Solar desalination is expensive
- Membrane treatment is the applicable solution. But
  - High energy cost of membrane system
  - Membrane fauling problems
  - Membrane brine



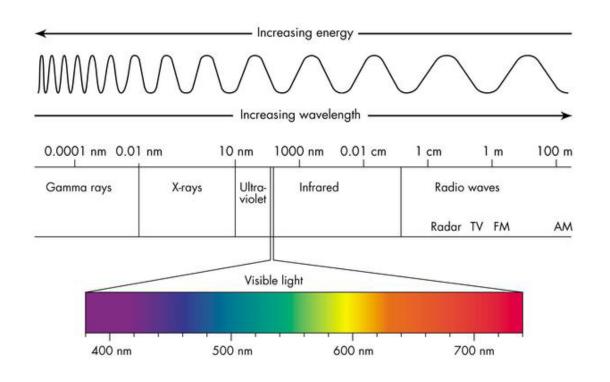
What should we do for an applicable UV/Solar system?

- 1. Enhancement of UV technologies
- 2. Development of efficient photocatalyst
- 3. Development of new photocatalytic systems



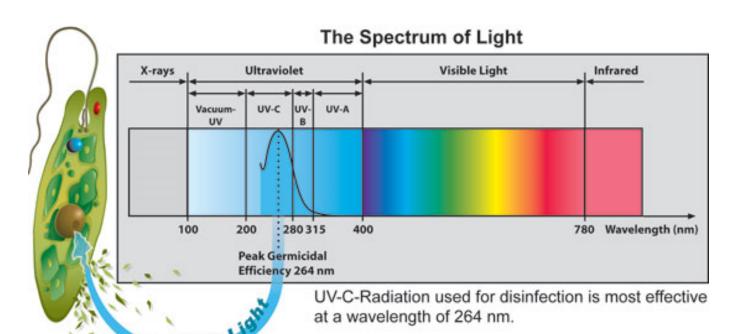
### 1. Enhancement of UV technologies

#### Wavelength-Photolysis





# Disinfection with photolysis





# LED UV disinfection and Treatment

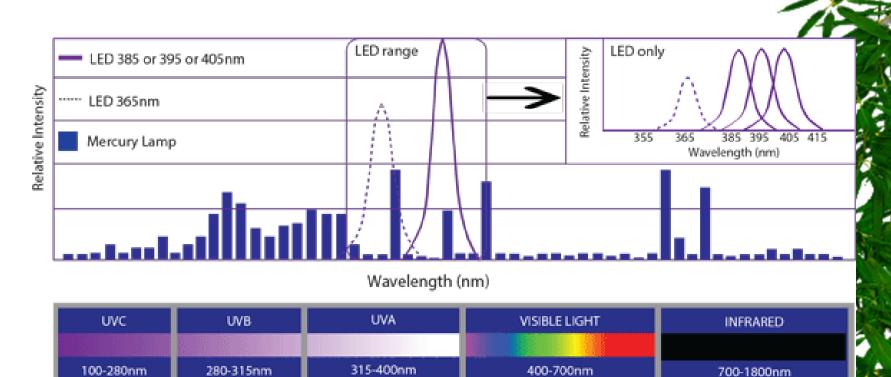
One important aspect is to have low-energy consuming systems. In that regard, the UV disinfection using LEDs (Light-Emitting Diode) seems a promising technology.

The market for water disinfection worldwide could be huge. LEDs are not yet competitive with legacy technologies, but there is hope that they could be within the decade

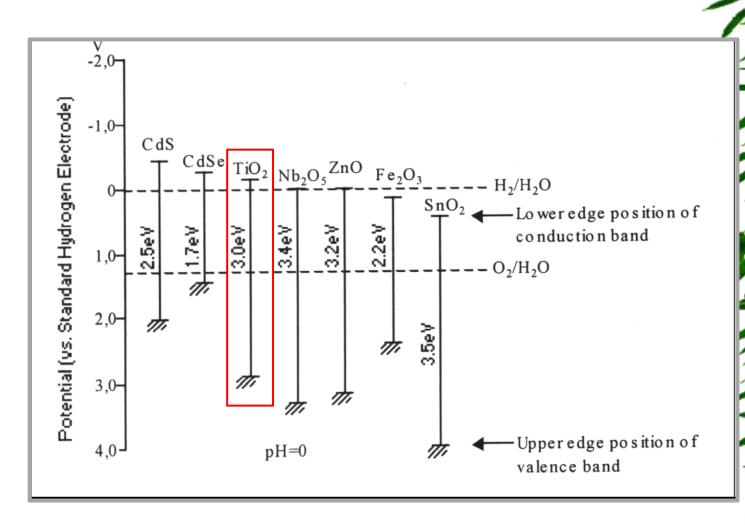
#### Basic advantages of LED Light

- Energy efficient LED's are now capable of outputting 135 lumens/watt
- Long Lifetime 50,000 hours or more if properly engineered
- No warm-up period LED's light instantly in nanoseconds
- Not affected by cold temperatures LED's "like" low temperatures and will startup even in subzero weather
- Directional With LED's you can direct the light where you want it, thus no light is wasted
- Environmentally friendly LED's contain no mercury or other hazardous substances

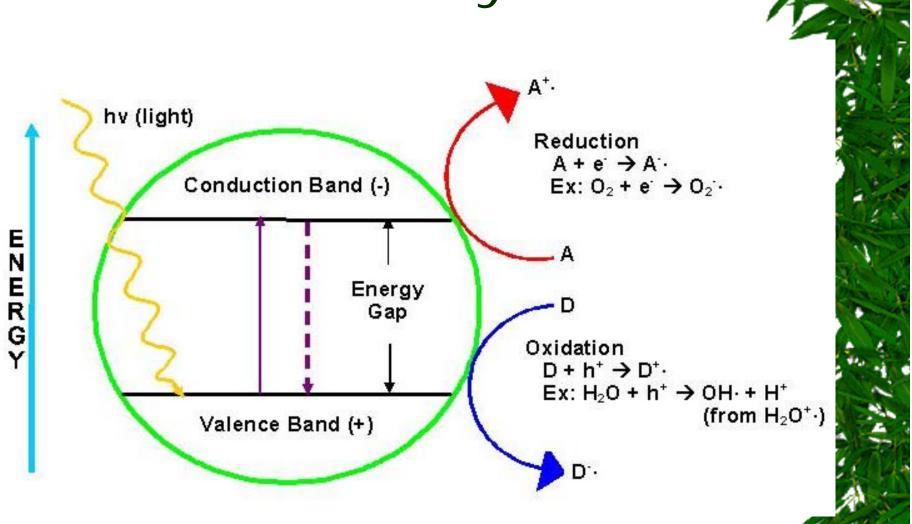
### UV light Tech.



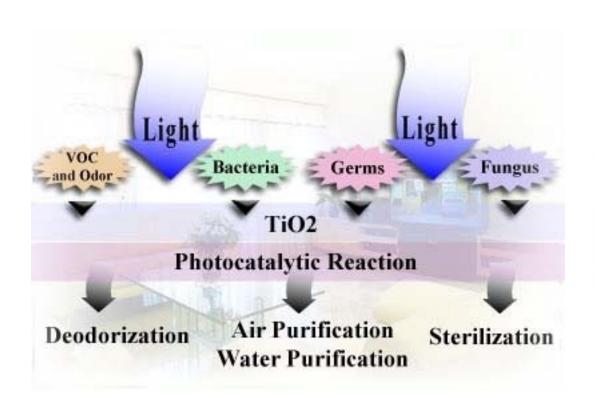
2. Development of efficient photocatalyst



### Photocatalysis



Photocatalysis can be used for?









# TiO<sub>2</sub> photocatalysis electon-hole reactions

$$rac{1}{2}$$
 TiO<sub>2</sub>(e<sup>-</sup> - h<sup>+</sup>)  $\rightarrow$  e<sup>-</sup> - h<sup>+</sup>

- e⁻ reactions;
  - $O_2 + e^- \rightarrow O_2^-$
  - $O_2 + 2e^- + 2H + \rightarrow H_2O_2$
  - $H_2O_2 + e^- \rightarrow HO^{\bullet} + OH^-$
  - $H_2O_2 + hv \rightarrow 2HO$ •
- - $H_2O + h^+ \rightarrow HO^{\bullet} + H^+$
  - $OH^- + h^+ \rightarrow HO^{\bullet}$



# Why solar treatment is not applicable??

- Low quantum efficiency
- Separation of NPs from solution is difficult
- Recombination of electron-hole pairs reduce photocatalytic efficiency
- Quenching of anode/cathode products decreases photocatalytic treatment.



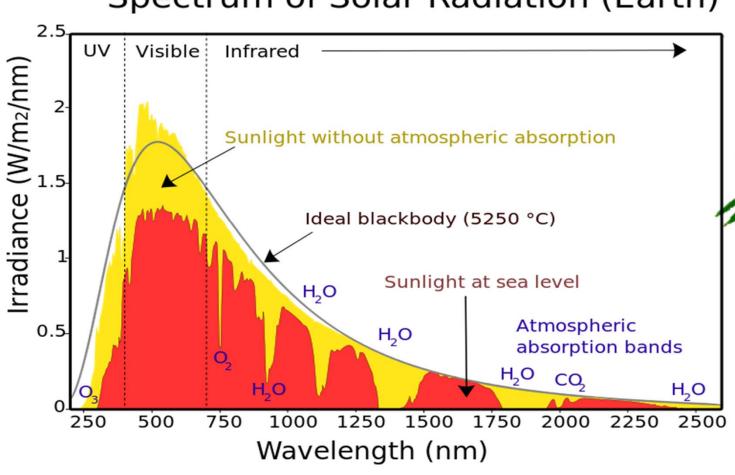
Lets do something but what?

- Shift wavelength from UV to visible
- Increase quantum efficiency (Develope more efficient catalyst)
- Immobilization of NPs
- Decrease recombination of electron-hole part (photoelectrocatalytic system)
- Decrease quenching of products (Seperation of hole-electron reactions, PEC cell)

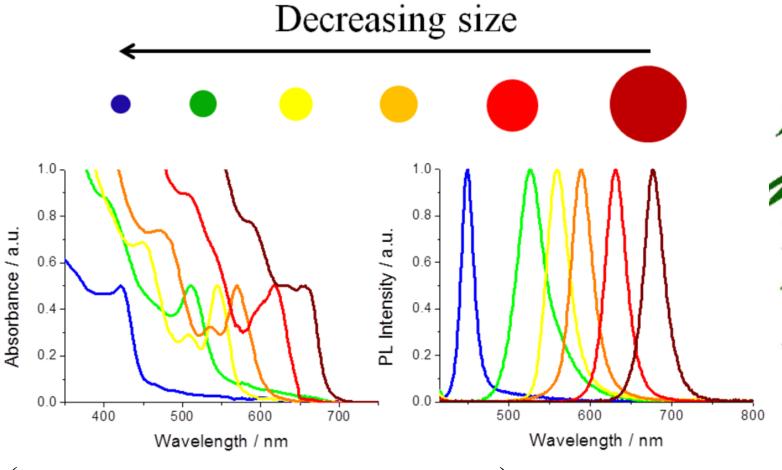


### Sunlight?

Spectrum of Solar Radiation (Earth)



Hybrid Catalysts: Absorption spectra of doped and differently sized nanocrystals (CdSe)



(Y. Yuan and M. Krüger *Polymers* **2012**, *4*(1), 1-19)

3. Development of new photocatalytic systems

Immobilization of semiconductor

Develope different reactor system

We are talking about

Photoelectrocatalytic (PEC) System



#### PEC process

PEC process that first time introduced in 1972 by Fujishima and Honda for splitting of water

In recent years, electron and hole reactions were separated in the PEC system for treatment of water (Vinodgopal et al., 1994; Selcuk et al., 2003). This provided great advantage for the disinfection and treatment of waters.

PEC is also known to be a combination of photocatalytic and electrochemical process.

In this system <u>insignificant</u> electrical potential is used to decrease hole-electron recombination in the bulk of photocatalyst.



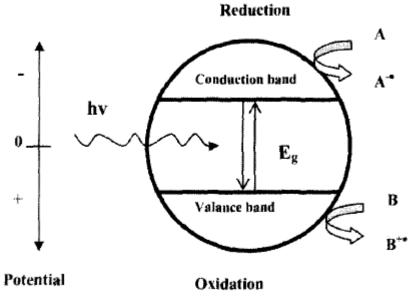


Fig. 1. Oxidation and reduction in the photocatalytic process (A, reducible and B, oxidizable species).

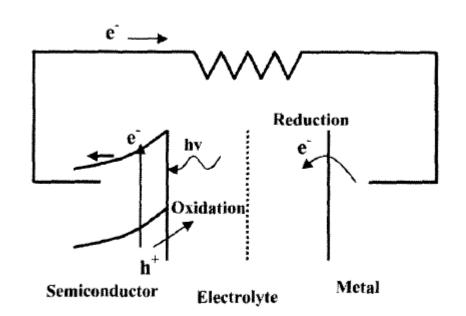


Fig. 2. Charge separation in the PEC system.



DESALINATION

Desalination 176 (2005) 219-227

www.elsevier.com/locate/desal

Effect of pH, charge separation and oxygen concentration in photoelectrocatalytic systems: active chlorine production and chlorate formation

Huseyin Selcuka\*, Marc A. Andersonb



#### PEC Reactor

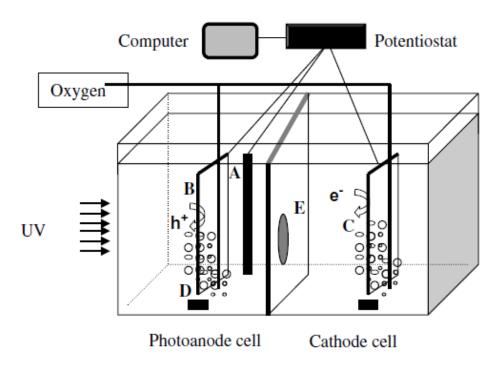


Fig. 1. Diagram for the reactor system for the photoelectrocatalytic reaction: (A) reference electrode (saturated calomel electrode); (B) photoanode TiO<sub>2</sub> coated electrode; (C) cathode electrode; (D) stirring bar; (E) Nafion 117 membrane.

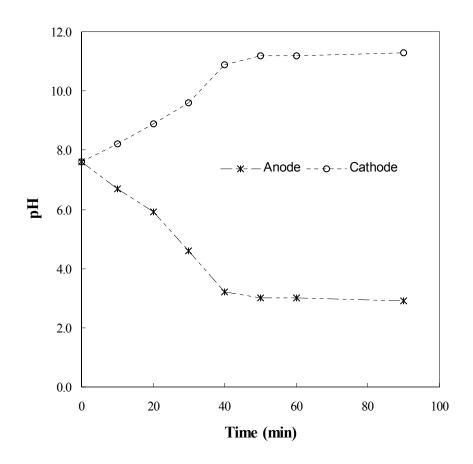


# TiO<sub>2</sub> photocatalysis electon-hole reactions

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  - $OH^- + h^+ \rightarrow HO^{\bullet}$







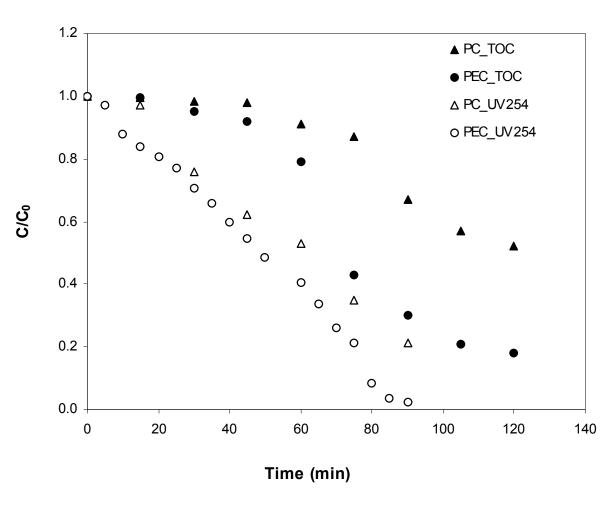
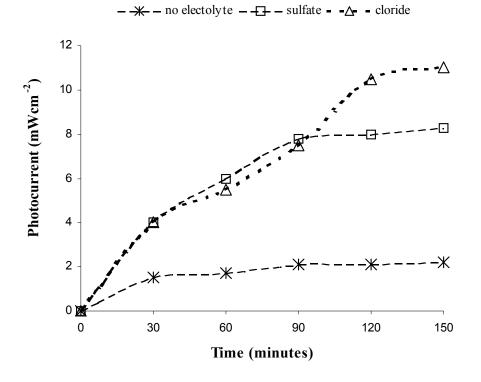


Figure: PEC and PC removal of 25 mgL<sup>-1</sup> HA in 1.25x10<sup>-2</sup> M NaCl solution using a titanium dioxide thin-film electrode.

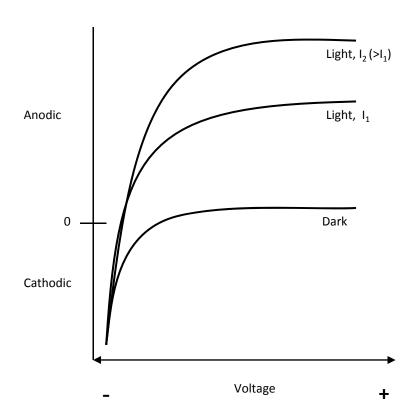
### Variables of PEC Treatment

#### Electrolyte



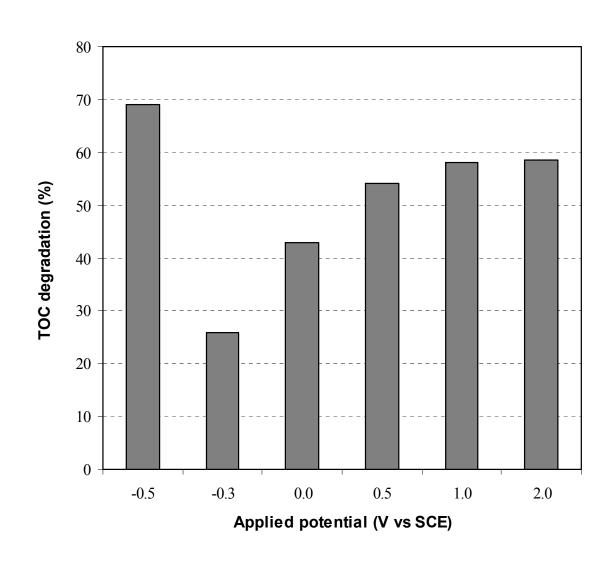


# Light intensity





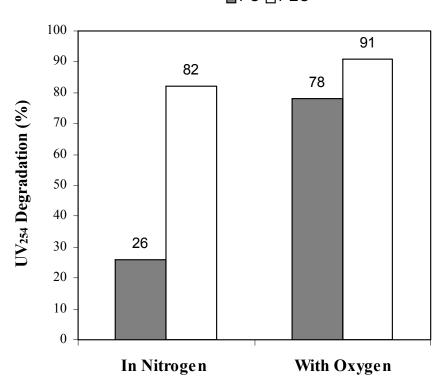
## Applied potential





# Oxygen

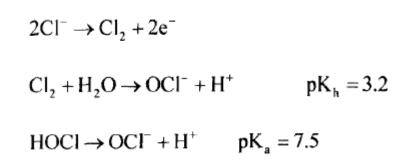


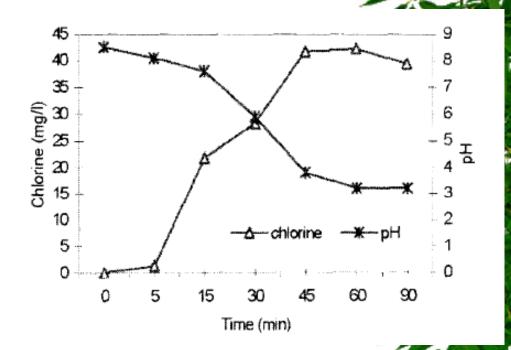




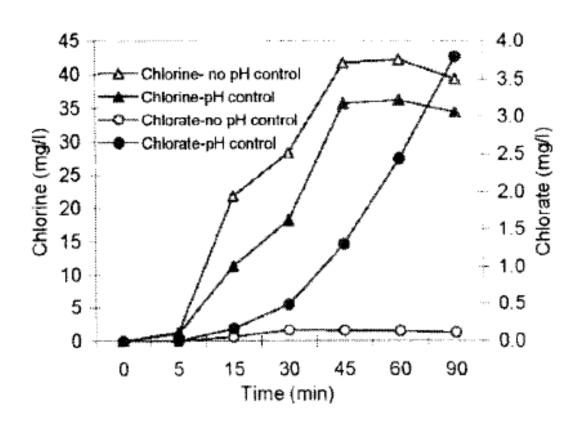
# Chlorine generation in a PEC system

Selcuk H. and Anderson M. Desalination 176 (2005) 219-227





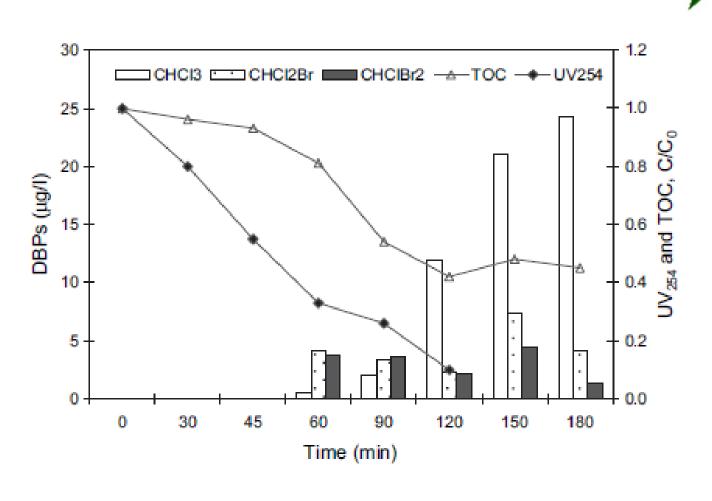
#### Chlorate Formation





#### Formation of THMs

Selcuk H., Water Research 44 (2010) 3966-3972



#### oxidation of halogens

$$2Br^- \rightarrow Br_2 + 2e^-_{CB}$$

$$Br_2 + H_2O \leftrightarrow HOBr + Br^- + H^+ \quad pK_h = 4.0$$

$$HOBr \leftrightarrow H^+ + BrO^- \quad pK_a = 8.8$$

$$Br_{aq}^- \leadsto (Br_{aq}^-)^* \to Br^{\scriptscriptstyle \bullet} + e_{aq}^-$$

$$2Br^{\scriptscriptstyle \bullet} \to Br_2$$

$$3BrO^- \rightarrow 2Br^- + BrO_3^-$$

$$BrO^- + 2HOBr \rightarrow H^+ + Br^- + BrO_3^-$$



### Ozone production-Formation of bromate

$$2OH_{ads} \rightarrow O_{ads} + H^+ + e^-$$

$$O_{ads} + O_2 \rightarrow O_3$$

$$O_3 + Br^- \rightarrow O_2 + BrO^ k = 160 \text{ M}^{-1} \text{ s}^{-1}$$

$$O_3 + BrO^- \rightarrow 2O_2 + Br^ k = 330 \text{ M}^{-1} \text{ s}^{-1}$$

$$O_3 + BrO^- \rightarrow BrO_2^- + O_2$$
  $k = 100 M^{-1} s^{-1}$ 

$$BrO_2^- + O_3 \rightarrow BrO_3^- + O_2$$
  $k > 10^5 M^{-1} s^{-1}$ 

$$^{\bullet}$$
OH + BrO $^{-}$  → BrO $^{\bullet}$  + OH $^{-}$   
 $k = 4.0 \times 10^{9} \text{ M}^{-1} \text{ s}^{-1}$ 

$$^{\bullet}$$
OH + HOBr → BrO $^{\bullet}$  + H<sub>2</sub>O  
 $k = 2.0 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ 

$$2\text{BrO}^{\bullet} + \text{H}_2\text{O} \rightarrow \text{BrO}_2^- + \text{OBr}^- + 2\text{H}^+$$
  
 $k = 4.9 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ 

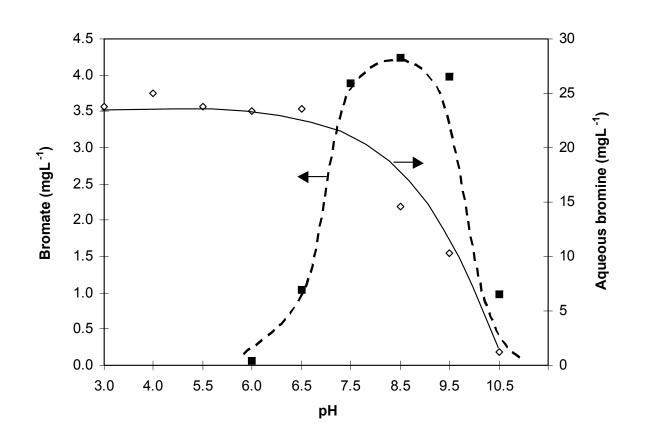
$$BrO_2^- + {}^{\bullet}OH \to BrO_2^{\bullet} + OH^-$$
  
 $k = 2.0 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ 

$$2BrO_{2^{\bullet}} \rightarrow Br_2O_4$$
  $k = 1.4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ 

$$Br_2O_4 + OH^- \rightarrow BrO_3^- + BrO_2^- + H^+$$
  
 $k = 7.0 \times 10^8 M^{-1} s^{-1}$ 

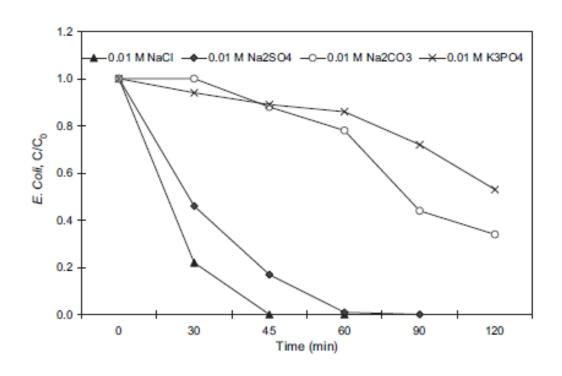


# Formation of bromate in a PEC system



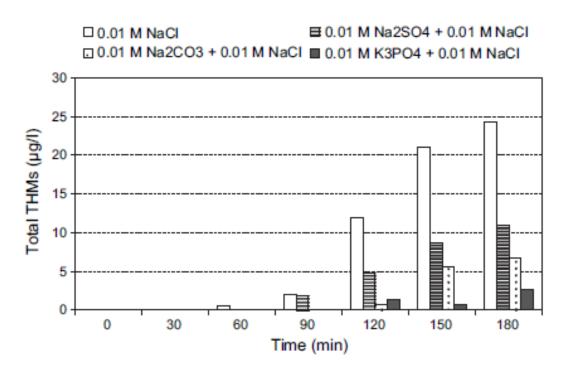


## Effect of scavengers





# Effects of radical scavancers





#### Conclusions

Anode peroducts	Cathode products
ozone	Hydrogen peroxide
Chlorine/chlorate/chlorinated organics	hydrogen
Bromine/bromate/brominated organics	
persulfate	

Possible Advanced oxidation		
Ozone+UV	H2O2+UV (OH radical generation)	
TiO2+UV		
persulfate+UV		

#### Problems

- Nanofilms is stable under UV illumination but not under high saline solutions
- Unit efficiency of the immobilized photocatalys is lower than slurry system
- Tech. Readiness level is still low (labscale)

