



Solar Photocatalytic Processes For Soil Washing Wastewater Treatment

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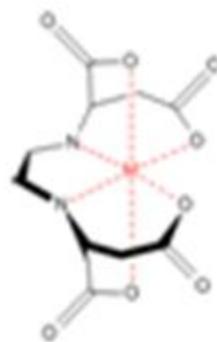
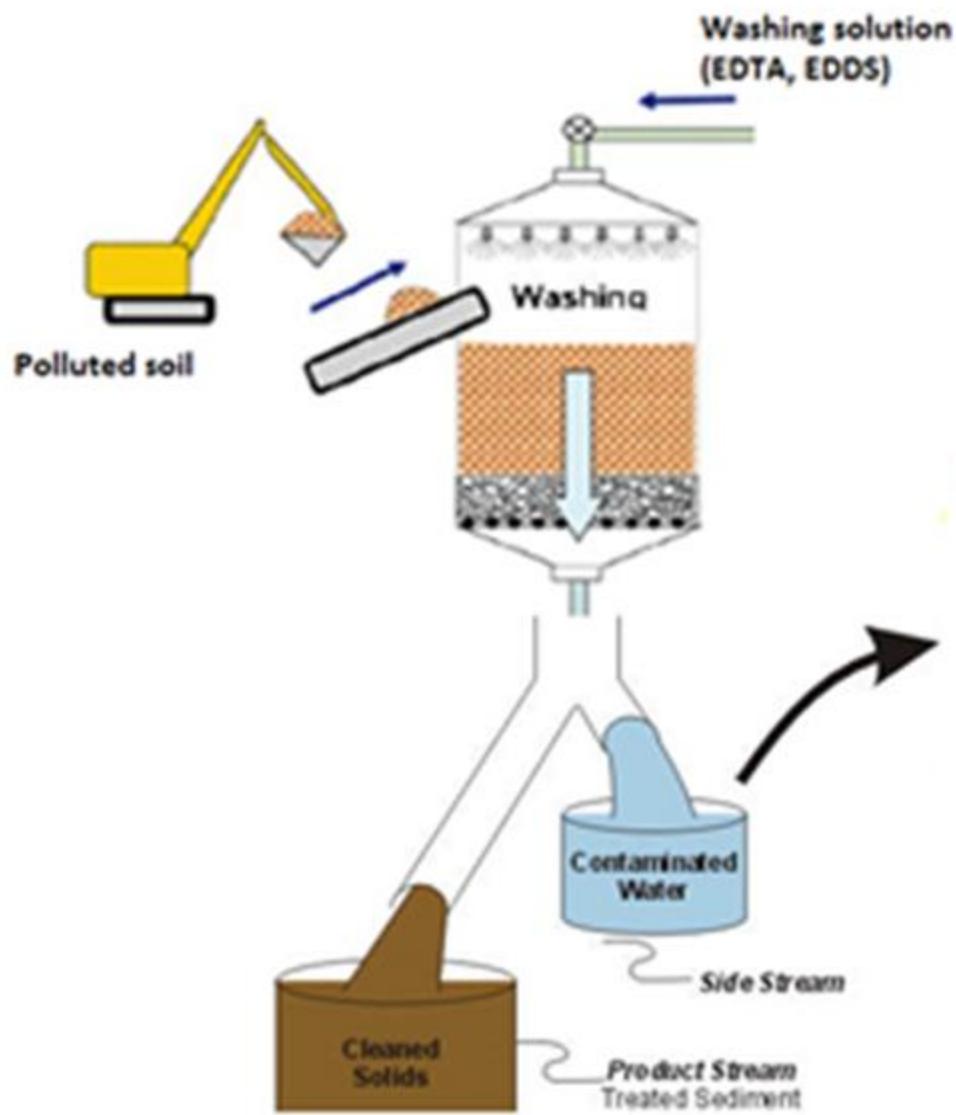
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Website 2: <http://scholar.google.it/citations?user=M3VH5ZMAAAJ&hl=it>

Soil washing procedure

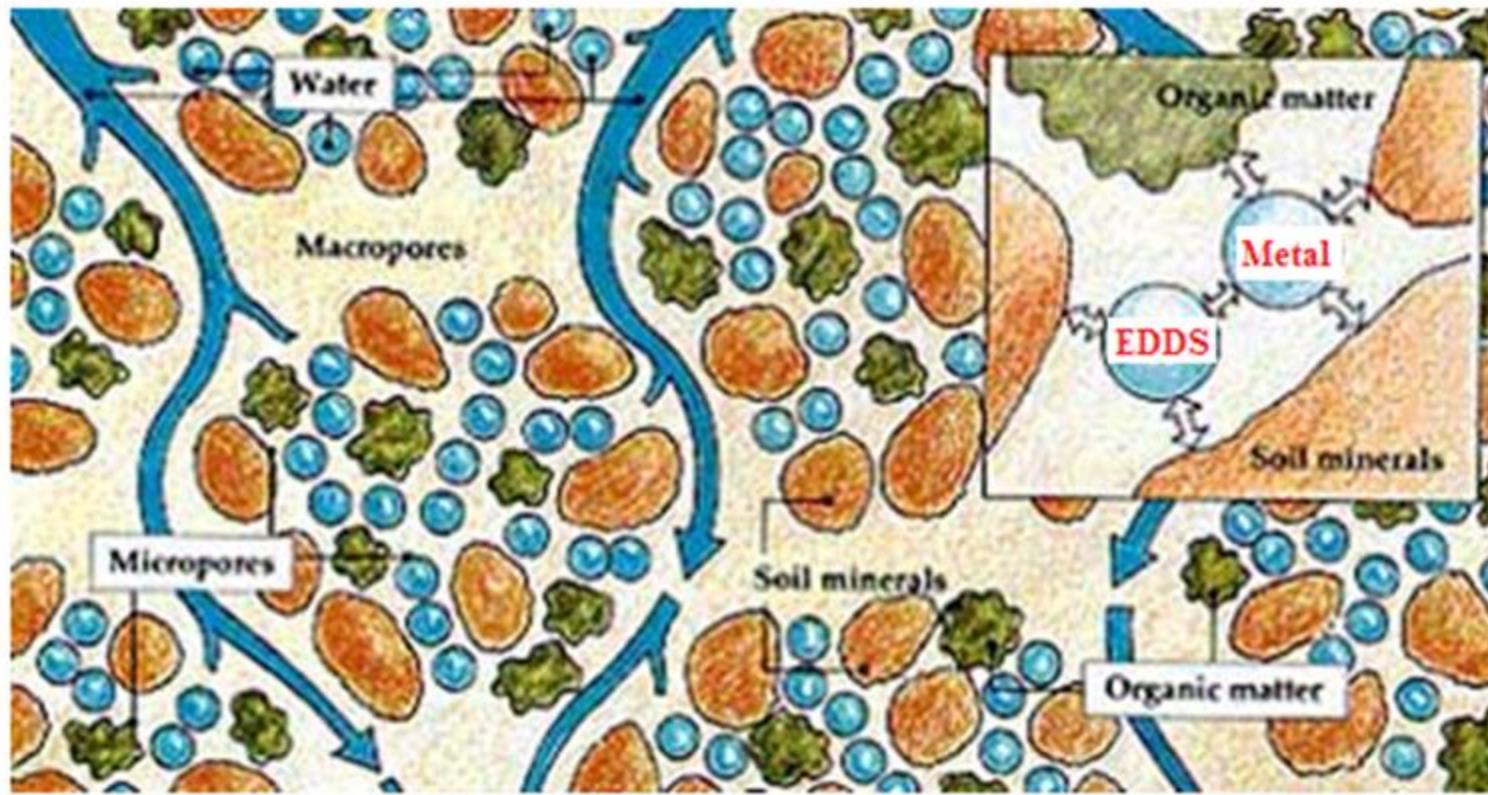
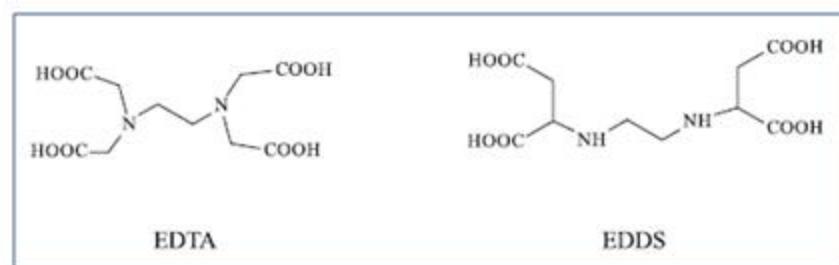
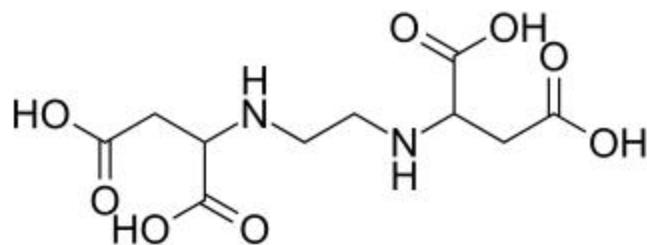


EDDS



Legal limits

Chelating agent: Ethylenediamine-*N,N'*-disuccinic acid (EDDS)

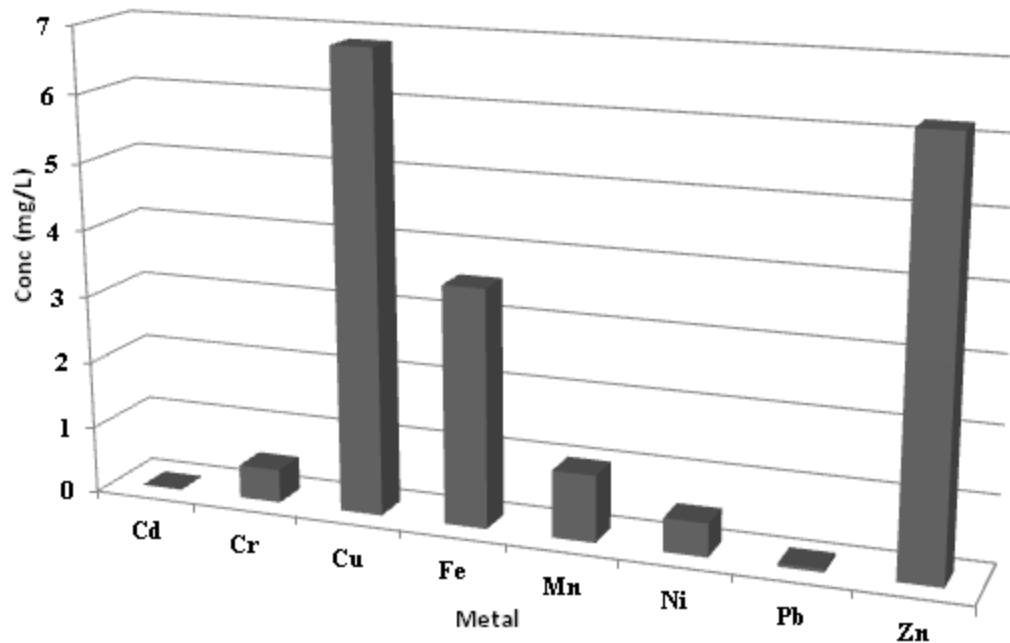


Soil sampling: Land of Fires



....where illegal dumping of toxic waste has been continuously perpetrated, for decades, by criminal organizations. This area is known due to the high incidence of cancer mortality, which exceeds both the Italian national and European average values

After the soil washing process, the effluent contains **heavy metals** and **chelating agents**



For example **copper** and **zinc**, extracted from soil, are at concentration levels higher than the Italian regulatory limits for discharge in public sewers and consequently one or more post-treatment processes are required, before the discharge into the environment.

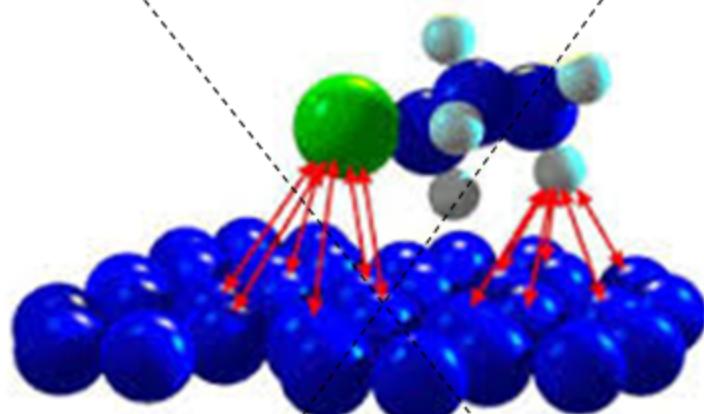
Limits for sewage discharge in Italy: Cu (0.4 ppm); Zn (1.0 ppm)

Treatment soil washing effluents step

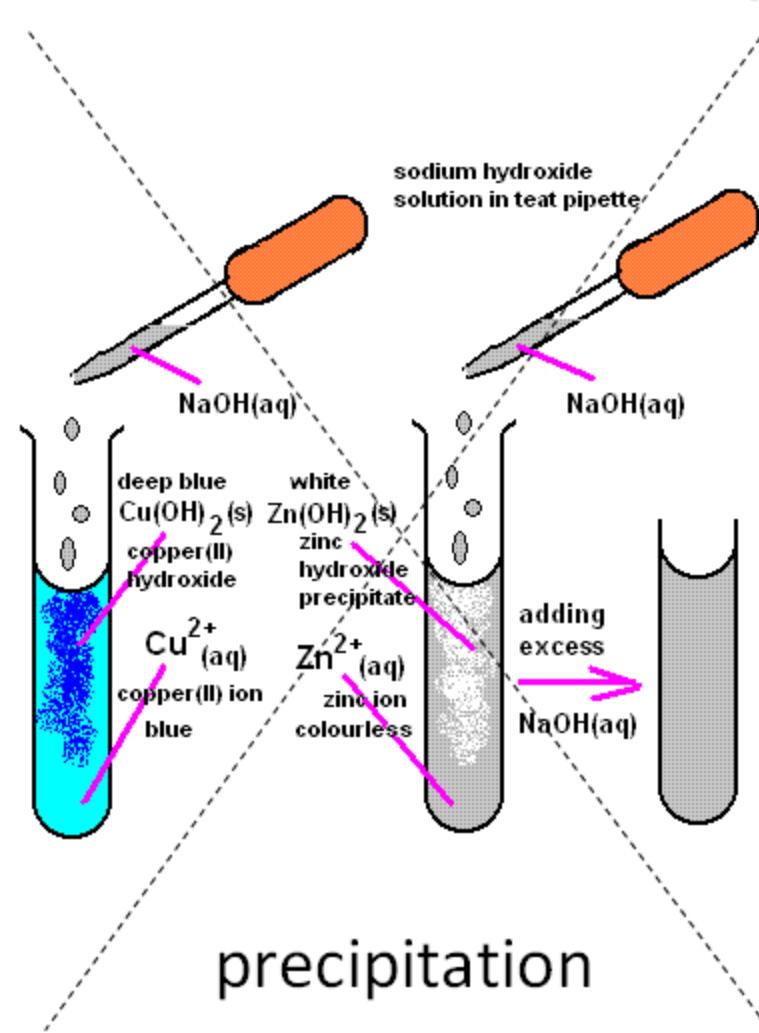
Due to the presence of metal-chelating agent chemical complexes.....

Cu(II)	Log K	Fe(III)	Log K
$Cu^{2+} + EDDS^{4-} \rightleftharpoons [CuEDDS]^{2-}$	18.6	$Fe^{3+} + EDDS^{4-} \rightleftharpoons [FeEDDS]^{-}$	20.6
$[CuEDDS]^{2-} + H^+ \rightleftharpoons [CuHEDDS]^{-}$	3.6	$[Fe(OH)EDDS]^{2-} + H^+ \rightleftharpoons [FeEDDS]^{-}$	7.9
$[CuHEDDS]^{-} + H^+ \rightleftharpoons CuH_2EDDS$	2.3	$[Fe(OH)_2EDDS]^{3-} \rightleftharpoons [Fe(OH)EDDS]^{2-} + HO^-$	9.9
$[Cu(OH)EDDS]^{3-} + H^+ \rightleftharpoons [CuEDDS]^{2-} + H_2O$	11.1		
$[CuEDDS]^{2-} + Cu^{2+} \rightleftharpoons Cu_2EDDS$	2.4		
$[CuEDDS]^{2-} + [HEDDS]^{3-} \rightleftharpoons [CuEDDS(HEDDS)]^{5-}$	2.5		
$[CuEDDS(HEDDS)]^{5-} + H^+ \rightleftharpoons [Cu(HEDDS)_2]^{4-}$	7.1		
Zn(II)	Log K	EDDS	pK _a
$Zn^{2+} + EDDS^{4-} \rightleftharpoons [ZnEDDS]^{2-}$	13.6	$H_4EDDS \rightleftharpoons H_3EDDS^- + H^+$	2.4
$[ZnEDDS]^{2-} + H^+ \rightleftharpoons [ZnHEDDS]^{-}$	3.7	$H_3EDDS^- \rightleftharpoons H_2EDDS^{2-} + H^+$	3.9
$[ZnHEDDS]^{-} + 2H^+ \rightleftharpoons [ZnH_2EDDS]^+$	5.9	$H_2EDDS^{2-} \rightleftharpoons HEDDS^{3-} + H^+$	6.8
$[Zn(OH)EDDS]^{3-} + H^+ \rightleftharpoons [ZnEDDS]^{2-} + H_2O$	11.3	$HEDDS^{3-} \rightleftharpoons EDDS^{4-} + H^+$	9.8
$[ZnHEDDS]^{-} + HEDDS^{3-} \rightleftharpoons [Zn(HEDDS)_2]^{4-}$	5.5		

....the simple physical process of adsorption on activated carbon or metal precipitation as hydroxides can not ensure a satisfactory removal of metals from soil washing wastewaters.



adsorption



Need to remove the chelating agent (i.e EDDS)



The soil washing effluent contains Iron too....

....Iron is naturally present in soils

Other “*ingredients*” economic and eco-friendly to be used are:

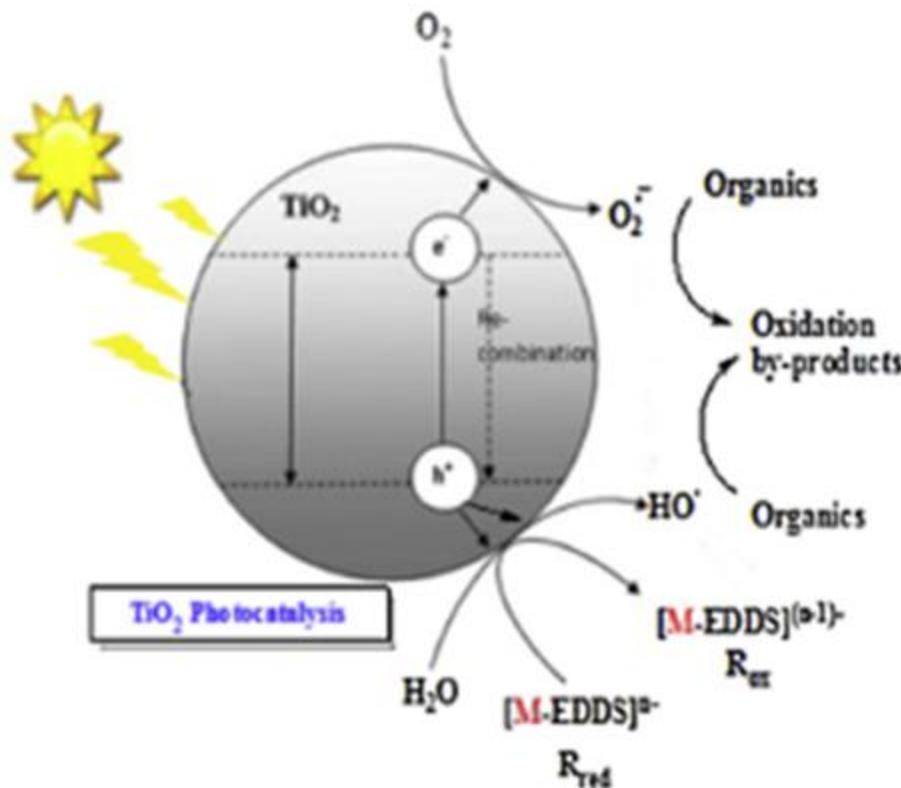
- 1) Sunlight
- 2) Air
- 3) Hydrogen peroxyde (*eventually*)
- 4) Titanium oxide

Different ways to proceed for removing of copper and zinc

Air/TiO₂:

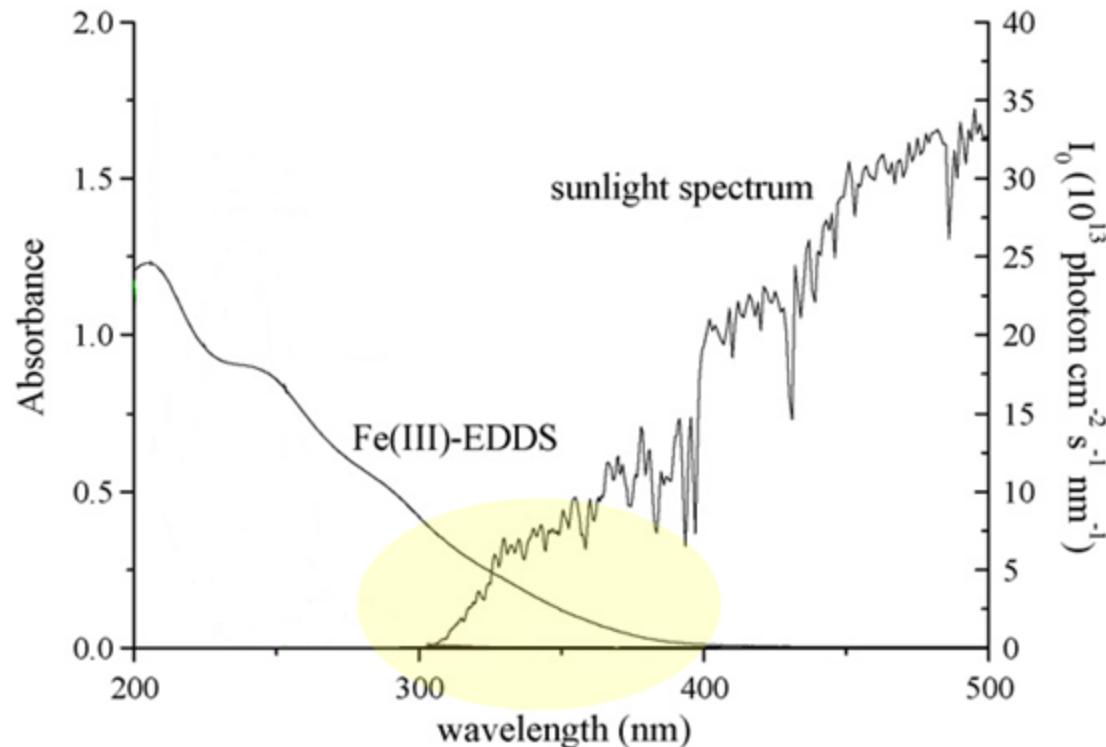
Heterogeneous photocatalytic process

- 1) Production of HO radicals which attack and destroy the chelating agent

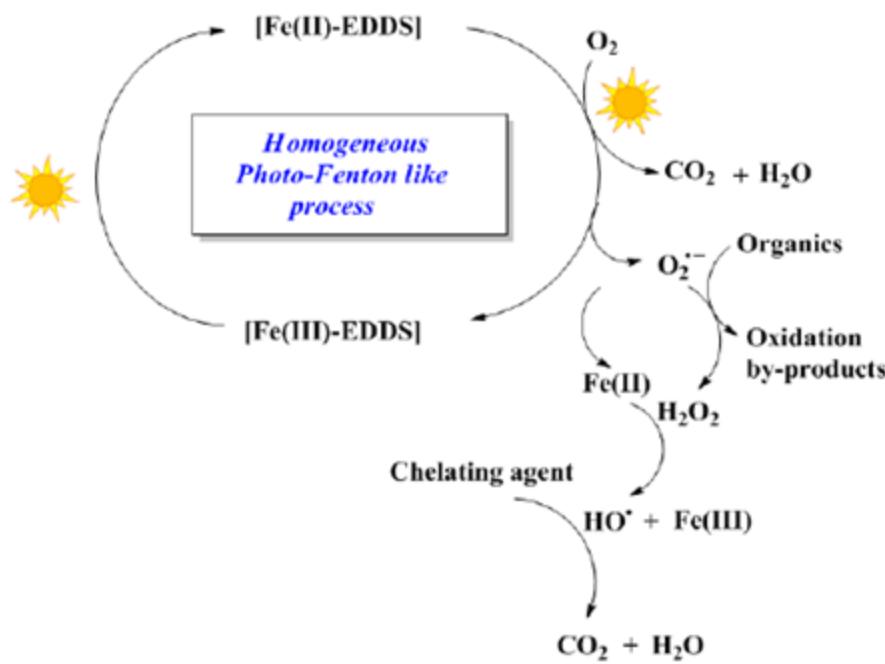


- 2) Some metals not longer complexed can precipitate as insoluble hydroxides

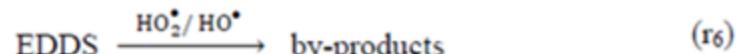
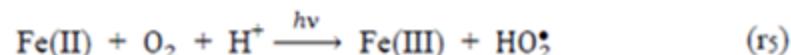
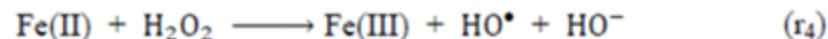
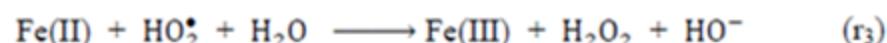
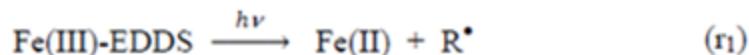
EDDS and its intermediate degradation products, form strong chelates with Fe(III). These species absorb in the UV-A range



Homogeneous photocatalytic process



The photolysis of Fe(III)-EDDS species through intramolecular LMCT (ligand to metal charge transfer) transitions occurs with good quantum yields

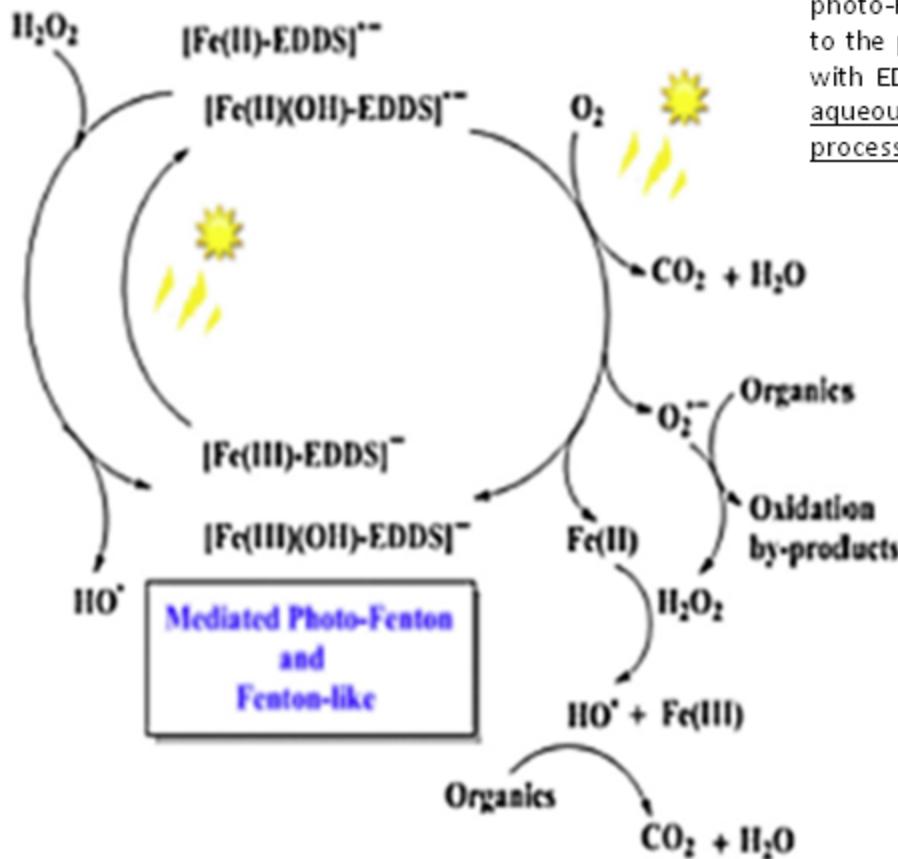


NO adding of chemicals!

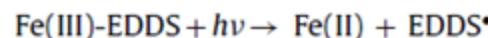
Oxidant species, such as HO^{\bullet} , $\text{O}_2^{\bullet\cdot}$, HO_2^{\bullet} and H_2O_2 , are formed during the photolysis of the iron(III)-EDDS complexes under aerated conditions

Homogeneous photocatalytic process

More expensive but...
more efficient

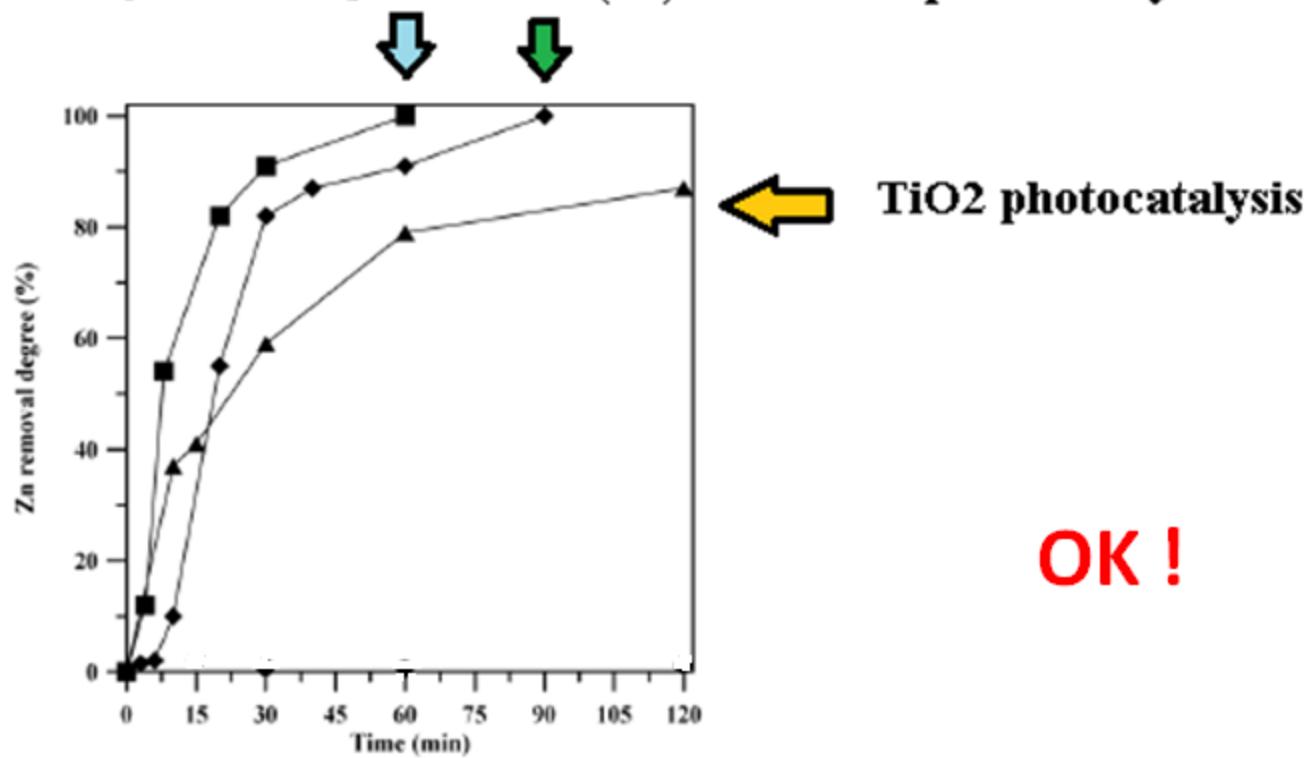


Difference with the “classic” photo-Fenton process: normally, the photo-Fenton reaction with $\text{Fe}(\text{III})$ is efficient in the pH range 2.0 – 4.0 due to the precipitation of iron at higher pH values. Whereas the complexation with EDDS produces a double effect by increasing the stability of iron in aqueous solution at higher pH and increasing the efficiency of the Fenton process by formation of hydroperoxyl/superoxide radicals:



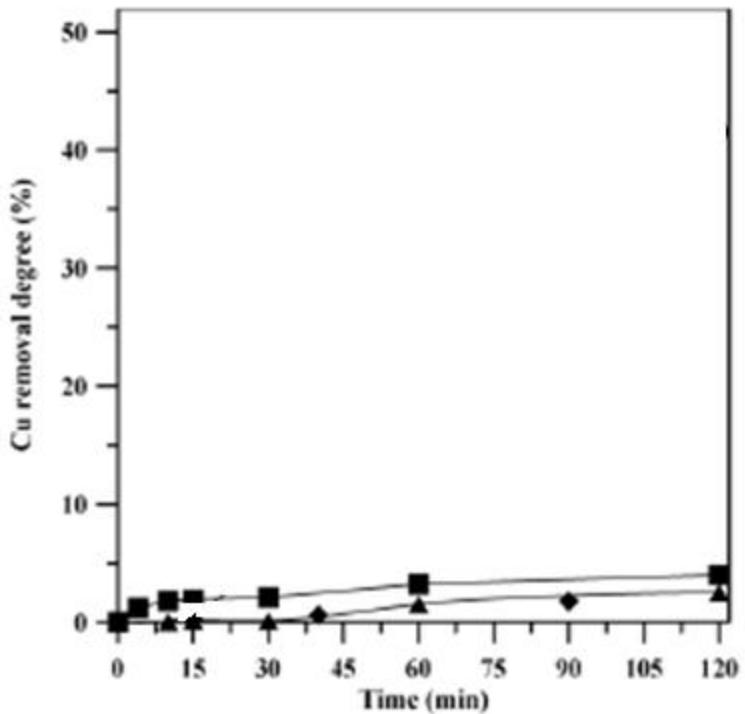
For Zinc

Fe(III)-EDDS/H₂O₂ photocatalysis Fe(III)-EDDS/Air photocatalysis



But for copper.....

However, the previous photocatalytic processes are not all effective in removing copper species

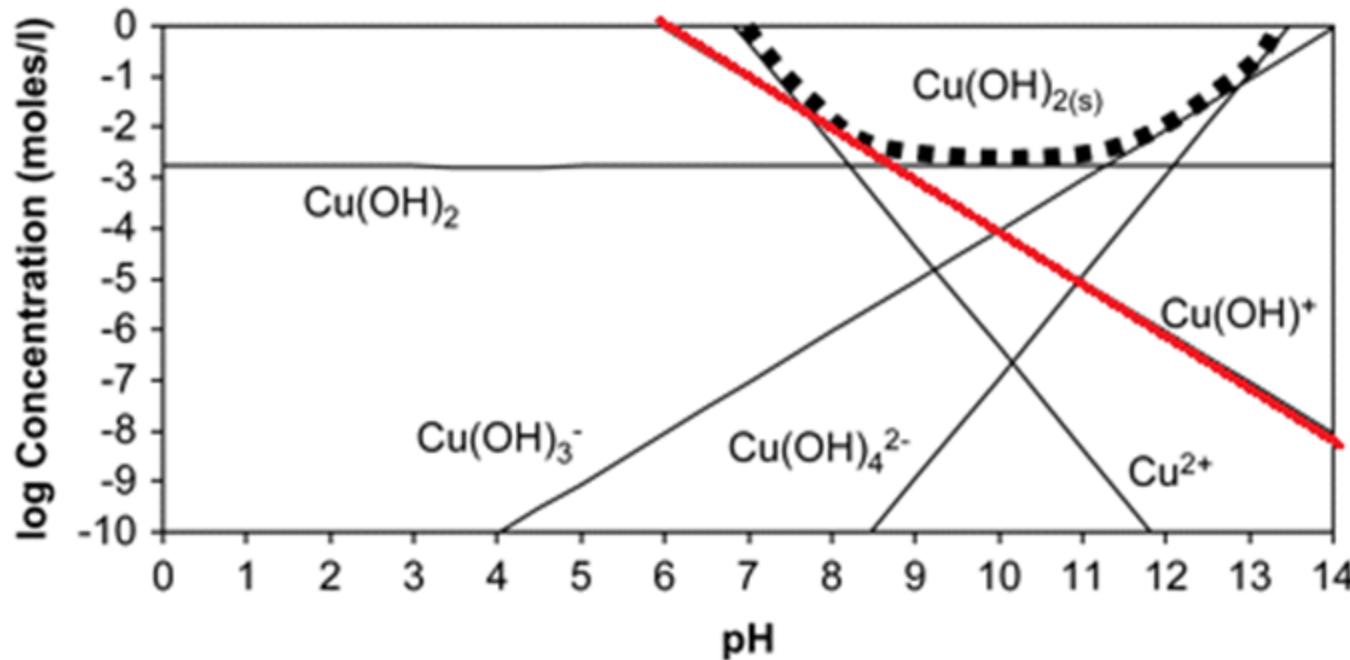


TiO₂ photocatalysis
Fe(III)-EDDS/Air photocatalysis
Fe(III)-EDDS/H₂O₂ photocatalysis

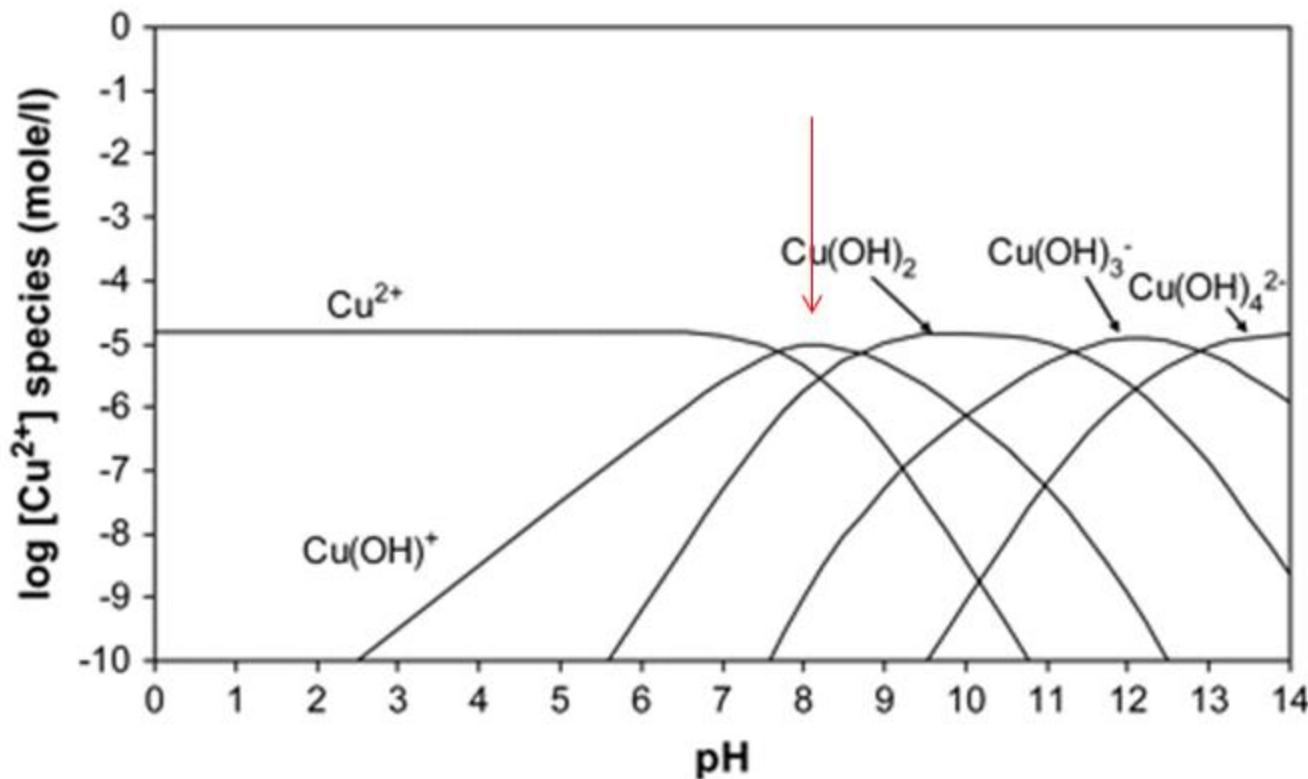
Why?



...probably due to the existence of soluble Cu-hydroxo-complexes such as $\text{Cu}(\text{OH})^+$ at the adopted pH



inside dotted line shows zone where copper hydroxide solid will form



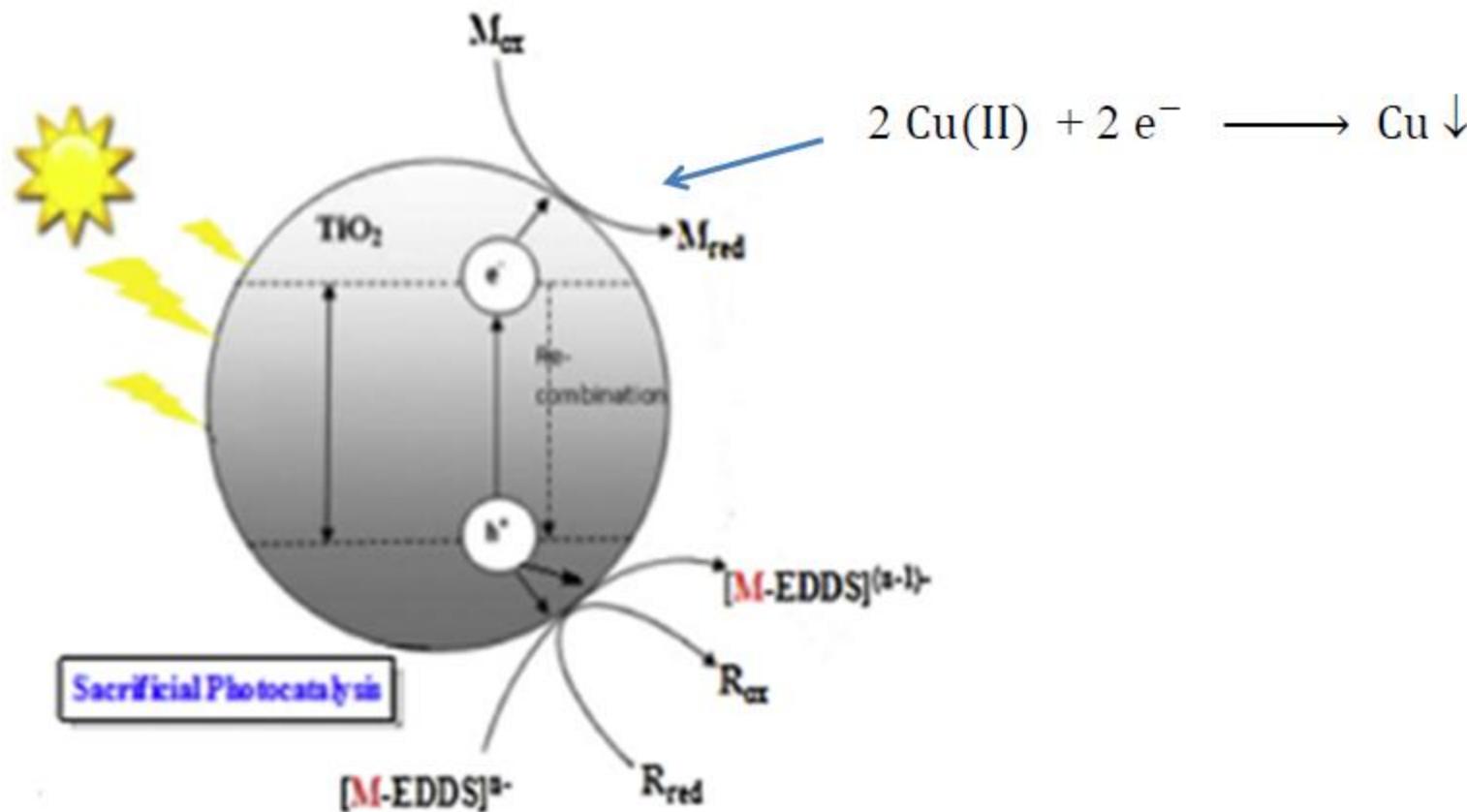
Theoretical copper speciation for hydroxy-complexes in pure water for a total copper concentration of 1 mg/l

How to remove Copper?

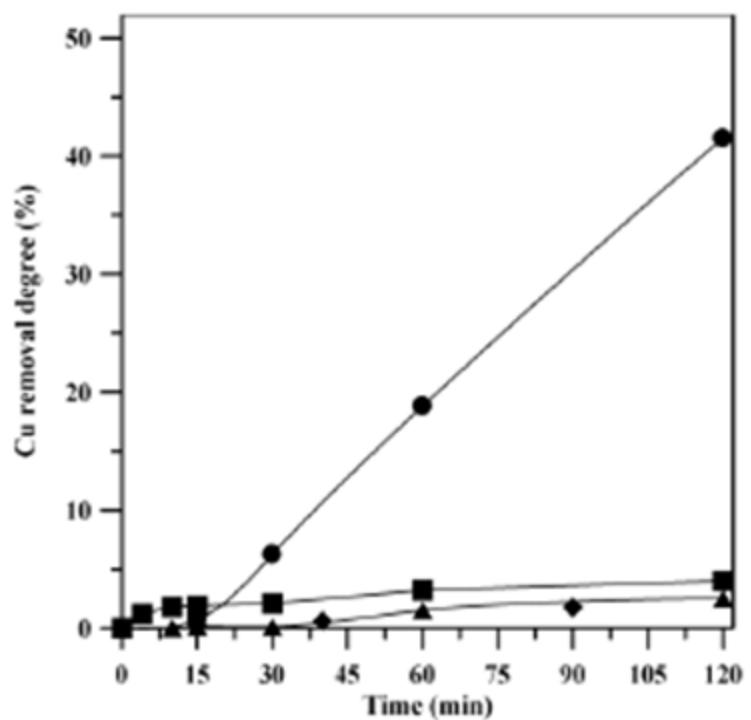


Sacrificial photocatalysis (de-aerated conditions)

Heterogenous photocatalytic process



For Copper



Sacrificial photocatalysis

OK !



TiO₂ photocatalysis

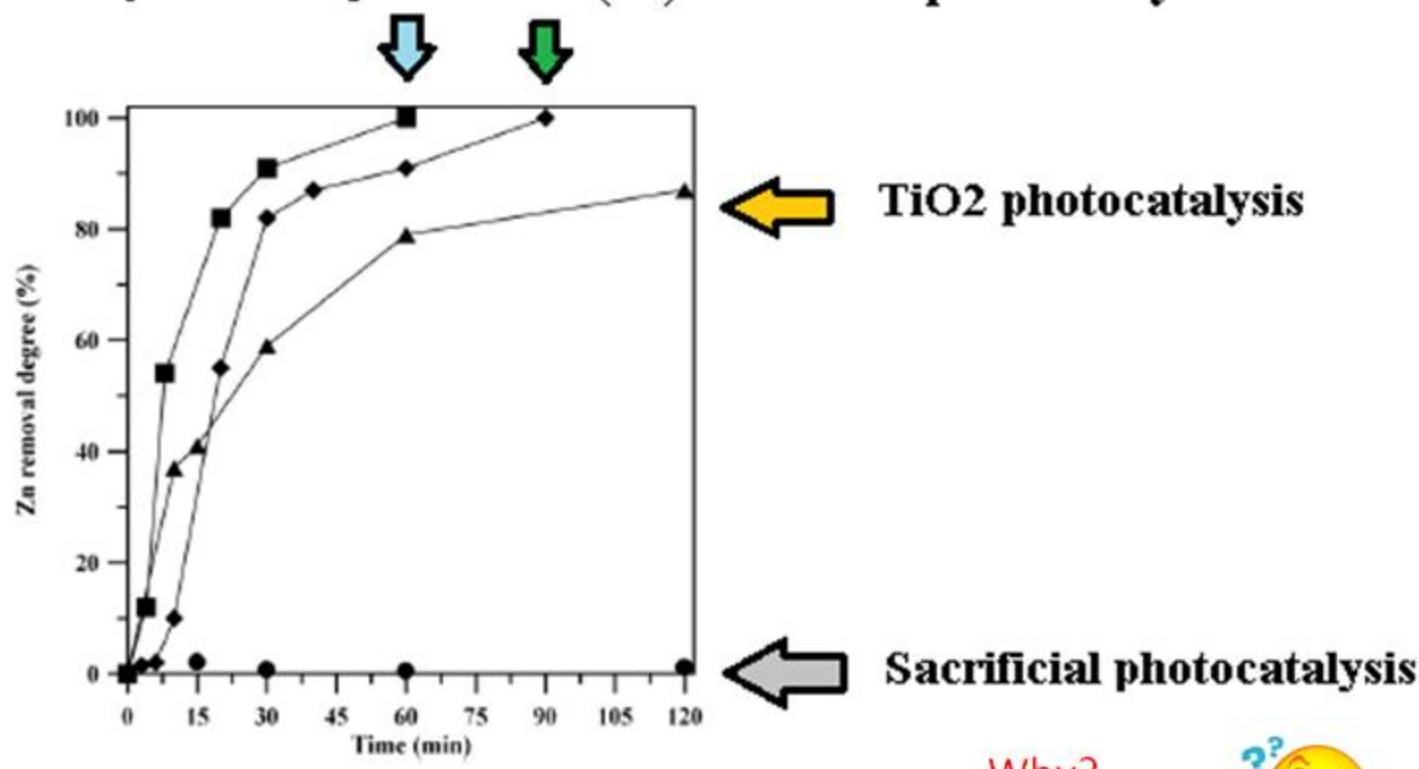
Fe(III)-EDDS/Air photocatalysis

Fe(III)-EDDS/H₂O₂ photocatalysis

In the case of Zinc.....

Fe(III)-EDDS/H₂O₂ photocatalysis

Fe(III)-EDDS/Air photocatalysis



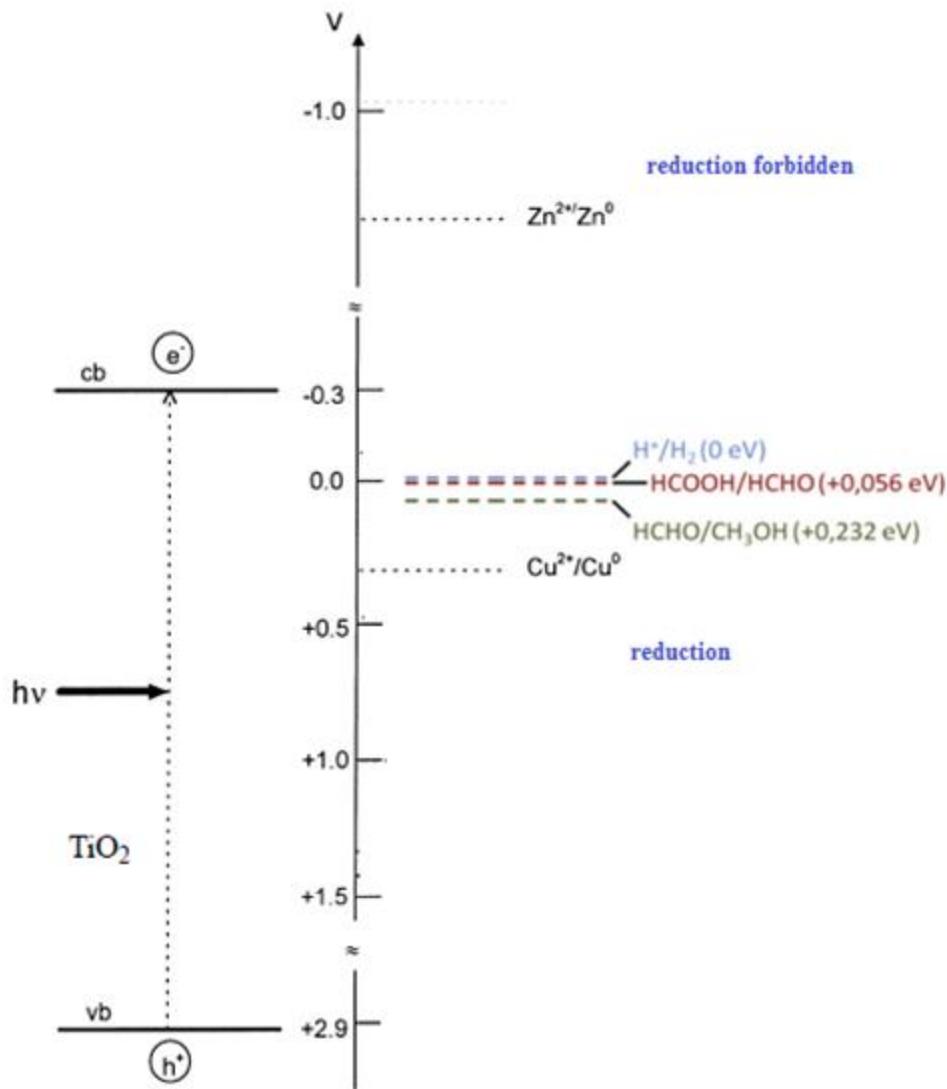
TiO₂ photocatalysis

Sacrificial photocatalysis

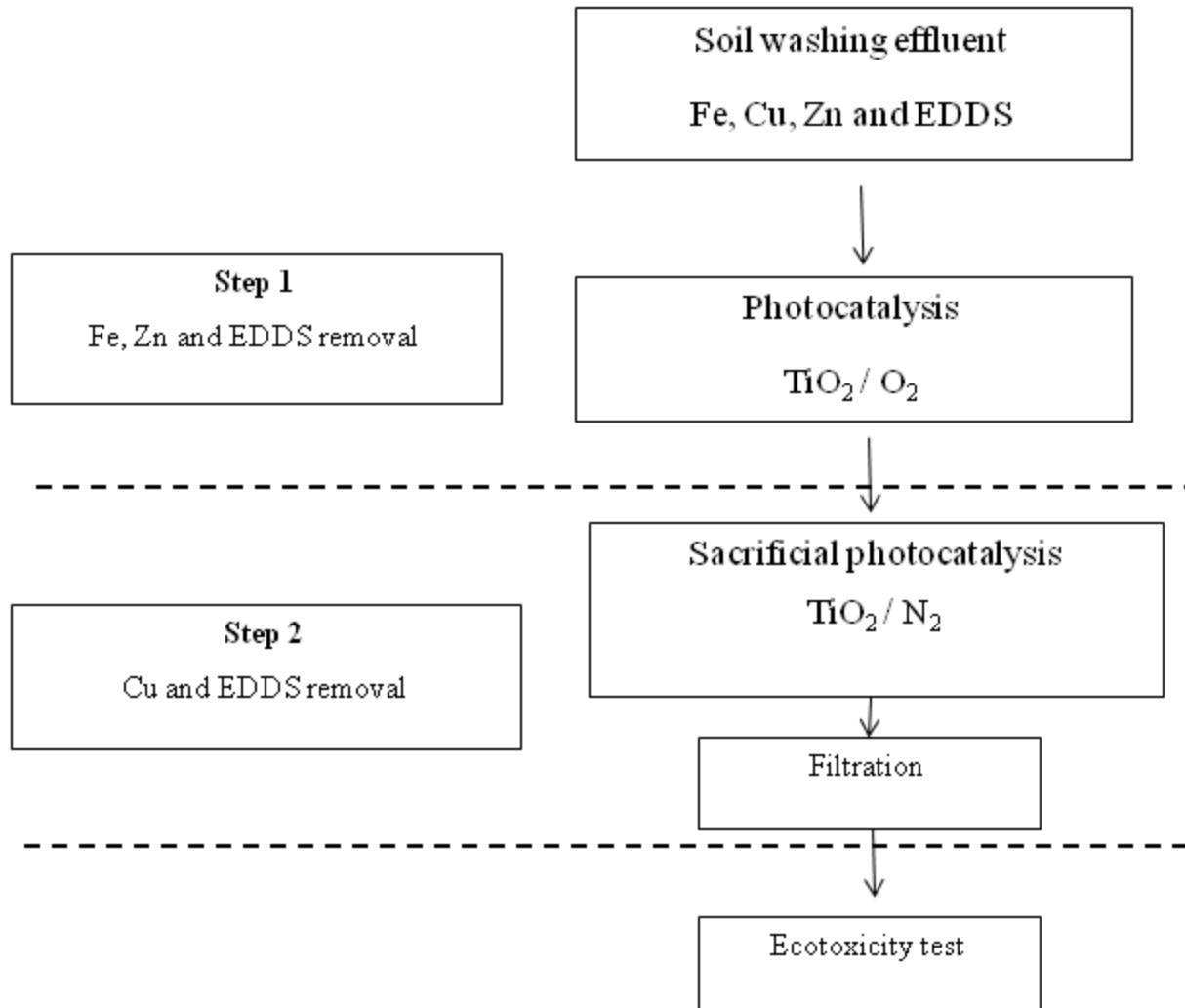
Why?



To achieve a redox reaction, the **conduction band** must be located at a **more negative potential** than the reduction potential of the chemical species that will be reduced, while the **valence band** must be positioned **more positively** than the oxidation potential of the chemical species that will be oxidized



One choice could be firstly the removal of iron, zinc and EDDS through a TiO_2 -photocatalysis with oxygen, followed by a photocatalytic step (sacrificial TiO_2 -photocatalysis) under inert atmosphere for the abatement of the residual metals, particularly copper, and residual organics.



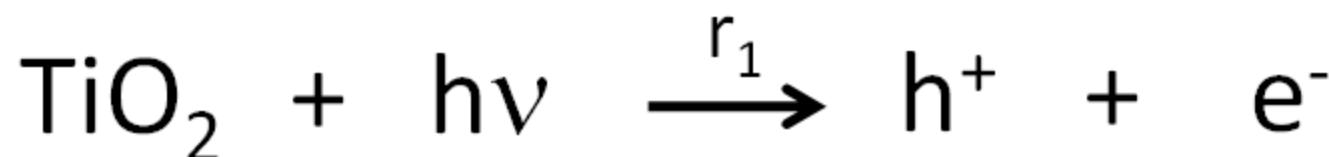
Mechanism and Kinetics for sacrificial photocatalysis

Different mechanisms may be proposed to account for the photocatalytic conversion of an organic substrate (S) depending on degree of adsorption of the latter on the TiO_2 photocatalyst surface

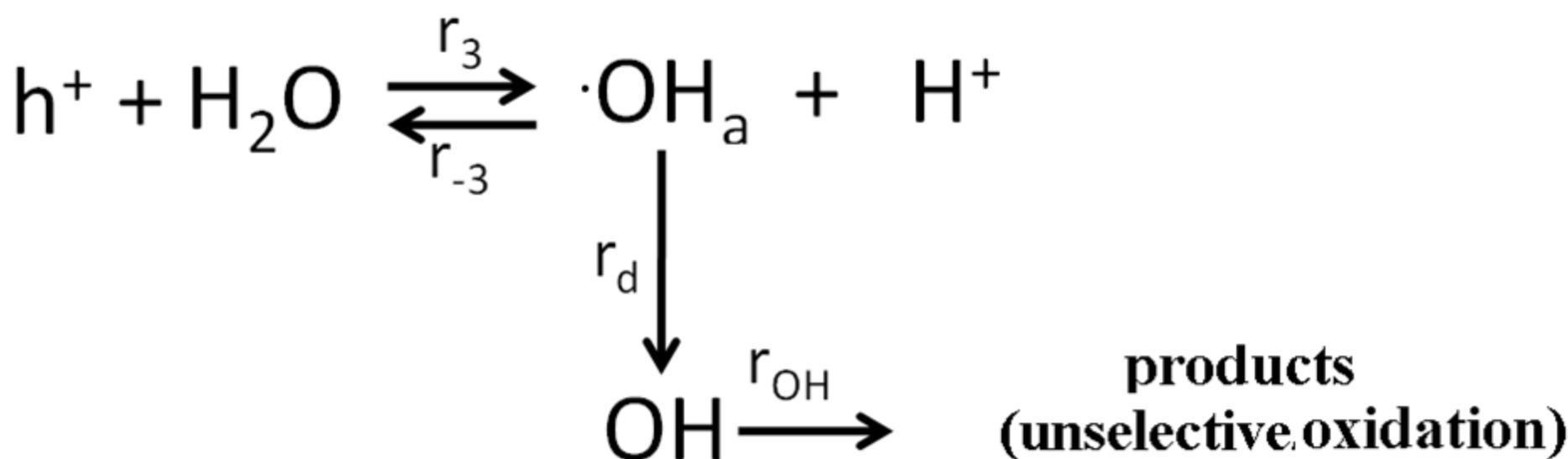
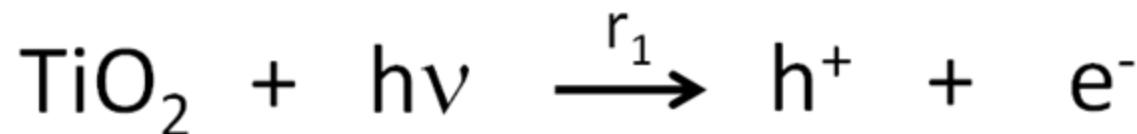
Langmuir 2000, 16, 8964-8972

Environ. Sci. Technol. 2005, 39, 1880-1886

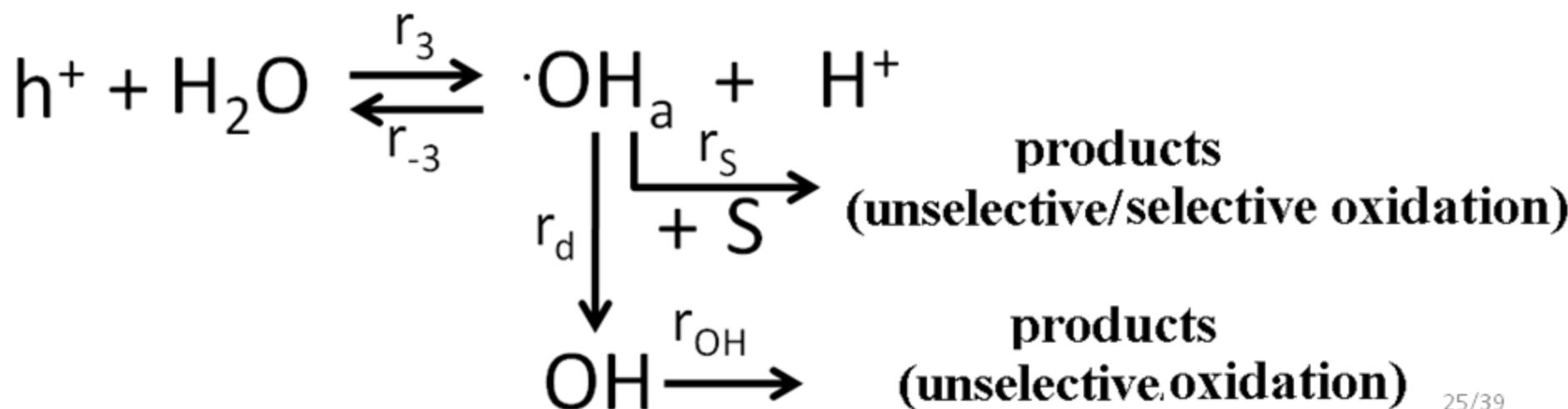
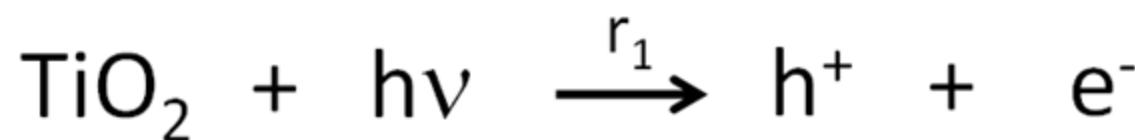
For **strongly** adsorbed organics, the reaction proceeds directly between adsorbed substrate molecules and photogenerated surface holes



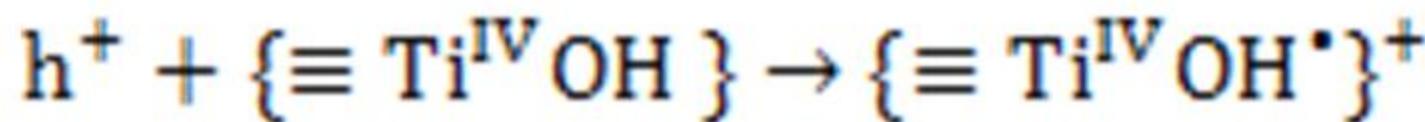
For **not** adsorbed substrates, the photo-oxidation reaction involves the dissolved organic species and free OH radicals (reaction r_{OH})



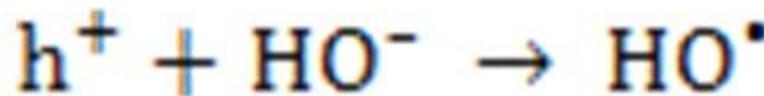
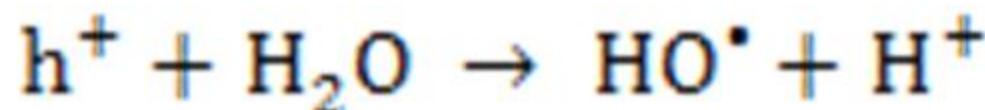
For **weakly** adsorbed substrates, the photo-oxidation reaction involves the dissolved organic species and surface-bound hydroxyl radicals (reaction r_s) or free OH radicals (reaction r_{OH})



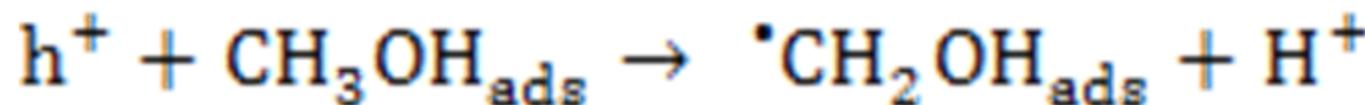
In particular, positive holes can migrate to the TiO₂ surface, where they are trapped by surface titanol groups that generate superficial HO[•] radicals



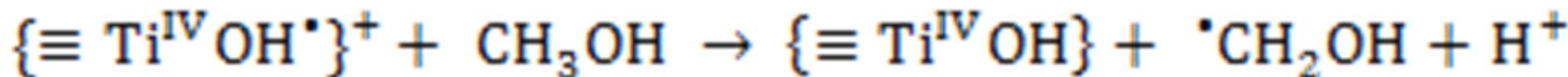
or they can react with adsorbed water molecules or HO⁻ anions, and thus generate free HO[•] radicals



For example, the TiO_2 photo-oxidation of methanol (adsorbed species) can be promoted either by direct hole transfer:



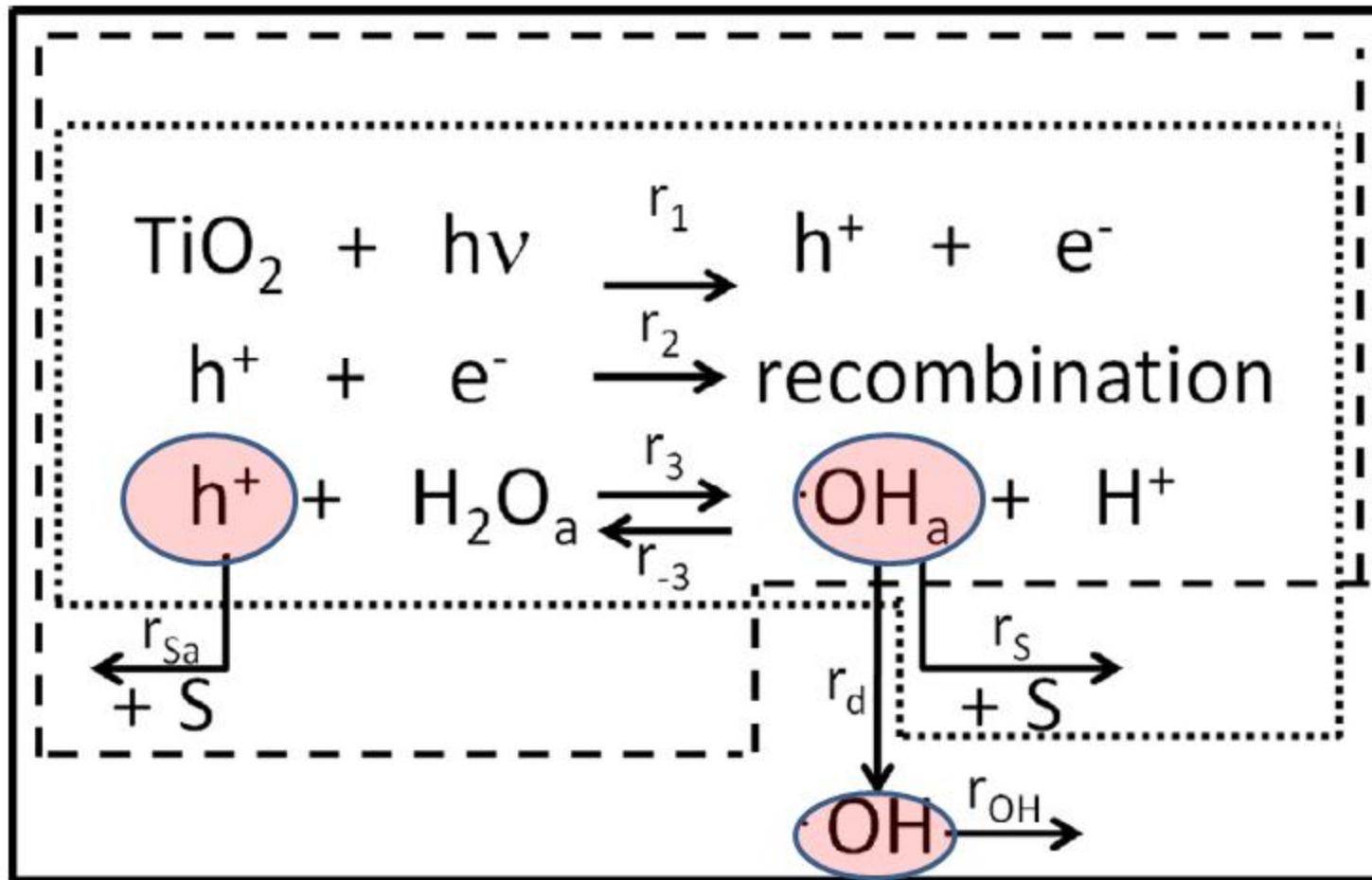
or by a reaction with surface radicals:



Electrochimica Acta 51 (2006) 2230–2236

unselective oxidation

For EDDS, as chelating agent, **three** different chemical models can be supposed



- | | |
|--------------------------|---------|
| Model 1- continuous line | (—) |
| Model 1.1- dashed line | (---) |
| Model 1.2.1- dotted line | (.....) |

Which is the correct mechanism?



Verification of the Proposed Mechanism using Scavengers

Effect of Iodide Ion. Iodide ion is a scavenger and reacts with h_{vb}^+ and $\cdot OH_{ads}$, reducing the number of oxidizing species available at the surface of the catalyst. The valence band hole is easily captured by I^- (the redox potential of the couple I/I^- is 1.3 V) and pathways due to oxidation by surface hydroxyl radicals are also possible because the rate constant of reaction with $\cdot OH_{ads}$ is $1.2 \times 10^{10} M^{-1} s^{-1}$

Iodide can react with both free positive holes and surface-bound hydroxyl radicals

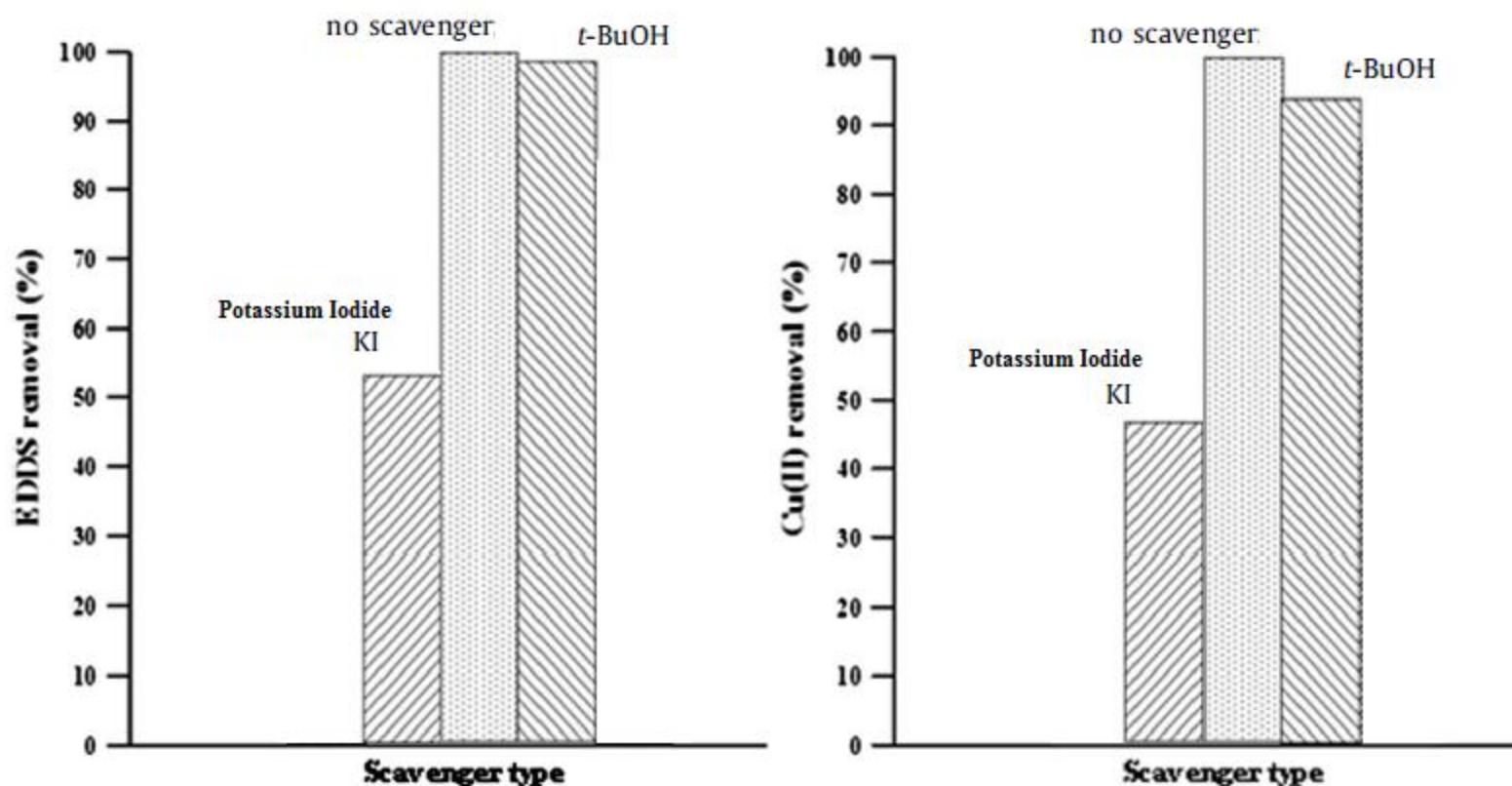
VOL. 41, NO. 16, 2007 / ENVIRONMENTAL SCIENCE & TECHNOLOGY

Effect of Tert-Butyl Alcohol. *t*-BuOH can react quickly with $\cdot OH$ with a rate constant of $6.0 \times 10^8 M^{-1} s^{-1}$

Environ. Sci. Technol. 2004, 38 (24), 6875–6880.

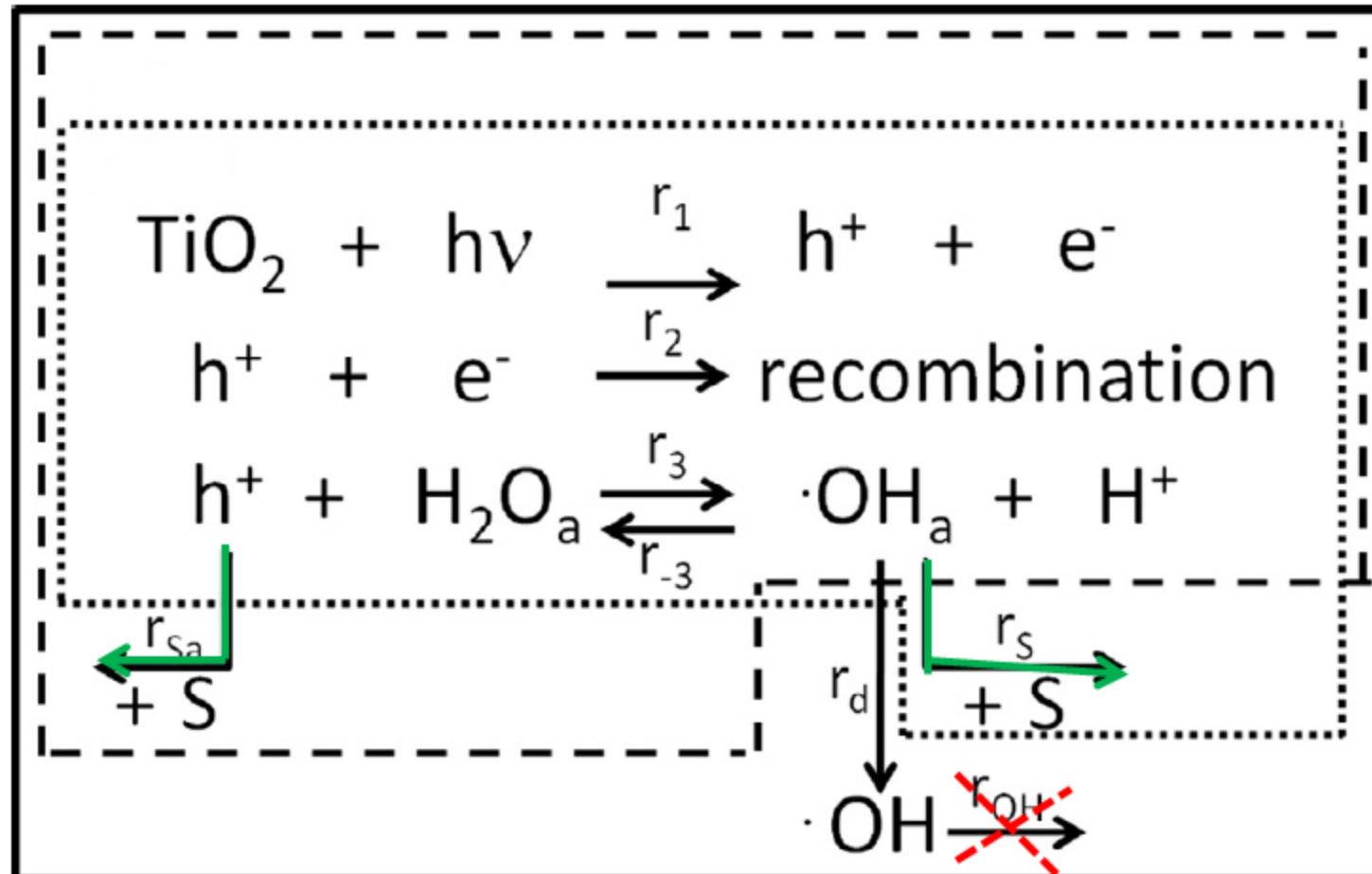
Ter-butanol is a hydroxyl radical scavenger

In presence of **Tert-butyl alcohol**, only **negligible** effects have been observed on the consumption rates of EDDS and Cu(II), on the other hand, in case of **Iodide** addition, there is a **marked** reduction of the system reactivity



EDDS (left) and cupric species (right) photocatalytic removals at 60 min of treatment. []₀ 0.2 mM; [CuSO₄]₀ 1.0 mM; [TiO₂] 50 mg L⁻¹, pH 2.0, purging gas: N₂. T: 25 °C.

Consequently...

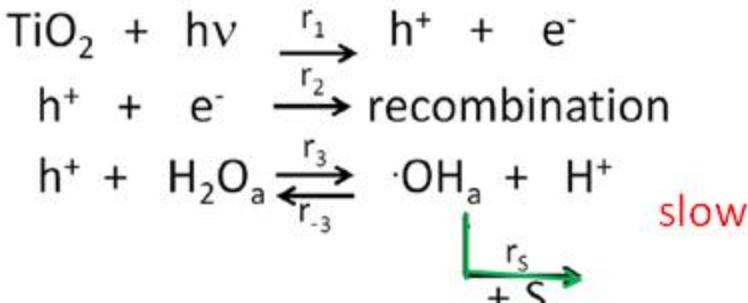
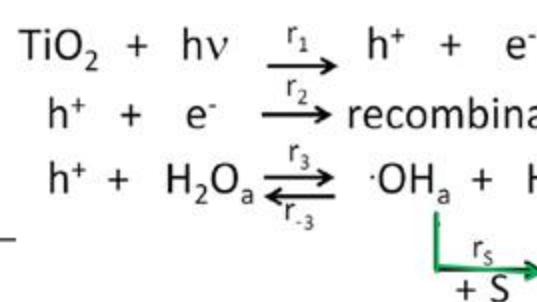


- Model 1- continuous line
- (---) Model 1.1- dashed line
- (.....) Model 1.2.1- dotted line



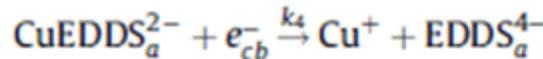
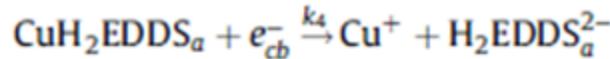
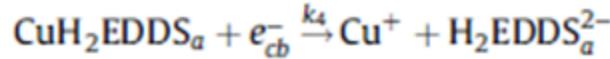
Positive holes or surface-bound HO radicals?

Models proposed and tested.

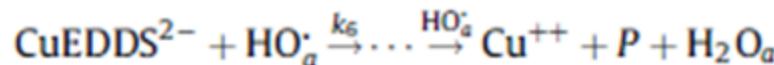
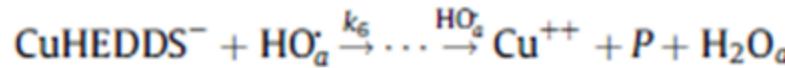
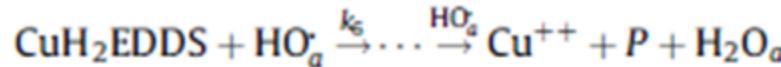
Model	Reactions considered for the organic species consumption	Equations adopted for the mass balances	
1.1	Reaction between substrate adsorbed on the surface and positive holes- r_{9t} , r_{10t} , r_{11t}	$\frac{d[\text{HO}_a]}{dt} = r_3 - r_{-3} = 0$ $\frac{d[h^+]}{dt} = r_1 - r_2 - 2 \cdot (r_{9t} + r_{10t} + r_{11t}) - r_{12} - r_{13}$	$\text{TiO}_2 + h\nu \xrightarrow{r_1} h^+ + e^-$ $h^+ + e^- \xrightarrow{r_2} \text{recombination}$ 
1.2.1	Reaction between the dissolved substrate and the surface-bound hydroxyl radicals- r_{6t} , r_{7t} , r_8	$\frac{d[\text{HO}_a]}{dt} = r_3 - r_{-3} - 2 \cdot (r_{6t} + r_{7t} + r_8) = 0$ $[\cdot\text{OH}_a] = \frac{k_3[h^+]\cdot[\text{H}_2\text{O}_a]}{k_{-3} + 2 \cdot (k_{6t}[\text{S}_{\text{CO}}] + k_{7t}[\text{S}_P] + k_8[P])}$ $\frac{d[h^+]}{dt} = r_1 - r_2 - r_3 + r_{-3} - r_{12} - r_{13}$	$\text{TiO}_2 + h\nu \xrightarrow{r_1} h^+ + e^-$ $h^+ + e^- \xrightarrow{r_2} \text{recombination}$ $h^+ + \text{H}_2\text{O}_a \xrightleftharpoons[r_{-3}]{r_3} \cdot\text{OH}_a + \text{H}^+$ 
1.2.2	Reaction between the dissolved substrate and the surface-bound hydroxyl radicals considering fast equilibration of surface-bound hydroxyl radicals with the positive holes- r_{6t} , r_{7t} , r_8	$[\cdot\text{OH}_a] = \frac{K_{eq}[h^+]\cdot[\text{H}_2\text{O}_a]}{[\text{H}^+]}$ $\frac{d[h^+]}{dt} = \frac{[r_1 - r_2 - 2 \cdot h^+ \cdot (k_{6t}[\text{S}_{\text{CO}}] + k_{7t}[\text{S}_P] + k_8[P]) - r_{12} - r_{13}]}{1 + K_{eq}\frac{[\text{H}_2\text{O}_a]}{[\text{H}^+]}}$	$\text{TiO}_2 + h\nu \xrightarrow{r_1} h^+ + e^-$ $h^+ + e^- \xrightarrow{r_2} \text{recombination}$ $h^+ + \text{H}_2\text{O}_a \xrightleftharpoons[r_{-3}]{r_3} \cdot\text{OH}_a + \text{H}^+$ fast 

Due to the **complexity** of the reacting system, some simplifications have been made:

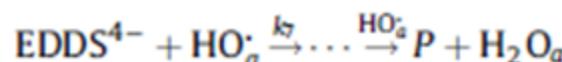
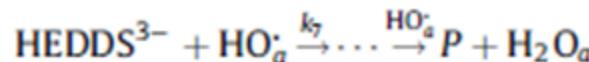
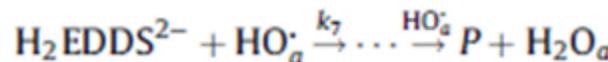
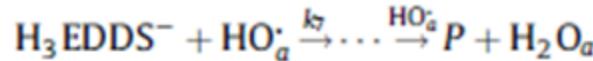
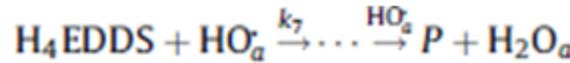
a single kinetic constant (k4) for reactions of different CuEDDS species with electrons



a single kinetic constant (k6) for reactions of different CuEDDS species with holes



a single kinetic constant (k7) for reactions of different EDDS species with holes



Equilibrium equations for substrate adsorption on the catalyst surface.

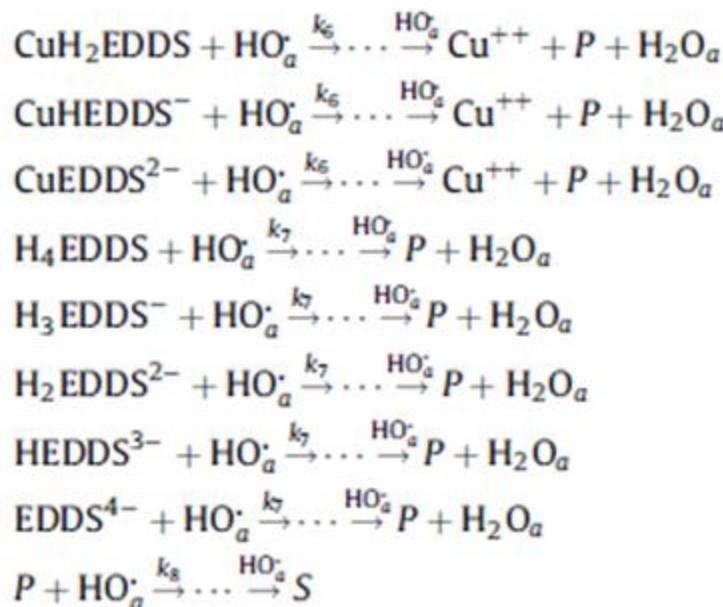
n°	Equilibrium adsorption
Eq.1	$[CuH_2EDDS_a] = K_{ad} \cdot [CuH_2EDDS] \cdot [C_f]$
Eq.2	$[CuHEDDS_a^-] = K_{ad} \cdot [CuHEDDS^-] \cdot [C_f]$
Eq.3	$[CuEDDS_a^{2-}] = K_{ad} \cdot [CuEDDS^{2-}] \cdot [C_f]$
Eq.4	$[H_4EDDS_a] = K_{ad} \cdot [H_4EDDS] \cdot [C_f]$
Eq.5	$[H_3EDDS_a^-] = K_{ad} \cdot [H_3EDDS^-] \cdot [C_f]$
Eq.6	$[H_2EDDS_a^{2-}] = K_{ad} \cdot [H_2EDDS^{2-}] \cdot [C_f]$
Eq.7	$[HEDDS_a^{3-}] = K_{ad} \cdot [HEDDS^{3-}] \cdot [C_f]$
Eq.8	$[EDDS_a^{4-}] = K_{ad} \cdot [EDDS^{4-}] \cdot [C_f]$

$[C_f]$ is the concentration of free active sites on the photocatalyst surface.

Due to the absence of experimental evidence of EDDS adsorption on the TiO₂ surface, is assumed

$$\cancel{[C_{tot}] = [C_f] + [C_{Sa}]}$$

all by-products are considered as a single component



steady-state hypothesis for all radical species

$$\frac{d[\cdot\text{OH}_a]}{dt} = r_3 - r_{-3} - r_S = 0$$

Table 1

Reaction network proposed for the investigated chemical system. (1) HSO_4^- is in equilibrium with SO_4^{2-} (see below the equilibrium of deprotonation of hydrogensulfate ion). The presence of these species is due to the fact that the cupric ions have been added to the solution as CuSO_4 and the reacting solution pH has been adjusted at the desired value by using concentrated H_2SO_4 .

<i>r</i> ^a	Reaction	Rate equation
<i>r</i> ₁	$\text{TiO}_2 + h\nu \xrightarrow{k_1} e_{\text{cb}}^- + h_{\text{vb}}^+$	$r_1 = k_1 \cdot [\text{TiO}_2] - \frac{\Phi_{\text{TiO}_2} h}{2}$
<i>r</i> ₂	$e_{\text{cb}}^- + h_{\text{vb}}^+ \xrightarrow{k_2} \text{heat}$	$r_2 = k_2 \cdot [e_{\text{cb}}^-] \cdot [h_{\text{vb}}^+]$
<i>r</i> ₃	$h_{\text{vb}}^+ + \text{H}_2\text{O}_2 \xrightarrow{k_3} \text{HO}_2^+ + \text{H}^+$	$r_3 = k_3 \cdot [h_{\text{vb}}^+] \cdot [\text{H}_2\text{O}_2]$
<i>r</i> ₋₃	$\text{HO}_2^+ + \text{H}^+ \xrightarrow{k_3} h_{\text{vb}}^+ + \text{H}_2\text{O}_2$	$r_{-3} = k_{-3} \cdot [\text{HO}_2^+]$
<i>Reactions with photogenerated electrons</i>		
<i>r</i> _{4a}	$\text{CuH}_2\text{EDDS}_a + e_{\text{cb}}^- \xrightarrow{k_4} \text{Cu}^+ + \text{H}_2\text{EDDS}_a^{2-}$	$r_{4a} = k_4 \cdot [e_{\text{cb}}^-] \cdot [\text{CuH}_2\text{EDDS}_a]$
<i>r</i> _{4b}	$\text{CuH}_2\text{EDDS}_a + e_{\text{cb}}^- \xrightarrow{k_4} \text{Cu}^+ + \text{H}_2\text{EDDS}_a^{2-}$	$r_{4b} = k_4 \cdot [e_{\text{cb}}^-] \cdot [\text{CuHEDDS}_a^-]$
<i>r</i> _{4c}	$\text{CuEDDS}_a^{2-} + e_{\text{cb}}^- \xrightarrow{k_4} \text{Cu}^+ + \text{EDDS}_a^{3-}$	$r_{4c} = k_4 \cdot [e_{\text{cb}}^-] \cdot [\text{CuEDDS}_a^{2-}]$
<i>r</i> ₅	$\text{Cu}^+ + e_{\text{cb}}^- \xrightarrow{k_5} \text{Cu}^0$	$r_5 = k_5 \cdot [\text{Cu}^+] \cdot [e_{\text{cb}}^-]$
<i>Reactions with surface-bound hydroxyl radicals</i>		
<i>r</i> _{6a}	$\text{CuH}_2\text{EDDS} + \text{HO}_2^+ \xrightarrow{k_6} \text{Cu}^{++} + P + \text{H}_2\text{O}_2$	$r_{6a} = k_6 \cdot [\text{HO}_2^+] \cdot [\text{CuH}_2\text{EDDS}]$
<i>r</i> _{6b}	$\text{CuHEDDS}^- + \text{HO}_2^+ \xrightarrow{k_6} \text{Cu}^{++} + P + \text{H}_2\text{O}_2$	$r_{6b} = k_6 \cdot [\text{HO}_2^+] \cdot [\text{CuHEDDS}^-]$
<i>r</i> _{6c}	$\text{CuEDDS}^{2-} + \text{HO}_2^+ \xrightarrow{k_6} \text{Cu}^{++} + P + \text{H}_2\text{O}_2$	$r_{6c} = k_6 \cdot [\text{HO}_2^+] \cdot [\text{CuEDDS}^{2-}]$
<i>r</i> _{7a}	$\text{H}_4\text{EDDS} + \text{HO}_2^+ \xrightarrow{k_7} P + \text{H}_2\text{O}_2$	$r_{7a} = k_7 \cdot [\text{HO}_2^+] \cdot [\text{H}_4\text{EDDS}]$
<i>r</i> _{7b}	$\text{H}_3\text{EDDS}^- + \text{HO}_2^+ \xrightarrow{k_7} P + \text{H}_2\text{O}_2$	$r_{7b} = k_7 \cdot [\text{HO}_2^+] \cdot [\text{H}_3\text{EDDS}^-]$
<i>r</i> _{7c}	$\text{H}_2\text{EDDS}^{2-} + \text{HO}_2^+ \xrightarrow{k_7} P + \text{H}_2\text{O}_2$	$r_{7c} = k_7 \cdot [\text{HO}_2^+] \cdot [\text{H}_2\text{EDDS}^{2-}]$
<i>r</i> _{7d}	$\text{EDDS}^{3-} + \text{HO}_2^+ \xrightarrow{k_7} P + \text{H}_2\text{O}_2$	$r_{7d} = k_7 \cdot [\text{HO}_2^+] \cdot [\text{EDDS}^{3-}]$
<i>r</i> _{7e}	$\text{EDDS}^{4-} + \text{HO}_2^+ \xrightarrow{k_7} P + \text{H}_2\text{O}_2$	$r_{7e} = k_7 \cdot [\text{HO}_2^+] \cdot [\text{EDDS}^{4-}]$
<i>r</i> ₈	$P + \text{HO}_2^+ \xrightarrow{k_8} S$	$r_8 = k_8 \cdot [P] \cdot [\text{HO}_2^+]$
<i>Reactions with photogenerated holes</i>		
<i>r</i> _{9a}	$\text{CuH}_2\text{EDDS}_a + h_{\text{vb}}^+ \xrightarrow{k_9} P + \text{H}^+ + \text{Cu}^{++}$	$r_{9a} = k_9 \cdot [h_{\text{vb}}^+] \cdot [\text{CuH}_2\text{EDDS}_a]$
<i>r</i> _{9b}	$\text{CuHEDDS}_a^- + h_{\text{vb}}^+ \xrightarrow{k_9} P + \text{H}^+ + \text{Cu}^{++}$	$r_{9b} = k_9 \cdot [h_{\text{vb}}^+] \cdot [\text{CuHEDDS}_a^-]$
<i>r</i> _{9c}	$\text{CuEDDS}_a^{2-} + h_{\text{vb}}^+ \xrightarrow{k_9} P + \text{H}^+ + \text{Cu}^{++}$	$r_{9c} = k_9 \cdot [h_{\text{vb}}^+] \cdot [\text{CuEDDS}_a^{2-}]$
<i>r</i> _{10a}	$\text{H}_4\text{EDDS}_a + h_{\text{vb}}^+ \xrightarrow{k_{10}} P + \text{H}^+$	$r_{10a} = k_{10} \cdot [h_{\text{vb}}^+] \cdot [\text{H}_4\text{EDDS}_a]$
<i>r</i> _{10b}	$\text{H}_3\text{EDDS}_a^- + h_{\text{vb}}^+ \xrightarrow{k_{10}} P + \text{H}^+$	$r_{10b} = k_{10} \cdot [h_{\text{vb}}^+] \cdot [\text{H}_3\text{EDDS}_a^-]$
<i>r</i> _{10c}	$\text{H}_2\text{EDDS}_a^{2-} + h_{\text{vb}}^+ \xrightarrow{k_{10}} P + \text{H}^+$	$r_{10c} = k_{10} \cdot [h_{\text{vb}}^+] \cdot [\text{H}_2\text{EDDS}_a^{2-}]$
<i>r</i> _{10d}	$\text{EDDS}_a^{3-} + h_{\text{vb}}^+ \xrightarrow{k_{10}} P + \text{H}^+$	$r_{10d} = k_{10} \cdot [h_{\text{vb}}^+] \cdot [\text{EDDS}_a^{3-}]$
<i>r</i> _{10e}	$\text{EDDS}_a^{4-} + h_{\text{vb}}^+ \xrightarrow{k_{10}} P + \text{H}^+$	$r_{10e} = k_{10} \cdot [h_{\text{vb}}^+] \cdot [\text{H}_4\text{EDDS}_a] \cdot [\text{EDDS}_a^{4-}]$
<i>r</i> ₁₁	$P + h_{\text{vb}}^+ \xrightarrow{k_{11}} S$	$r_{11} = k_{11} \cdot [P] \cdot [h_{\text{vb}}^+]$
<i>r</i> ₁₂	$\text{Cu}^+ + h_{\text{vb}}^+ \xrightarrow{k_{12}} \text{Cu}^{++}$	$r_{12} = k_{12} \cdot [\text{Cu}^+] \cdot [h_{\text{vb}}^+]$
<i>r</i> ₁₃	$\text{HSO}_4^- + h_{\text{vb}}^+ \xrightarrow{k_{13}} \text{HSO}_4^{(1)}$	$r_{13} = k_{13} \cdot [\text{HSO}_4^-] \cdot [h_{\text{vb}}^+]$

For example...

Mass balance equations for the species included in the reaction network reported in the Model 1. $r_{nt} = (r_{na} + r_{nb} + \dots)$ with $n = 6, 7, 9, 10$.

n.	Balance	Species
Bal.1	$\frac{d[e^-]}{dt} = r_1 - r_2 - r_{4a} - r_{4b} - r_{4c} - r_5$	Electrons
Bal.2	$\frac{d[h^+]}{dt} = r_1 - r_2 - r_3 + r_{-3} - 2 \cdot (r_{9t} + r_{10t} + r_{11}) - r_{12} - r_{13}$	Holes
Bal.3	$\frac{d[H_2O_a]}{dt} = \text{constant}$	Water
Bal.4	$\frac{d[HO_a]}{dt} = r_3 - r_{-3} - 2 \cdot (r_{6t} + r_{7t} + r_8)$	HO_a
Bal.5	$\frac{d[Cu^0]}{dt} = r_5$	Cu^0
Bal.6	$\frac{d[Cu^+]}{dt} = r_{4a} + r_{4b} + r_{4c} - r_5 - r_{12}$	Cu^+
Bal.7	$\frac{d[P]}{dt} = r_{6t} + r_{7t} - r_8 + r_{9t} + r_{10t} - r_{11}$	P
Bal.8	$\frac{d[S]}{dt} = r_8 + r_{11}$	S
Bal.9	$[SO_4^{2-}]_0 = [SO_4^{2-}] + [HSO_4^-] + [HSO_{4a}^-]$	HSO_4^-
Bal.10	$[Cu^{2+}] = \frac{[CuSO_4]_0 - [Cu_0] - [Cu^+]}{1 + [H_4EDDS] \cdot Den_2 \cdot (1 + K_{ad} \cdot [C_f])}$	Cu^{2+}
Bal.11	$[H_4EDDS] = \frac{[EDDS_0] - [P] - [S]}{(1 + K_{ad} \cdot [C_f]) \cdot (1 + Den_1 + Den_2 \cdot [Cu^{++}])}$	H_4EDDS

where:

$$[Cu_l] = [CuEDDS^{2-}] + [CuHEDDS^-] + [CuH_2EDDS].$$

$$[Cu_a] = K_{ad} \cdot [C_f] \cdot [Cu_l].$$

$$[EDDS_f] = [EDDS^{4-}] + [HEDDS^{3-}] + [H_2EDDS^{2-}] + [H_3EDDS^-] + [Cu_l].$$

$$[EDDS_a] = K_{ad} \cdot [C_f] \cdot [EDDS_f] + [H_4EDDS_a].$$

Optimization mode...

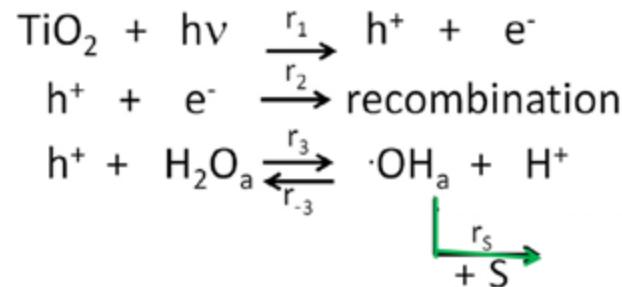
Table 7

Objective function values (φ) obtained by the different models proposed.

Model	φ value
1.1	1.23
1.2.1	Does not converge
1.2.2	0.23

$$\varphi = \sum_{l=1}^f \sum_{j=1}^k \sum_{i=1}^n (y_{i,j,l} - c_{i,j,l})^2$$

where $y_{i,j,l}$ and $c_{i,j,l}$ indicate the concentrations of the species measured and calculated by the model respectively, n is the number of experimental time at which samples have been taken from the reactor, k is the number of the component (2 in the present case, Cu(II) and EDDS) and f indicates the number of the run used in the optimization procedure. The results of the nine experimental runs have been simultaneously used in a single optimization procedure. The values of φ as derived at the end of the optimization procedure are shown in Table 7 for each model tested.



Kinetic parameters	$[M^{-1} s^{-1}]$
k_4	$(4.27 \pm 0.45) \cdot 10^9$
k_6	$(1.42 \pm 0.15) \cdot 10^7$
k_7	$(5.88 \pm 0.28) \cdot 10^6$
k_8	$(6.26 \pm 0.85) \cdot 10^6$
Equilibrium constant	[expression dependent]
K_{ad}	$(1.36 \pm 0.12) \cdot 10^1 [M^{-1}]$
$K_{eq} \cdot [H_2O_a]$	$\forall K_{eq} \cdot [H_2O_a] \in [10^{-4} \dots 10^4] [M]$

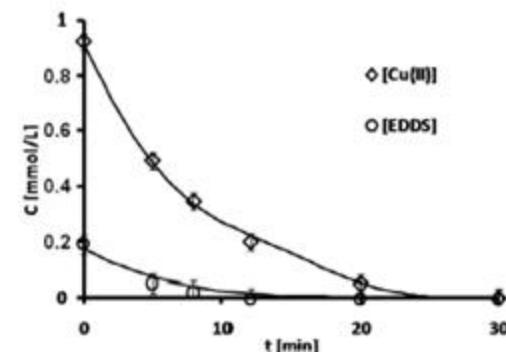


Fig. 3. Comparison between experimental (symbol) and evaluated (continuous lines) data: $[EDDS]_0 = 0.19 \text{ mM}$, $[CuSO_4]_0 = 0.92 \text{ mM}$, TiO_2 (pure anatase) = 500 mg L^{-1} , purging gas = N_2 , Hg vapor lamp, pH = 2.0, $T = 25^\circ\text{C}$.

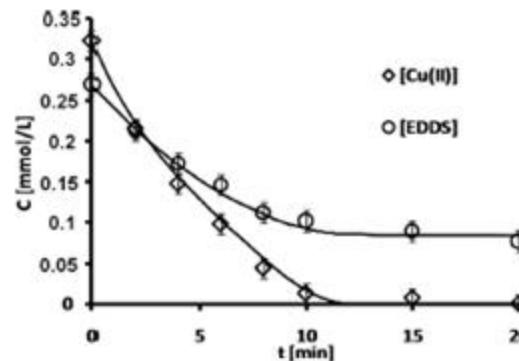


Fig. 6. Comparison between experimental (symbol) and simulated (continuous lines) data: $[EDDS]_0 = 0.27 \text{ mM}$, $[CuSO_4]_0 = 0.32 \text{ mM}$, TiO_2 (pure anatase) = 50 mg L^{-1} , purging gas = N_2 , Hg vapor lamp, pH = 2.0, $T = 25^\circ\text{C}$.

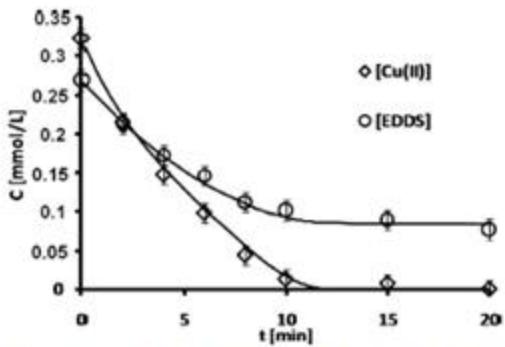


Fig. 6. Comparison between experimental (symbol) and simulated (continuous lines) data: $[EDDS]_0 = 0.27 \text{ mM}$, $[CuSO_4]_0 = 0.32 \text{ mM}$, TiO_2 (pure anatase) = 50 mg L^{-1} , purging gas = N_2 , Hg vapor lamp, pH = 2.0, $T = 25^\circ\text{C}$.

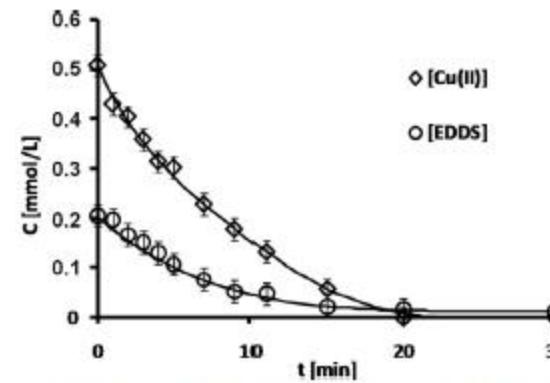


Fig. 5. Comparison between experimental (symbol) and evaluated (continuous lines) data: $[EDDS]_0 = 0.21 \text{ mM}$, $[CuSO_4]_0 = 0.51 \text{ mM}$, TiO_2 (pure anatase) = 50 mg L^{-1} , purging gas = N_2 , Hg vapor lamp, pH = 2.0, $T = 25^\circ\text{C}$.

Unknown parameters

Simulation examples

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IMPLEMENTATION OF ECO-COMPATIBLE PROTOCOLS FOR AGRICULTURAL SOIL
REMEDIATION IN LITORALE DOMIZIO-AGRO AVERSANO