

SIMULATION AND DESIGN OF PHOTOREACTORS

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**Summer School 2017
Porto, 11th July 2017**

Outline

- 1.- Introduction ————— The Scaling-Up Problem
- 2.- Methodology ————— Proposed Scaling-Up Procedure
- 3.- Lab Scale —————
 - Photoreactor
 - Mass Balance
 - Kinetic Model
 - Radiation Model
 - Kinetic Parameters Estimation
- 4.- Bench Scale —————
 - Photoreactor
 - Radiation Model
 - Kinetic Model
 - Mass Balance
 - Scaling-Up Validation
- 5.- Conclusions

The Scaling-Up Problem

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

Lab Scale.

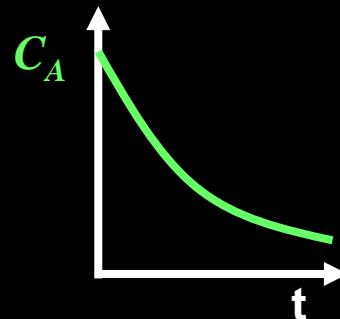
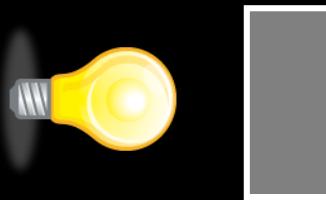
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Conclusions.

Laboratory Experiments



$$r = \frac{dC_A}{dt} = kC_A$$

$$r = \frac{dC_A}{dt} = k \frac{KC_A}{1 + KC_A}$$

The Scaling-Up Problem

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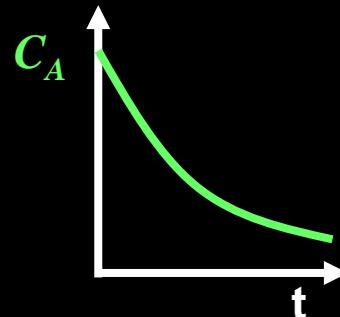
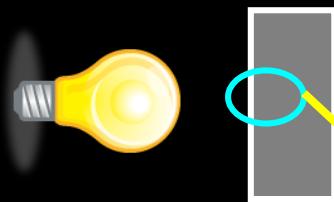
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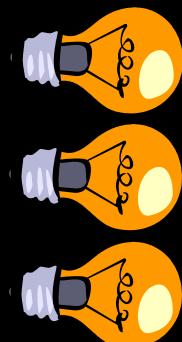
Laboratory Experiments



$$r = \frac{dC_A}{dt} = kC_A$$

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Design of Large Photoreactors



TiO_2
suspension

Radiation
Profiles

The Scaling-Up Problem

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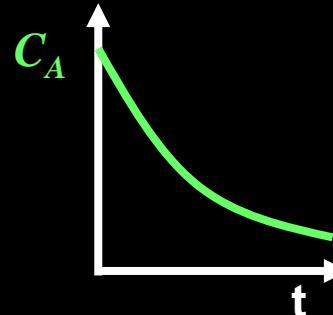
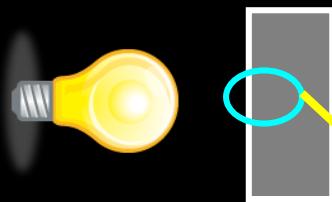
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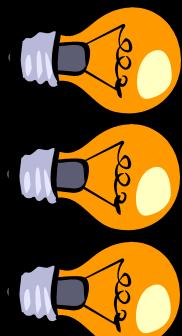
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Laboratory Experiments



$$r = \frac{dC_A}{dt} = kC_A$$
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Design of Large Photoreactors



TiO₂ suspension

Radiation Profiles

$$r = f(x) = f(C_A, LVRPA)$$

Proposed Scaling-Up Procedure

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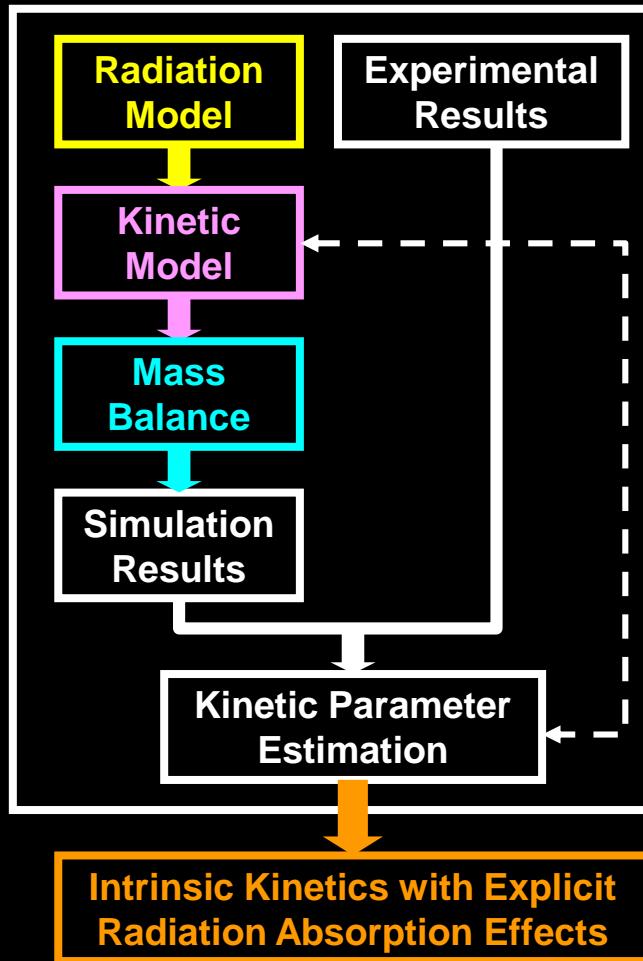
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Laboratory Scale Photoreactor



Proposed Scaling-Up Procedure

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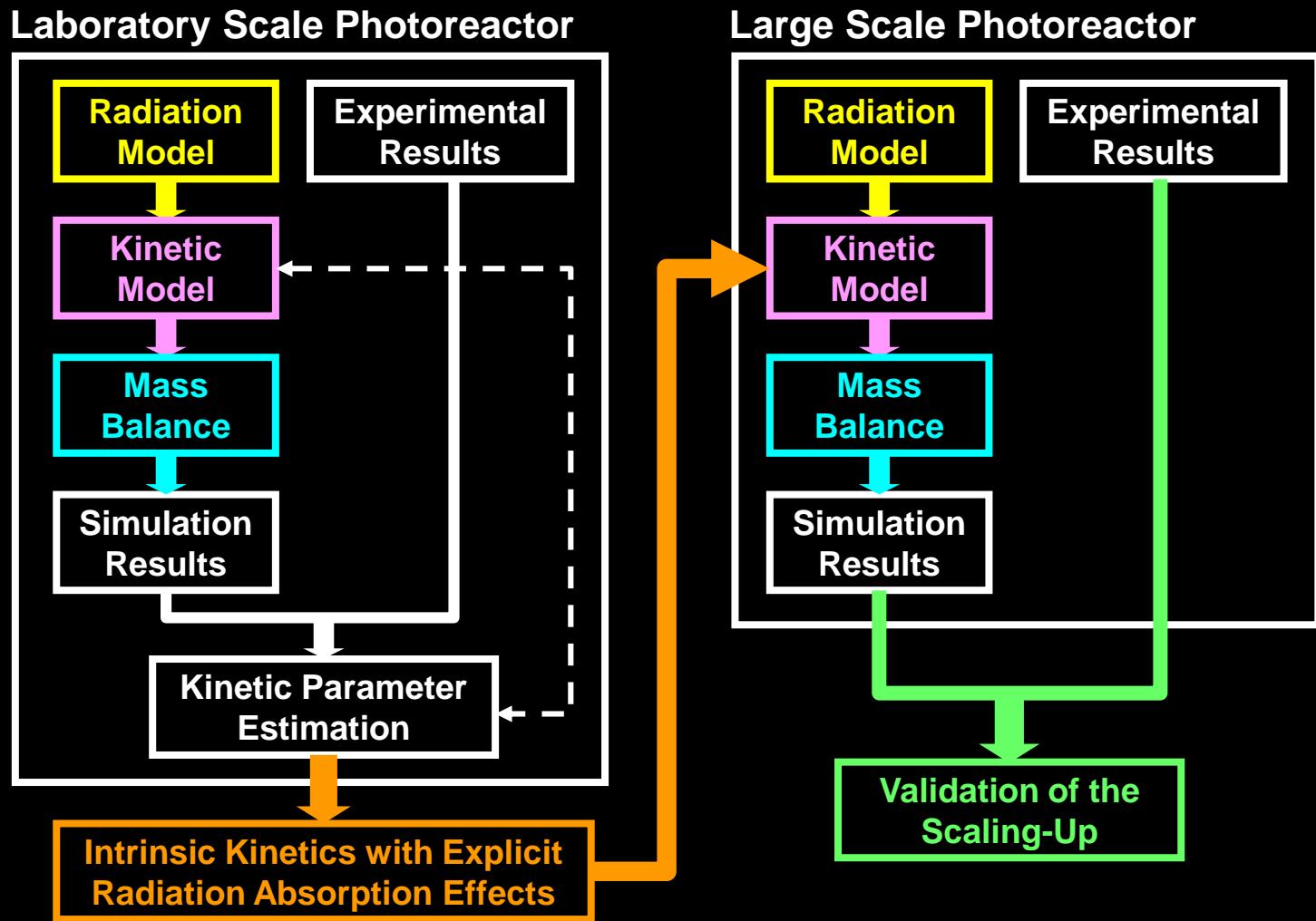
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Lab Scale: Photoreactor & Experimental

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Introduction.

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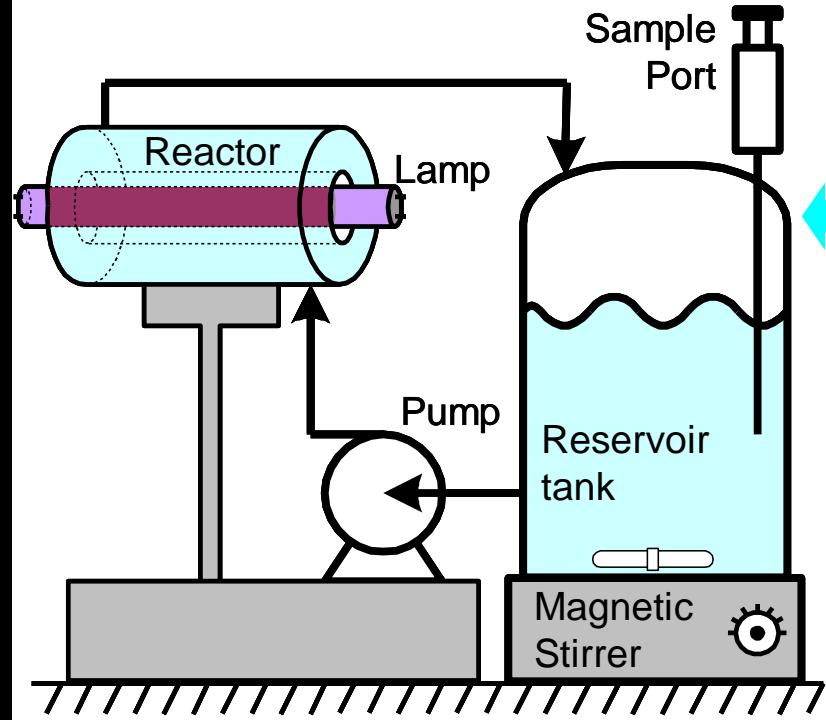
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Laboratory scale reactor:

$$V_R = 188.5 \text{ cm}^3, V_{\text{Tot}} = 1 \text{ L}$$

Lamp: Philips TL 6W
L = 21 cm, $\Phi = 1.6 \text{ cm}$

Lab Scale: Photoreactor & Experimental

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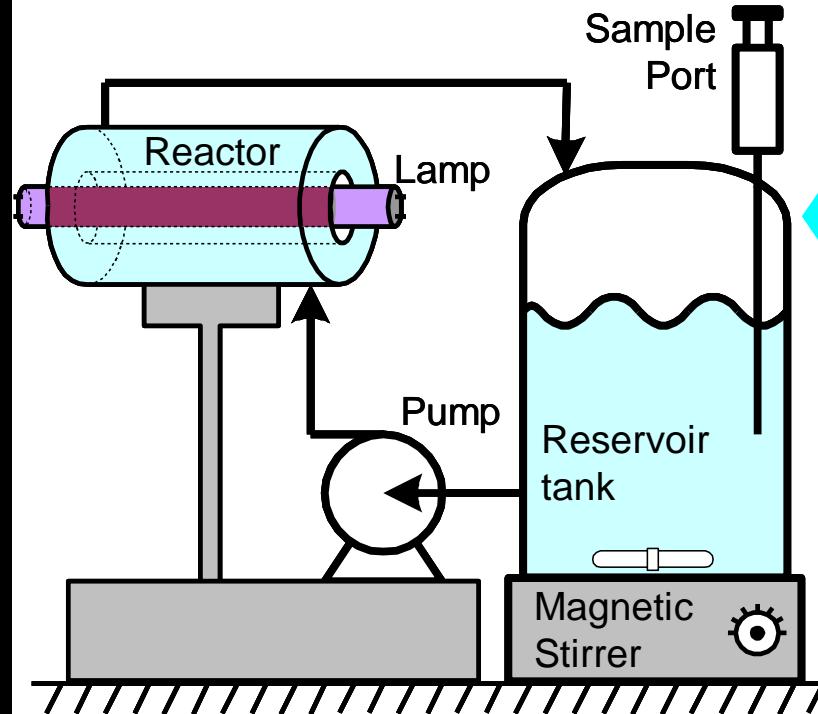
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Lamp: Philips TL 6W
 $L = 21 \text{ cm}, \Phi = 1.6 \text{ cm}$



Lamp + Neutral Filters

Actinometry

$$\sim 40 \text{ W / m}^2$$



Serial Dilutions + Plating



Catalyst: **0.02 – 0.2 g/L TiO₂ Degussa P25**

Radiation: **0.8 – 2.7 × 10⁻⁶ Einstein / s**

Microorg.: **10³ – 10⁶ CFU/mL *E.coli***

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Lab Scale: Photoreactor: Mass Balance

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Methodology.

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Lab Scale.

- Photoreactor
- **Mass Balance.**
- Kinetic Model.
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ASSUMPTIONS:

1. The system is perfectly mixed.
2. No mass transport limitations.
3. Differential conversion per pass.
4. No parallel dark reactions.

$$\left. \frac{d[B](t)}{dt} \right|_{\text{Tank}} = \frac{V_{\text{React}}}{V_{\text{Tot}}} \langle R_B(x,t) \rangle_{V_{\text{React}}}$$

- | | | |
|---|---|---|
| [B] | : | Bacterial concentration |
| <i>t</i> | : | Time |
| <i>V_{React}</i> / <i>V_{Tot}</i> | : | Reactor volume / Total volume |
| $\langle R_B(x,t) \rangle_{V_{\text{React}}}$ | : | Bacterial reaction rate averaged over the reactor volume |

Kinetic Model: Lab Scale Experimental Data

OUTLINE

Introduction.

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Methodology.

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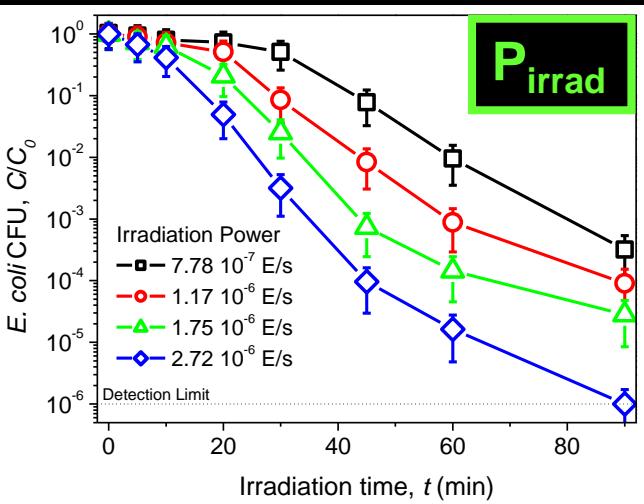
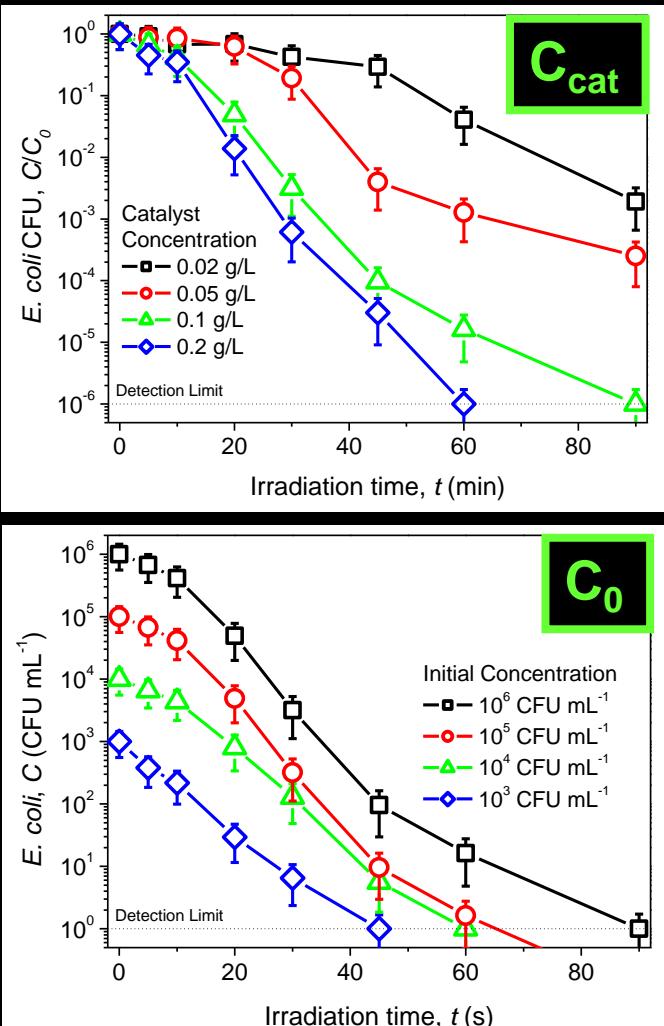
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Kinetics Parameters for
Reactor Design & Scaling-Up

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Kinetic Model: Empiric Equations

OUTLINE

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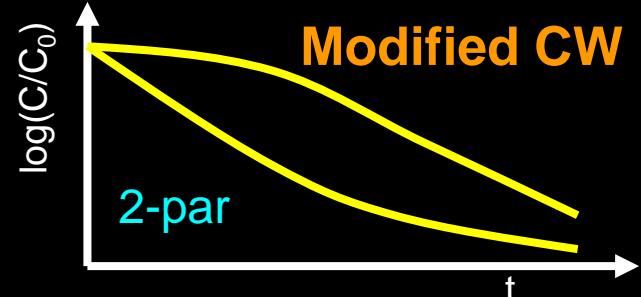
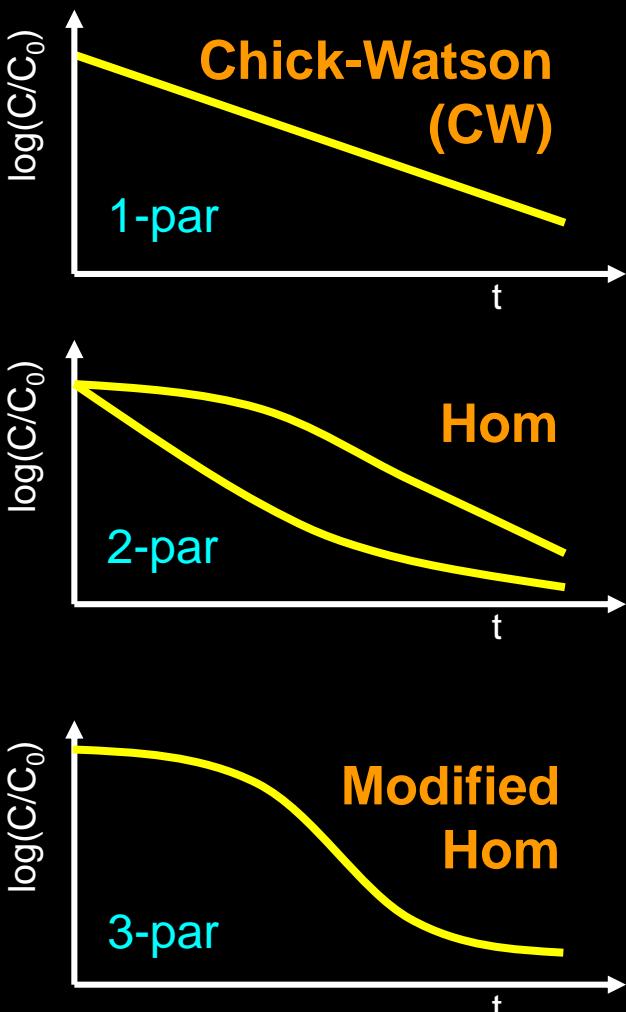
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Kinetic Model: Empiric Equations

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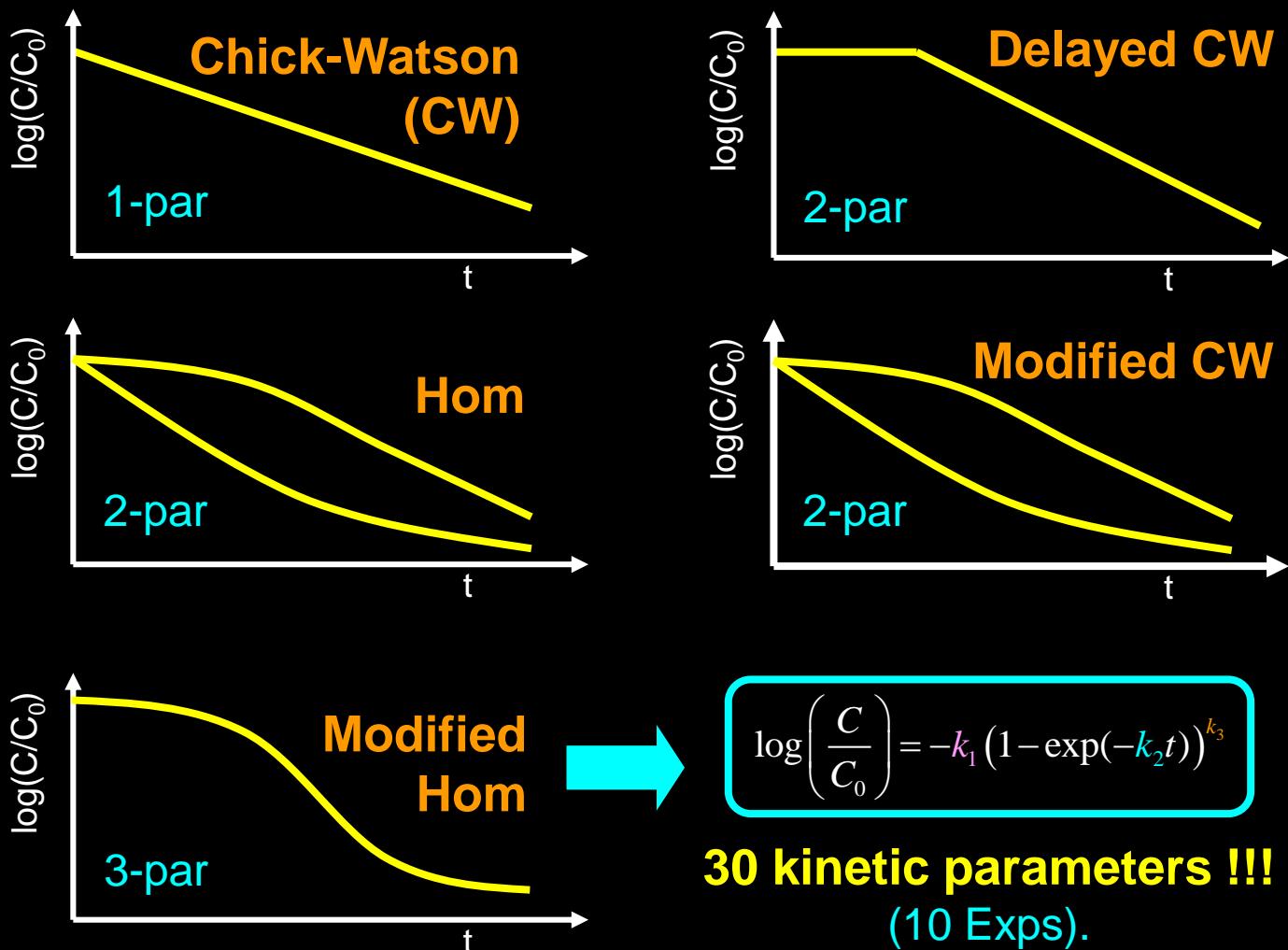
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Kinetic Model: Series Event Mechanism

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Methodology.

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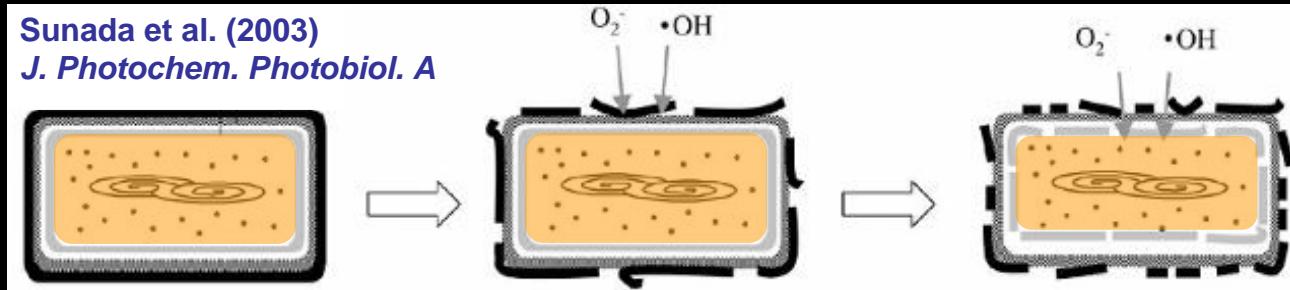
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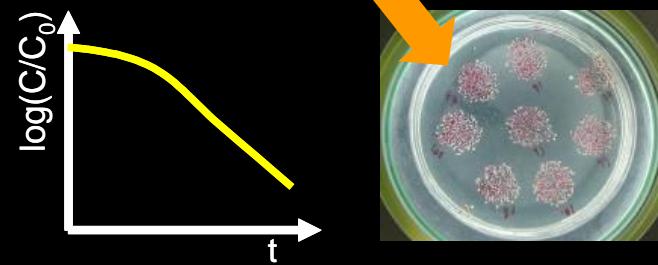
Sunada et al. (2003)
J. Photochem. Photobiol. A



Severin et al. (1983)
Water Res.



$$\log \frac{C}{C_0} = -kt + \ln \left(1 + \sum_{i=1}^n \frac{(kt)^i}{i!} \right)$$



Kinetic Model: Series Event Mechanism

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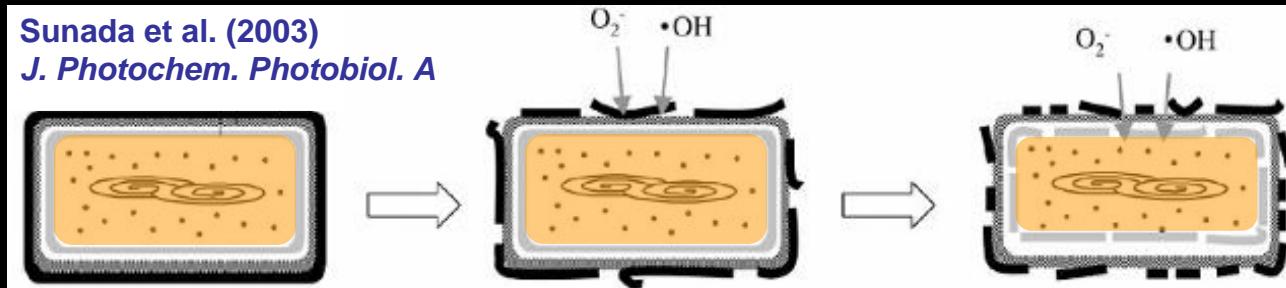
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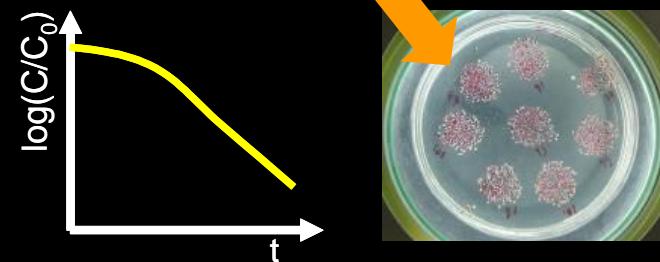
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$$\log \frac{C}{C_0} = -kt + \ln \left(1 + \sum_{i=1}^n \frac{(kt)^i}{i!} \right)$$



Photonic efficiency: ~ 10^{-11} bacteria / photon

$10^9 \cdot \text{OH} / \text{bacteria} !!!$

Marugán et al. (2008)
Appl. Catal. B: Environ

Kinetic Model: Pseudo-Mechanistic

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Introduction.

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Methodology.

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Marugán et al. (2008)
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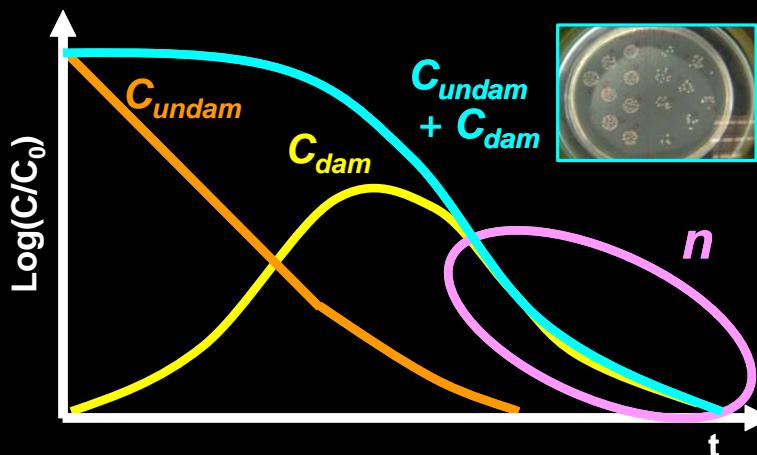
$$\frac{dC_{undam}}{dt} = -k \frac{K C_{undam}^n}{1 + K C_{undam}^n + K C_{dam}^n}$$

$$\frac{dC_{dam}}{dt} = k \frac{K C_{undam}^n - K C_{dam}^n}{1 + K C_{undam}^n + K C_{dam}^n}$$

k: Kinetic constant

K: Pseudo-adsorption constant

n: Inhibition coefficient



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Kinetic Model: Pseudo-Mechanistic

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Methodology.

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Lab Scale.

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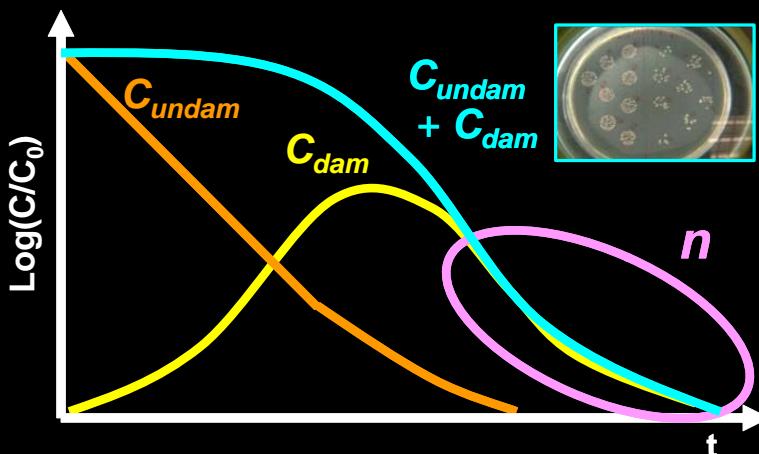
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$$\frac{dC_{undam}}{dt} = -k \frac{K C_{undam}^n}{1 + K C_{undam}^n + K C_{dam}^n}$$

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k: Kinetic constant

K: Pseudo-adsorption constant

n: Inhibition coefficient

K, n: Constant

k = f (**C_{cat}** , **P_{irrad}**)

Radiation Absorption

9 kinetic parameters
(10 Exps.).

Intrinsic Kinetic Model: Proposed Mechanism

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STEP	REACTION	RATE
Activation	$\text{TiO}_2 \xrightarrow{h\nu} \text{TiO}_2 + e^- + h^+$	r_g
Recombination	$e^- + h^+ \rightarrow \text{heat}$	$v_i k_2 [e^-][h^+]$
Electron trapping	$e^- + O_2 \rightarrow \cdot O_2^-$	$v_i k_3 [e^-][O_2]$
Hole trapping	$h^+ + H_2O \rightarrow \cdot OH + H^+$	$v_i k_4 [h^+][H_2O]$
Hydroxyl attack	$B_u + \cdot OH \rightarrow B_d$	$v_i k_5 [\cdot OH]^\ell [B_u]$
	$B_d + \cdot OH \rightarrow B_i$	$v_i k_6 [\cdot OH]^\ell [B_d]$
	$B_i + \cdot OH \rightarrow B_{p1} + B_{p2} + \dots B_{pi} \dots + B_{pn}$	$v_i k_7 [\cdot OH]^\ell [B_i]$
	$B_{p1} + \cdot OH \rightarrow \text{Products}$	$v_i k_{81} [\cdot OH]^\ell [B_{p1}]$
	$B_{p2} + \cdot OH \rightarrow \text{Products}$	$v_i k_{82} [\cdot OH]^\ell [B_{p2}]$

	$B_{pi} + \cdot OH \rightarrow \text{Products}$	$v_i k_{8i} [\cdot OH]^\ell [B_{pi}]$

	$B_{pn} + \cdot OH \rightarrow \text{Products}$	$v_i k_{8n} [\cdot OH]^\ell [B_{pn}]$
Adsorption	$\text{cell site} + \text{TiO}_{2,\text{bulk}} \leftrightarrow \text{TiO}_{2,\text{ads}}$	K_{ads}

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Intrinsic Kinetic Model: General Equation

OUTLINE

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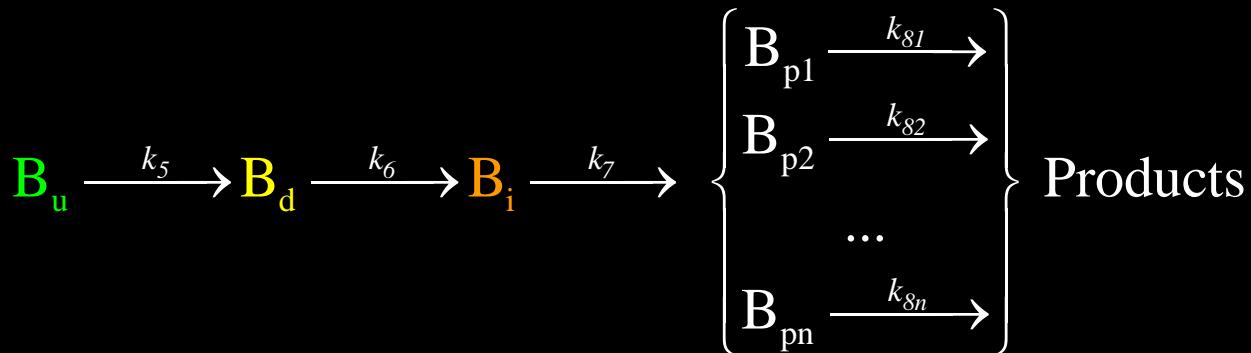
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Conclusions.



$$R_u \left(\frac{\text{CFU}}{\text{s cm}^3} \right) = -\alpha_1 \left(\frac{K_{ads} C_{cat}}{1 + K_{ads} C_{cat}} \right) \frac{[B_u]^2}{[B_u] + \alpha_4 [B_d] + \alpha_3 ([B]_0 - [B_u] - [B_d])} \left[-1 + \sqrt{1 + \frac{\alpha_2 e^a}{S_g C_{cat}}} \right]$$

$$R_d \left(\frac{\text{CFU}}{\text{s cm}^3} \right) = \alpha_1 \left(\frac{K_{ads} C_{cat}}{1 + K_{ads} C_{cat}} \right) \frac{[B_u]^2 - \alpha_4 [B_d]^2}{[B_u] + \alpha_4 [B_d] + \alpha_3 ([B]_0 - [B_u] - [B_d])} \left[-1 + \sqrt{1 + \frac{\alpha_2 e^a}{S_g C_{cat}}} \right]$$

5 kinetic parameters
 $\neq f(N^o \text{ Exps.})$

$\alpha_1, \alpha_2, \alpha_3, \alpha_4, K_{ads}$

$R = f(C_{cat}, e^a, [B]_0)$



$e^a = f(C_{cat}, P_{irrad}, \text{geometry})$

Intrinsic Kinetic Model: Limiting Cases

OUTLINE

Introduction.

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Methodology.

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$$K_{ads} C_{cat} \gg 1$$

$$\cancel{K_{ads}}$$

4 kinetic parameters

$$\alpha_1, \alpha_2, \alpha_3, \alpha_4$$

Meaningless simulation results for C_{cat} effect

$$K_{ads} C_{cat} \rightarrow 0$$

$$\alpha = \alpha_1 K_{ads}$$

4 kinetic parameters

$$\alpha, \alpha_2, \alpha_3, \alpha_4$$

Intrinsic Kinetic Model: Limiting Cases

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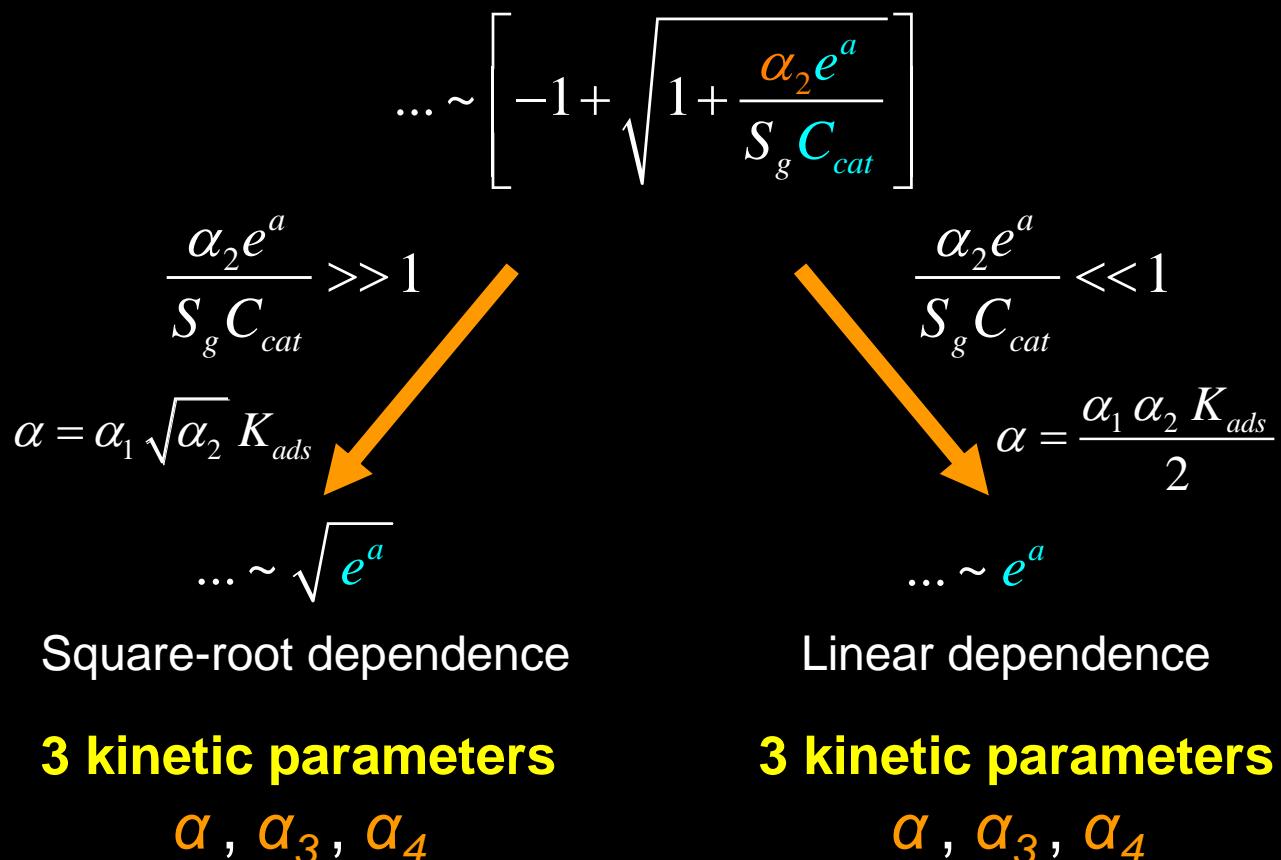
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Conclusions.



Lab Scale Photoreactor: Radiation Model

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Introduction.

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Methodology.

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Lab Scale.

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Conclusions.

$$\frac{dI_{\lambda,\Omega}}{ds} = - \underbrace{\kappa_\lambda \cdot I_{\lambda,\Omega}}_{\text{ABSORPTION}} - \underbrace{\sigma_\lambda \cdot I_{\lambda,\Omega}}_{\text{OUT-SCATTERING}} + \underbrace{\frac{\sigma_\lambda}{4\pi} \int_{\Omega'=4\pi} p \cdot I_{\lambda,\Omega'} d\Omega'}_{\text{IN-SCATTERING}}$$

Lab Scale Photoreactor: Radiation Model

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Lab Scale.

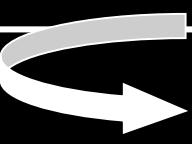
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RTE Solution  $I_{\lambda,\Omega}$

INTENSITY OF RADIATION
Monochromatic, Directional

Lab Scale Photoreactor: Radiation Model

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Conclusions.

$$\frac{dI_{\lambda,\Omega}}{ds} = - \underbrace{\kappa_\lambda \cdot I_{\lambda,\Omega}}_{\text{ABSORPTION}} - \underbrace{\sigma_\lambda \cdot I_{\lambda,\Omega}}_{\text{OUT-SCATTERING}} + \underbrace{\frac{\sigma_\lambda}{4\pi} \int_{\Omega'=4\pi} p \cdot I_{\lambda,\Omega'} d\Omega'}_{\text{IN-SCATTERING}}$$

RTE Solution

$I_{\lambda,\Omega}$

Integration on the
spherical space of directions



$$G_\lambda = \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega$$

INTENSITY OF RADIATION
Monochromatic, Directional

**INCIDENT
RADIATION**

Lab Scale Photoreactor: Radiation Model

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

Lab Scale.

- Photoreactor
- Mass Balance.
- Kinetic Model.
- **Radiation Model.**
- Kinetic Parameters Estimation.

Bench Scale.

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RTE Solution

$$I_{\lambda,\Omega}$$

Integration on the
spherical space of directions



$$G_\lambda = \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega$$

INTENSITY OF RADIATION
Monochromatic, Directional

**INCIDENT
RADIATION**

$$e_\lambda^a = \kappa_\lambda \cdot G_\lambda$$

**MONOCHROMATIC
RADIATION ABSORPTION**

Lab Scale Photoreactor: Radiation Model

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

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- Scaling-Up Validation.

Conclusions.

$$\frac{dI_{\lambda,\Omega}}{ds} = - \underbrace{\kappa_\lambda \cdot I_{\lambda,\Omega}}_{\text{ABSORPTION}} - \underbrace{\sigma_\lambda \cdot I_{\lambda,\Omega}}_{\text{OUT-SCATTERING}} + \underbrace{\frac{\sigma_\lambda}{4\pi} \int_{\Omega'=4\pi} p \cdot I_{\lambda,\Omega'} d\Omega'}_{\text{IN-SCATTERING}}$$

RTE Solution

$$I_{\lambda,\Omega}$$

Integration on the
spherical space of directions

$$G_\lambda = \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega$$

INTENSITY OF RADIATION
Monochromatic, Directional

**INCIDENT
RADIATION**

$$e_\lambda^a = \kappa_\lambda \cdot G_\lambda$$

**MONOCHROMATIC
RADIATION ABSORPTION**

Integration on wavelength

$$\text{LVRPA} = e^a = \int_{\lambda_1}^{\lambda_2} e_\lambda^a d\lambda$$

**LOCAL VOLUMETRIC
RATE OF PHOTON
ABSORPTION**

RTE Resolution

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

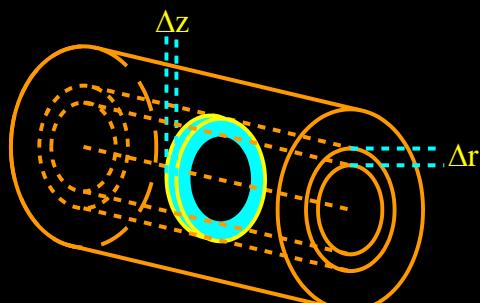
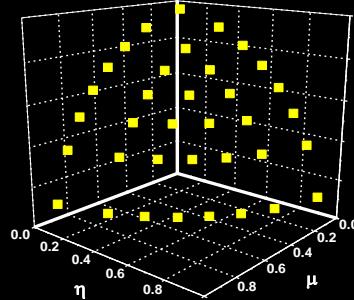
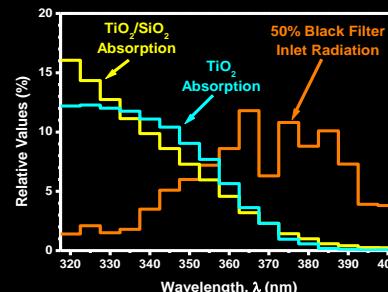
Lab Scale.

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- Kinetic Model.
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Bench Scale.

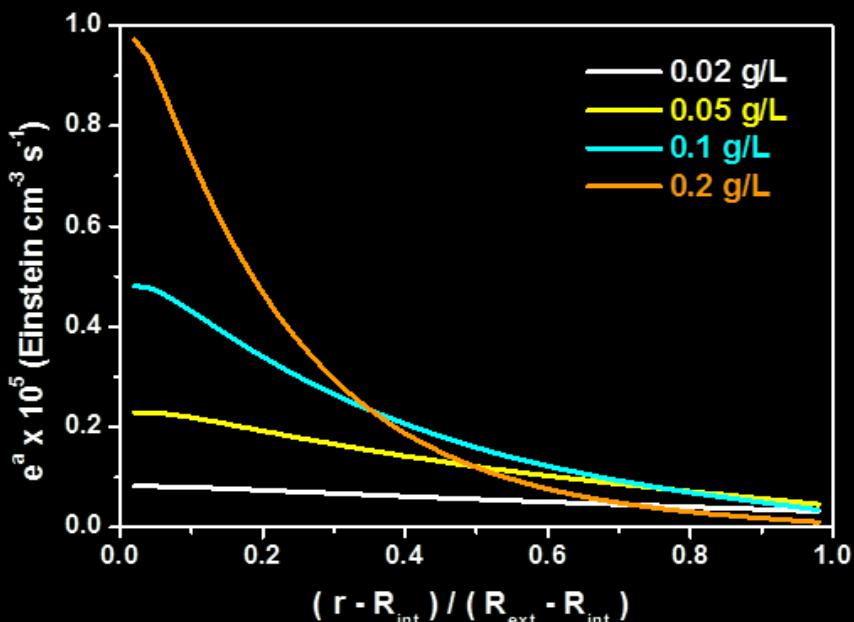
- Photoreactor
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Conclusions.



$$\frac{dI_{\lambda,\Omega}}{ds} = -\kappa_\lambda \cdot I_{\lambda,\Omega} - \sigma_\lambda \cdot I_{\lambda,\Omega} + \frac{\sigma_\lambda}{4\pi} \int_{\Omega'=4\pi} p \cdot I_{\lambda,\Omega'} d\Omega'$$

$I_{\lambda}(r, z, \Omega) \rightarrow e^a(C_{cat}, P_{irrad})$



Simulation and Design of Photoreactors

Javier Marugán

AOPs School, Porto, 11th July 2017



Universidad
Rey Juan Carlos

Kinetic Parameters Estimation

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

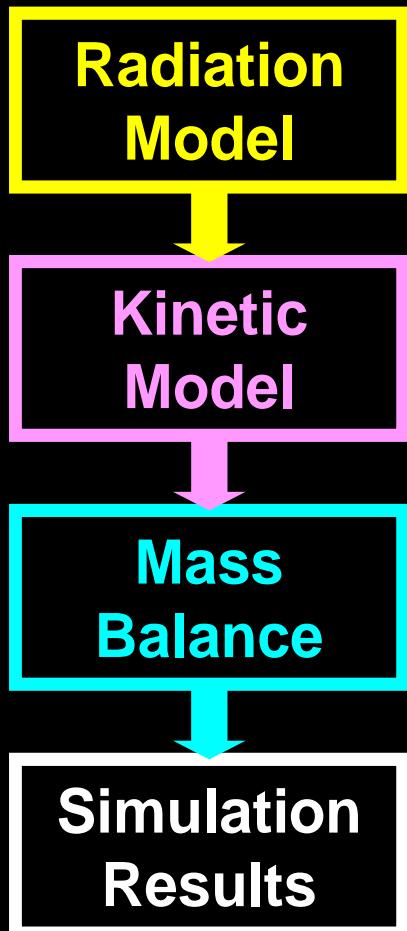
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Bench Scale.

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- Radiation Model.
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- Mass Balance.
- Scaling-Up Validation.

Conclusions.



RTE

$$I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$$

$$LVRPA = e^a = \int_{\lambda_1}^{\lambda_2} K_\lambda \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$

Kinetic Parameters Estimation

OUTLINE

Introduction.

- The Problem.

Methodology.

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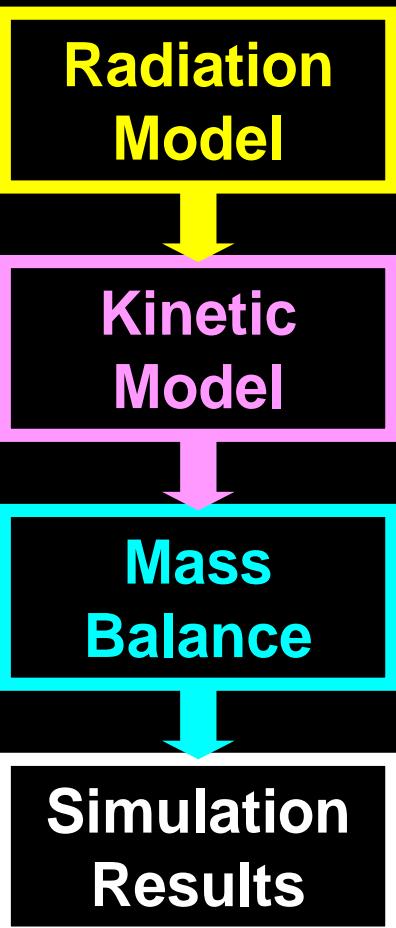
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Conclusions.



RTE $\longrightarrow I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$

$$LVRPA = e^a = \int_{\lambda_1}^{\lambda_2} \kappa_\lambda \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$
$$R_u, R_d = f(\alpha_1, \alpha_2, \alpha_3, \alpha_4, K_{ads}, C_{cat}, e^a, [B]_0)$$

Kinetic Parameters Estimation

OUTLINE

Introduction.

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- Proposed Scaling-Up Procedure.

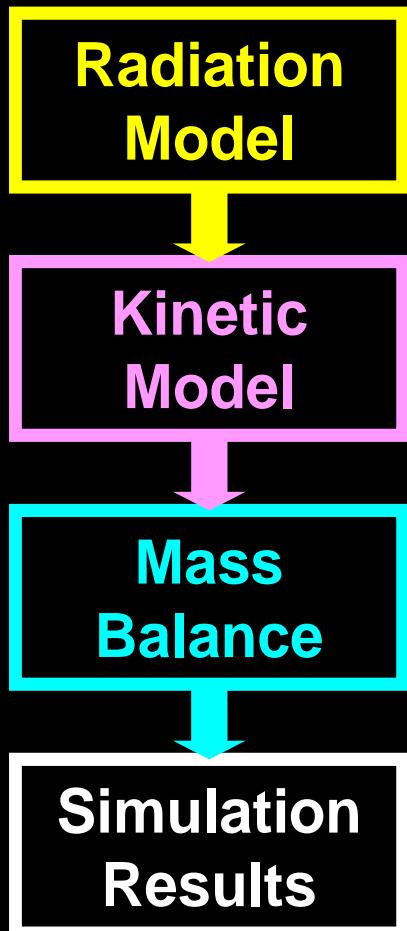
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$$RTE \longrightarrow I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$$

$$LVRPA = e^a = \int_{\lambda_1}^{\lambda_2} \kappa_{\lambda} \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$

$$R_u, R_d = f(\alpha_1, \alpha_2, \alpha_3, \alpha_4, K_{ads}, C_{cat}, e^a, [B]_0)$$

$$\frac{d[B_u](t)}{dt} \Big| = \frac{V_{React}}{V_{Tot}} \langle R_u(x,t) \rangle_{V_{React}}$$

$$\frac{d[B_d](t)}{dt} \Big| = \frac{V_{React}}{V_{Tot}} \langle R_d(x,t) \rangle_{V_{React}}$$

Kinetic Parameters Estimation

OUTLINE

Introduction.

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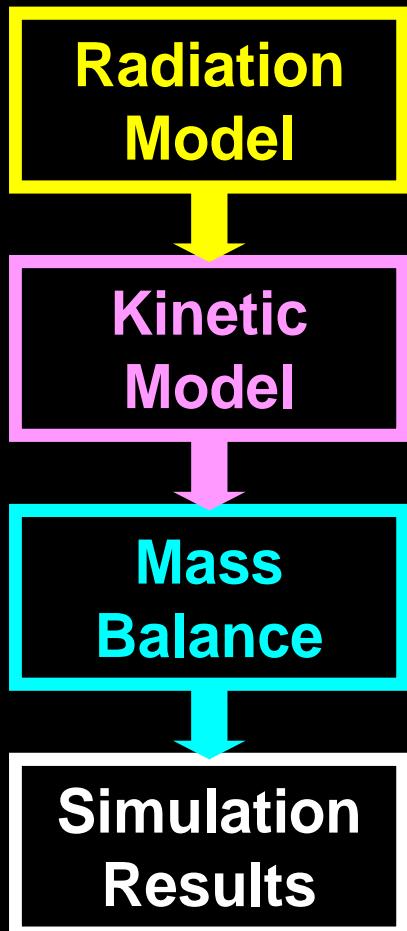
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Conclusions.



$$\text{RTE} \longrightarrow I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$$
$$\text{LVRPA} = e^a = \int_{\lambda_1}^{\lambda_2} \kappa_{\lambda} \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$
$$R_u, R_d = f(\alpha_1, \alpha_2, \alpha_3, \alpha_4, K_{ads}, C_{cat}, e^a, [B]_0)$$
$$\frac{d[B_u](t)}{dt} \Big| = \frac{V_{React}}{V_{Tot}} \langle R_u(x,t) \rangle_{V_{React}}$$
$$\frac{d[B_d](t)}{dt} \Big| = \frac{V_{React}}{V_{Tot}} \langle R_d(x,t) \rangle_{V_{React}}$$
$$[B_u + B_d](t)$$

Kinetic Parameters Estimation

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

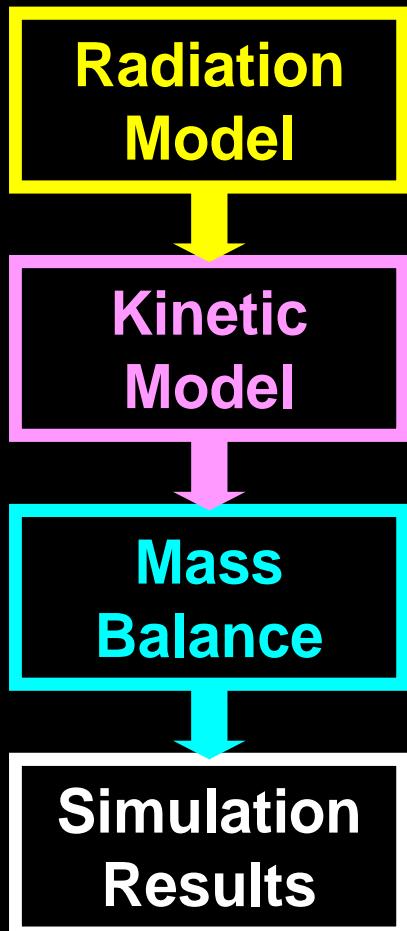
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Conclusions.



$$RTE \longrightarrow I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$$

$$LVRPA = e^a = \int_{\lambda_1}^{\lambda_2} \kappa_{\lambda} \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$

$$R_u, R_d = f(\alpha_1, \alpha_2, \alpha_3, \alpha_4, K_{ads}, C_{cat}, e^a, [B]_0)$$

$$\frac{d[B_u](t)}{dt} \Big| = \frac{V_{React}}{V_{Tot}} \langle R_u(x,t) \rangle_{V_{React}}$$

$$\frac{d[B_d](t)}{dt} \Big| = \frac{V_{React}}{V_{Tot}} \langle R_d(x,t) \rangle_{V_{React}}$$

$$[B_u + B_d](t)$$

vs Experimental

Simulation Results: 5-Par Model

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

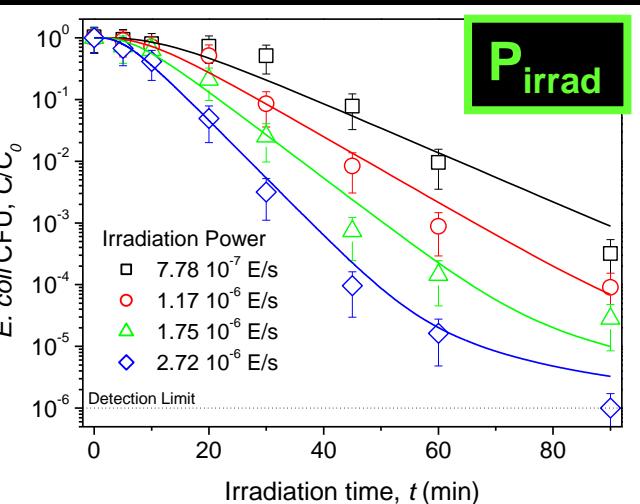
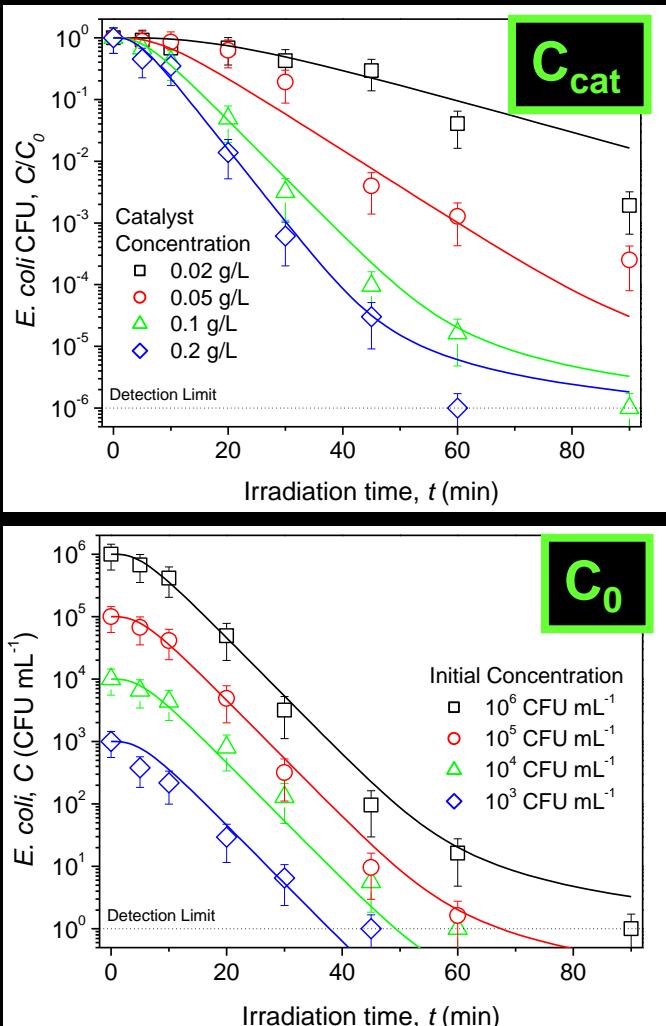
Lab Scale.

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- Mass Balance.
- Kinetic Model.
- Radiation Model.
- Kinetic Parameters Estimation.

Bench Scale.

- Photoreactor
- Radiation Model.
- Kinetic Model.
- Mass Balance.
- Scaling-Up Validation.

Conclusions.



$$\alpha_1 = 1.64 \times 10^2 \text{ s}^{-1}$$

$$\alpha_2 = 1.13 \times 10^{11} \text{ cm}^2 \cdot \text{s} \cdot \text{E}^{-1}$$

$$\alpha_3 = 3.11 \times 10^{-6}$$

$$\alpha_4 = 1.00 \times 10^{-1}$$

$$K_{ads} = 1.00 \text{ cm}^3 \cdot \text{g}^{-1}$$

$$SSLE = 6.64$$

Simulation Results: 4-Par Model

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

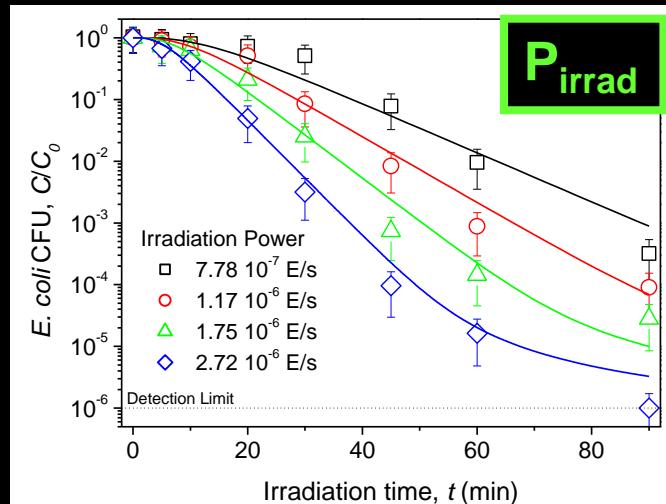
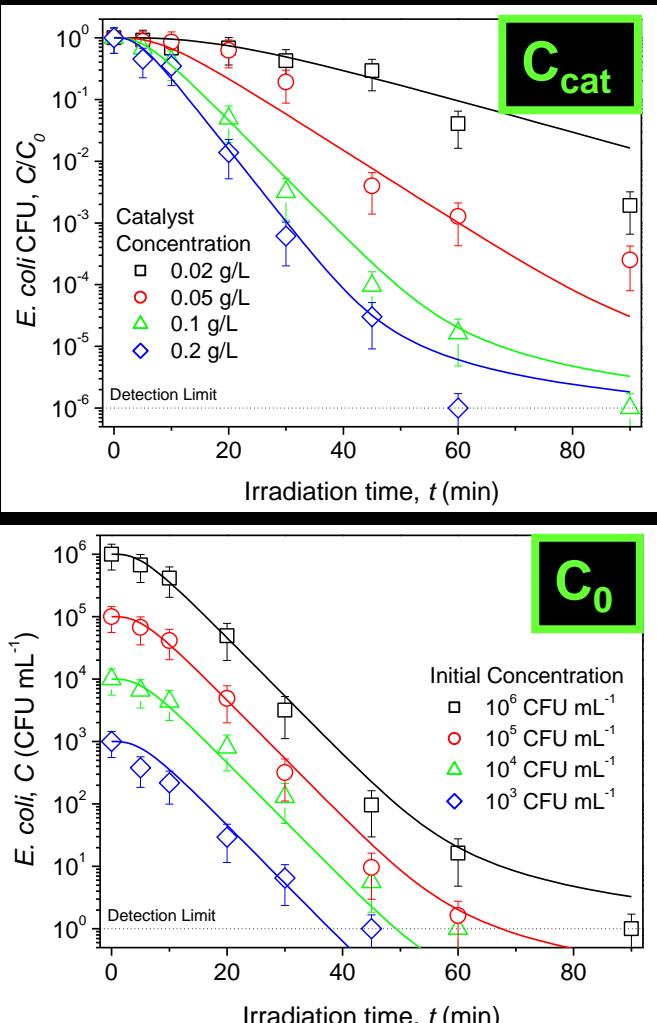
Lab Scale.

- Photoreactor
- Mass Balance.
- Kinetic Model.
- Radiation Model.
- Kinetic Parameters Estimation.

Bench Scale.

- Photoreactor
- Radiation Model.
- Kinetic Model.
- Mass Balance.
- Scaling-Up Validation.

Conclusions.



$$K_{ads} C_{cat} \rightarrow 0 \quad \alpha = \alpha_1 K_{ads}$$

$$\alpha = 1.64 \times 10^2 \text{ cm}^3 \cdot \text{s}^{-1} \cdot \text{g}^{-1}$$

$$\alpha_2 = 1.13 \times 10^{11} \text{ cm}^2 \cdot \text{s} \cdot \text{E}^{-1}$$

$$\alpha_3 = 3.37 \times 10^{-6}$$

$$\alpha_4 = 1.07 \times 10^{-1}$$

$$\text{SSLE} = 6.64$$

Simulation Results: 3-Par Model $\sim e^{a_0 t^{0.5}}$

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

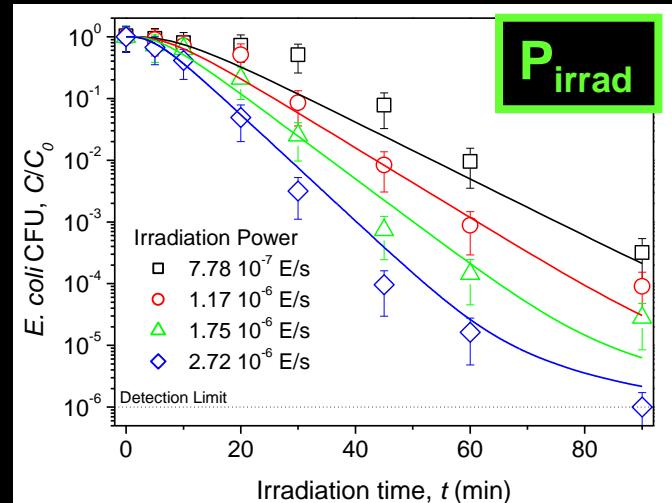
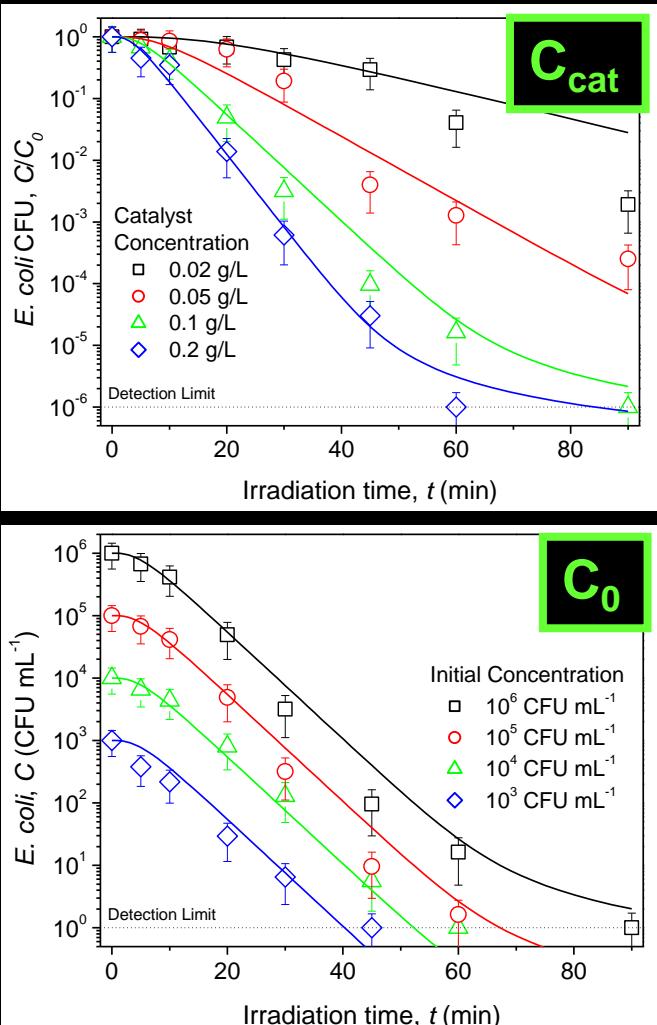
Lab Scale.

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- Mass Balance.
- Kinetic Model.
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Bench Scale.

- Photoreactor
- Radiation Model.
- Kinetic Model.
- Mass Balance.
- Scaling-Up Validation.

Conclusions.



$$\alpha = 3.86 \times 10^7 \text{ cm}^4 \cdot \text{g}^{-1} \cdot \text{s}^{-0.5} \cdot \text{E}^{-0.5}$$

$$\alpha_3 = 2.06 \times 10^{-6}$$

$$\alpha_4 = 1.67 \times 10^{-1}$$

SSLE = 7.12

Simulation Results: 3-Par Model $\sim e^a$

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

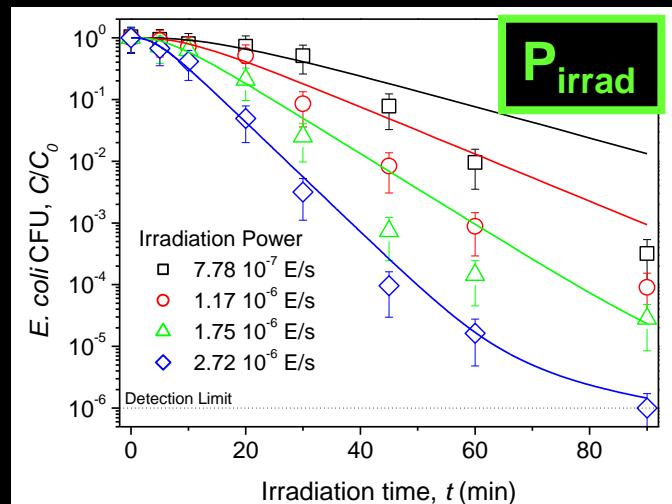
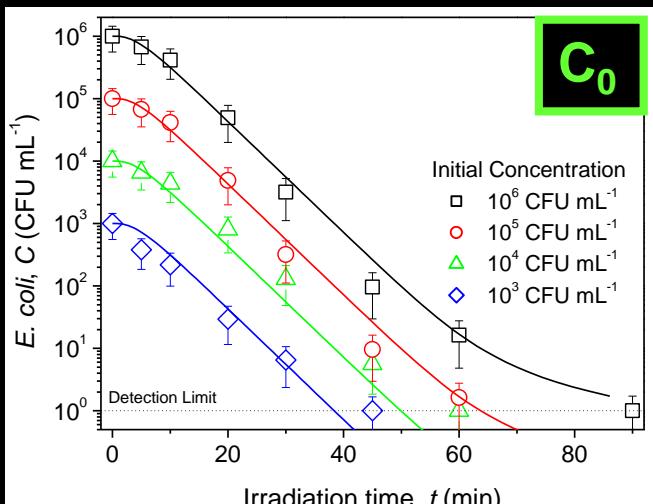
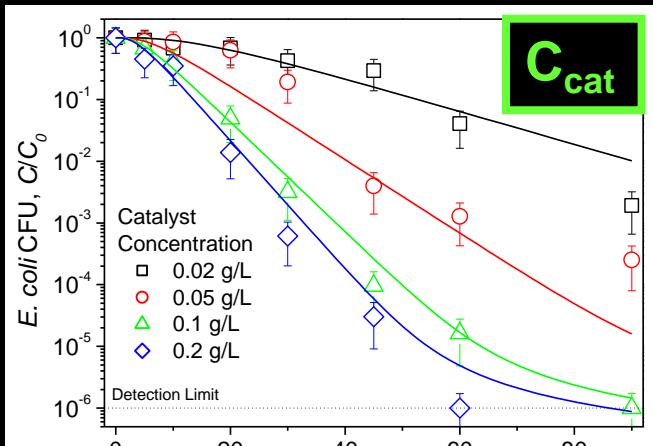
Lab Scale.

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Bench Scale.

- Photoreactor
- Radiation Model.
- Kinetic Model.
- Mass Balance.
- Scaling-Up Validation.

Conclusions.



$$\dots \sim e^a \quad \alpha = \frac{\alpha_1 \alpha_2 K_{ads}}{2}$$

$$\alpha = 3.66 \times 10^{12} \text{ cm}^5 \cdot \text{g}^{-1} \cdot \text{E}^{-1}$$

$$\alpha_3 = 2.00 \times 10^{-6}$$

$$\alpha_4 = 2.18 \times 10^{-1}$$

SSLE = 14.28

Bench Scale Photoreactor

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

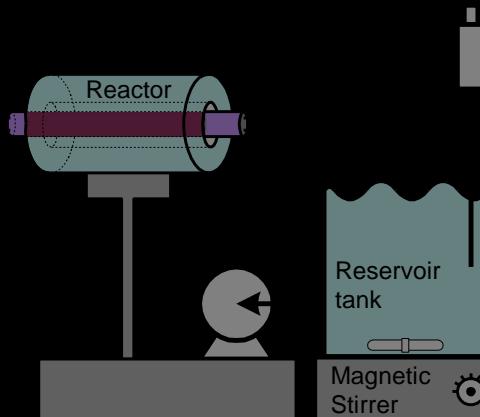
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- Scaling-Up Validation.

Conclusions.



Laboratory scale reactor:

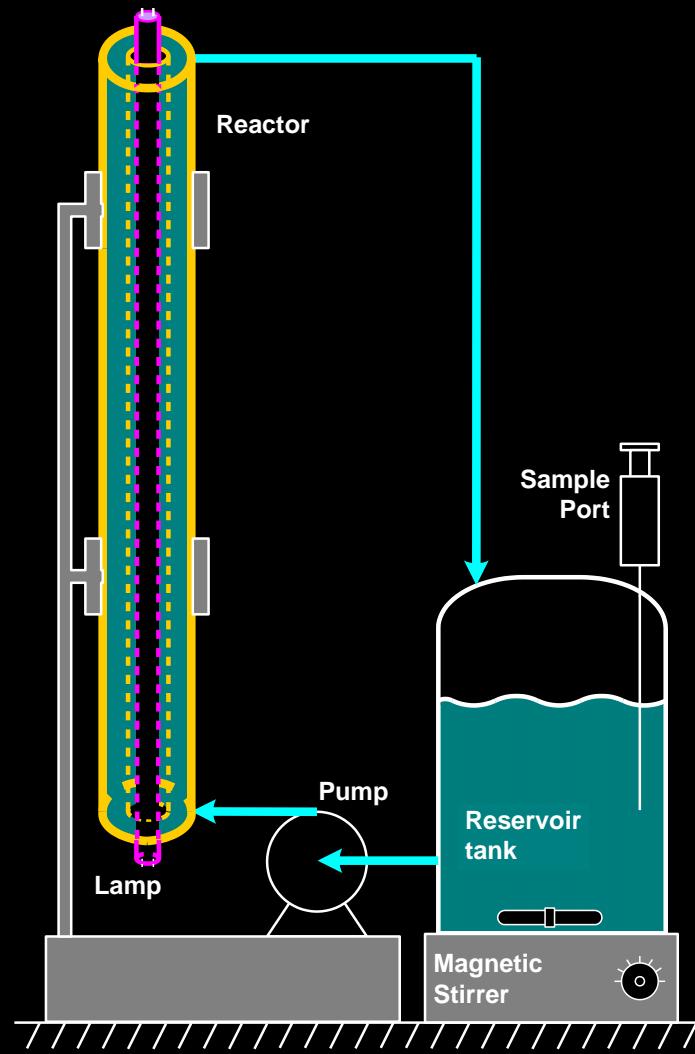
$$V_R = 188.5 \text{ cm}^3, V_{\text{Tot}} = 1 \text{ L}$$

Lamp: Philips TL 6W
 $L = 21 \text{ cm}, \Phi = 1.6 \text{ cm}$

Bench scale reactor:

$$V_R = 1250 \text{ cm}^3, V_{\text{Tot}} = 5 \text{ L}$$

Lamp: Osram L 36W
 $L = 120 \text{ cm}, \Phi = 2.6 \text{ cm}$



Simulation and Design of Photoreactors

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Bench Scale Photoreactor

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

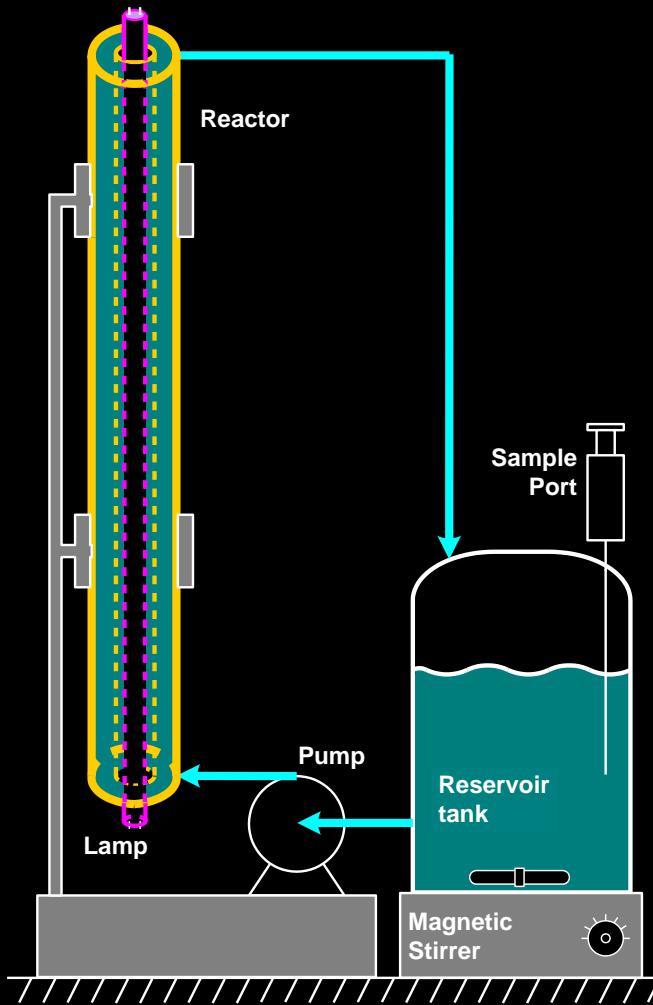
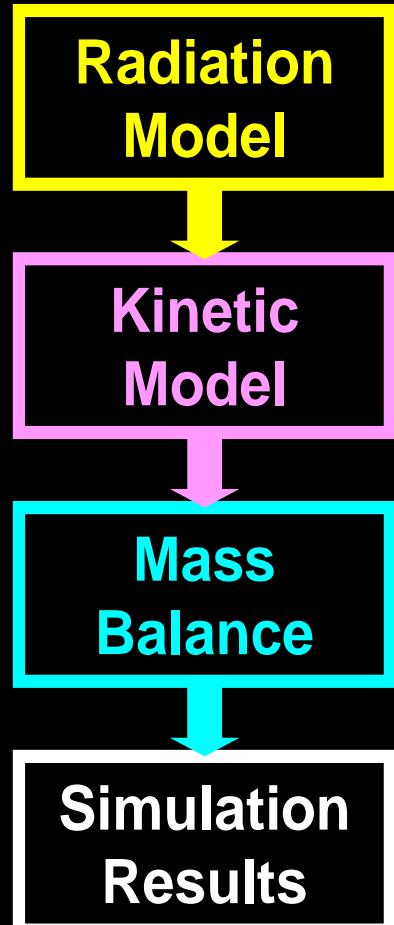
Lab Scale.

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Bench Scale.

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- Mass Balance.
- Scaling-Up Validation.

Conclusions.



Bench Scale Photoreactor: Mass Balance

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

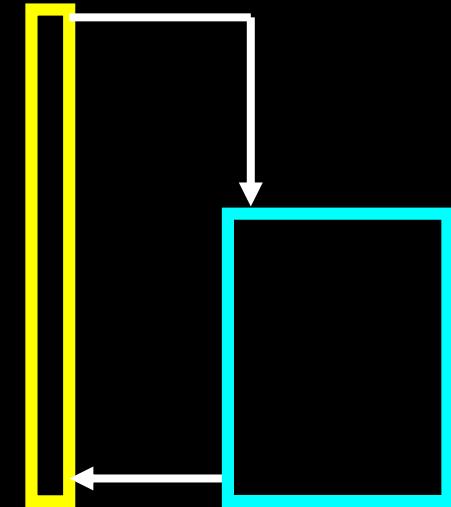
Lab Scale.

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Bench Scale.

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- Mass Balance.**
- Scaling-Up Validation.

Conclusions.



$$\left. \frac{d[B](t)}{dt} \right|_{\text{Tank}} = \frac{1}{\tau_{\text{Tank}}} ([B]^{\text{inlet}}(t) - [B](t))$$

$$[B](0) = [B]^0$$

Bench Scale Photoreactor: Mass Balance

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

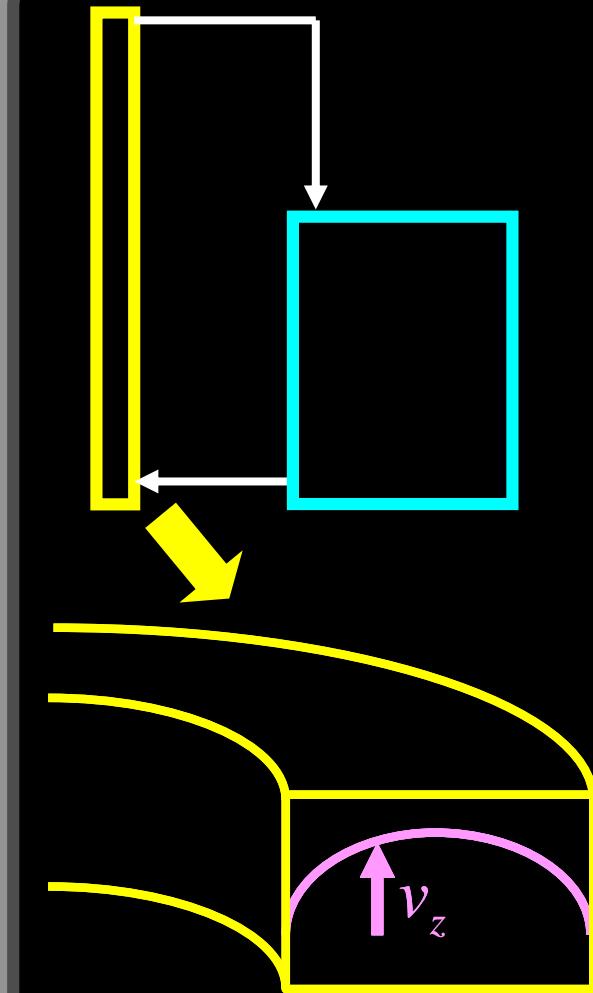
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Bench Scale.

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- Kinetic Model.
- Mass Balance.**
- Scaling-Up Validation.

Conclusions.



$$\frac{d[B](t)}{dt} \Big|_{\text{Tank}} = \frac{1}{\tau_{\text{Tank}}} ([B]^{\text{inlet}}(t) - [B](t))$$

$$[B](0) = [B]^0$$

$$v_z \frac{\partial [B]}{\partial z} = D_{B-Water}^0 \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial [B]}{\partial r} \right) \right) + R_B$$

$$[B](z=0, r) = [B](t)$$

$$\frac{\partial [B](z, r_{int})}{\partial r} = \frac{\partial [B](z, r_{ext})}{\partial r} = 0$$

Bench Scale Photoreactor: Simulation

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

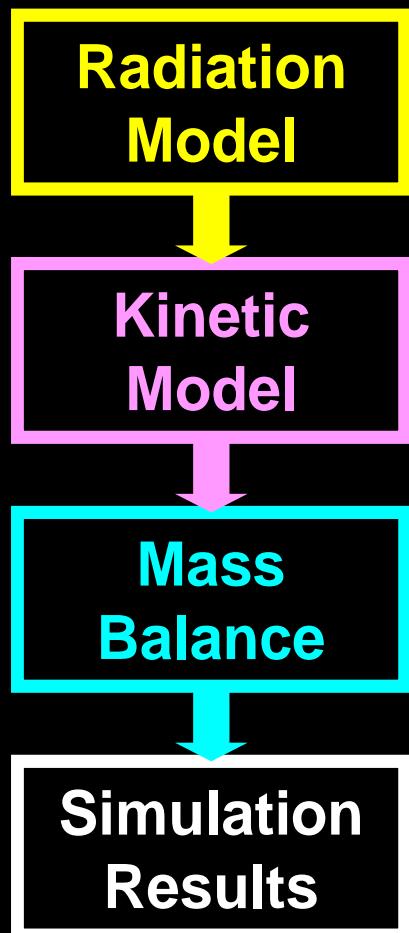
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- Scaling-Up Validation.

Conclusions.



RTE

$$I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$$

$$LVRPA = e^a = \int_{\lambda_1}^{\lambda_2} K_\lambda \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$

Bench Scale Photoreactor: Simulation

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

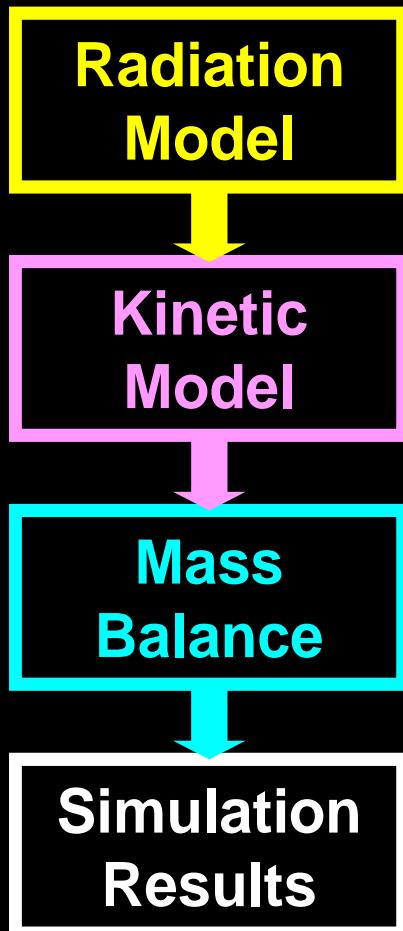
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Conclusions.



$$\text{RTE} \rightarrow I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$$
$$\text{LVRPA} = e^a = \int_{\lambda_1}^{\lambda_2} K_\lambda \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$
$$R_u, R_d = f(\alpha_1, \alpha_2, \alpha_3, \alpha_4, K_{ads}, C_{cat}, e^a, [B]_0)$$

Bench Scale Photoreactor: Simulation

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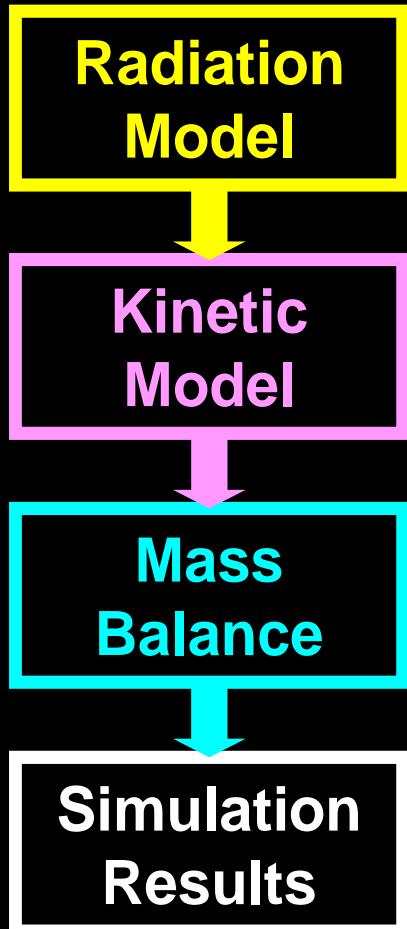
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$$\text{RTE} \rightarrow I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$$
$$\text{LVRPA} = e^a = \int_{\lambda_1}^{\lambda_2} K_\lambda \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$
$$R_u, R_d = f(\alpha_1, \alpha_2, \alpha_3, \alpha_4, K_{ads}, C_{cat}, e^a, [B]_0)$$
$$v_z \frac{d[B]}{dz} = D_{B-Water}^0 \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial [B]}{\partial r} \right) \right) + R_B$$
$$\left. \frac{d[B](t)}{dt} \right|_{Tank} = \frac{1}{\tau_{Tank}} ([B]^{inlet}(t) - [B](t))$$

Bench Scale Photoreactor: Simulation

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

Lab Scale.

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Bench Scale.

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- Radiation Model.
- Kinetic Model.
- Mass Balance.
- Scaling-Up Validation.

Conclusions.

Radiation Model

$$RTE \rightarrow I_{\lambda,\Omega} = f(C_{cat}, P_{irrad}, geometry)$$

$$LVRPA = e^a = \int_{\lambda_1}^{\lambda_2} K_{\lambda} \int_{\Omega=4\pi} I_{\lambda,\Omega} d\Omega d\lambda$$

$$R_u, R_d = f(\alpha_1, \alpha_2, \alpha_3, \alpha_4, K_{ads}, C_{cat}, e^a, [B]_0)$$

$$\nu_z \frac{d[B]}{dz} = D_{B-Water}^0 \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial [B]}{\partial r} \right) \right) + R_B$$

$$\frac{d[B](t)}{dt}_{Tank} = \frac{1}{\tau_{Tank}} ([B]^{inlet}(t) - [B](t))$$

[B](t)

Simulated Results

Bench Scale Photoreactor: Simulation

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

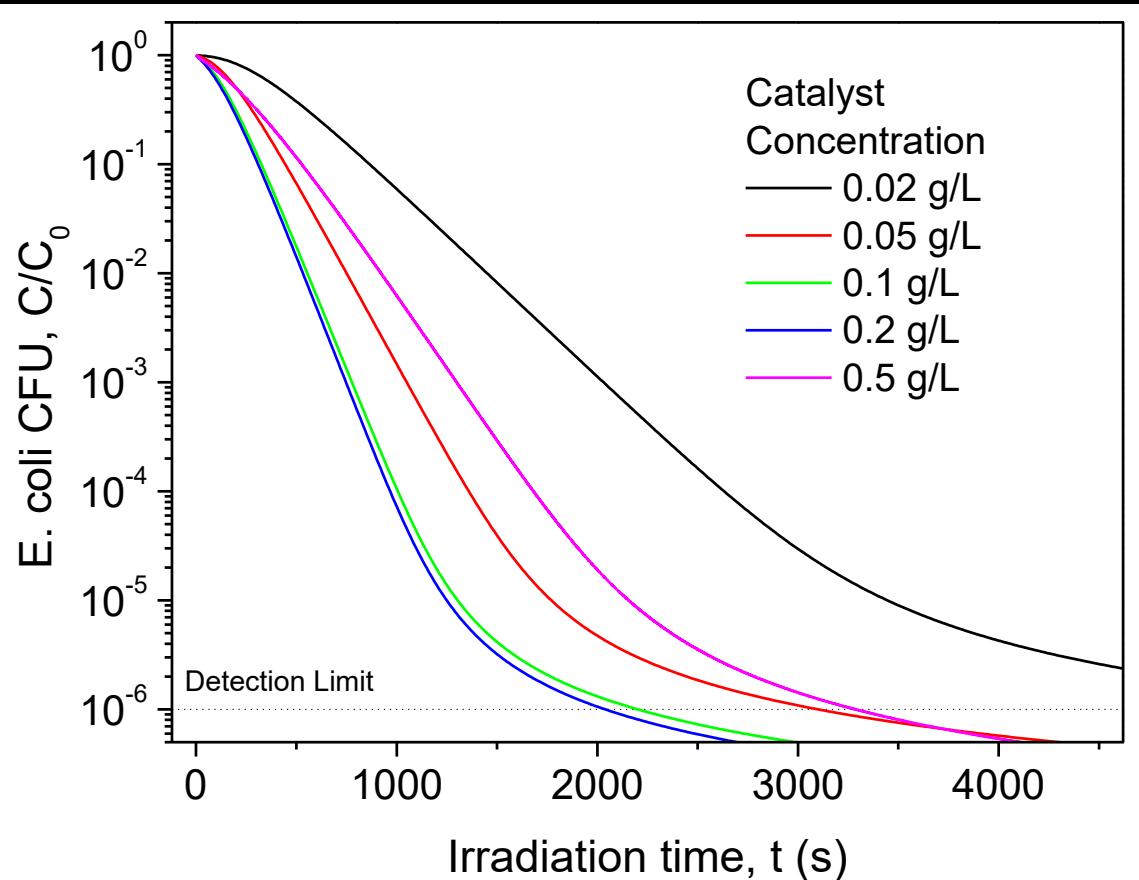
Lab Scale.

- Photoreactor
- Mass Balance.
- Kinetic Model.
- Radiation Model.
- Kinetic Parameters Estimation.

Bench Scale.

- Photoreactor
- Radiation Model.
- Kinetic Model.
- Mass Balance.
- Scaling-Up Validation.

Conclusions.



**Maximum Activity 0.1-0.2 g/L TiO₂
Significant decrease in activity for 0.5 g/L TiO₂**

Bench Scale Photoreactor: VALIDATION

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

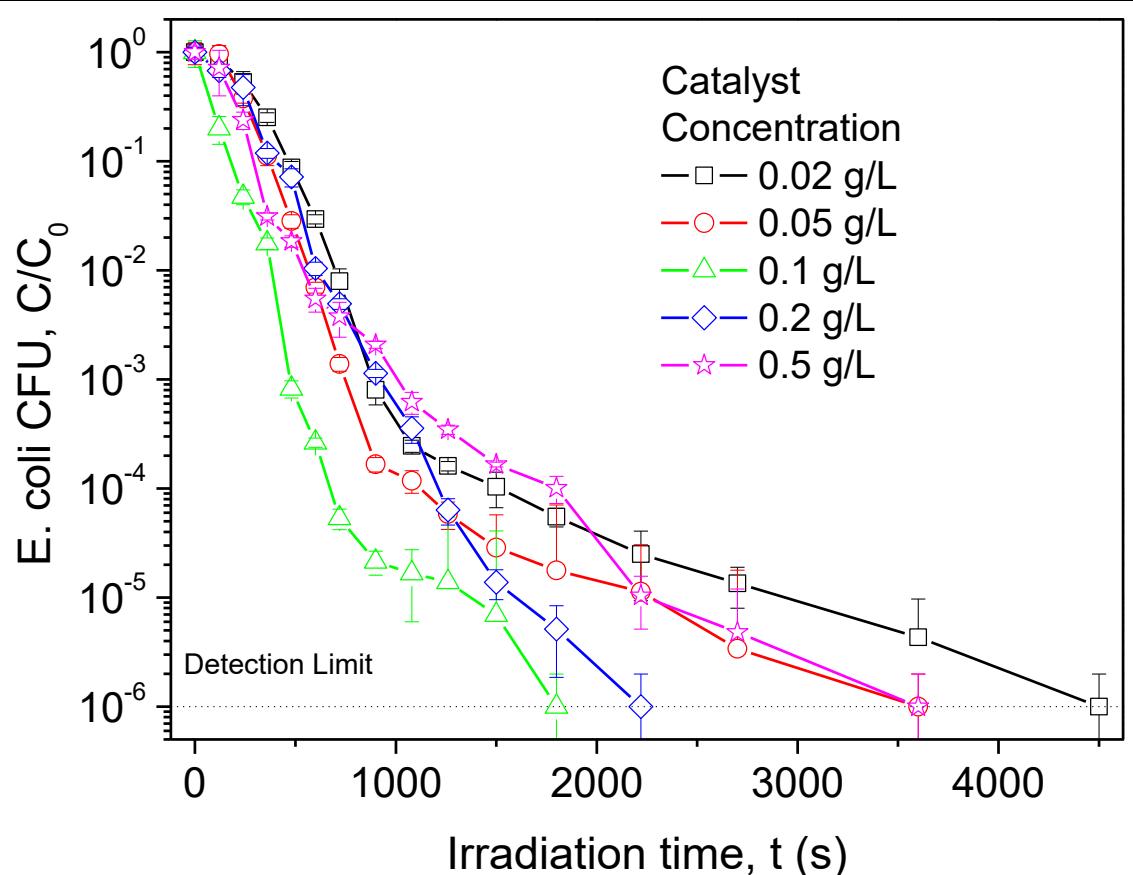
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Conclusions.



Maximum Activity 0.1 g/L TiO₂
Significant decrease in activity for 0.5 g/L TiO₂

Bench Scale Photoreactor: **VALIDATION**

OUTLINE

Introduction.

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Methodology.

- Proposed Scaling-Up Procedure.

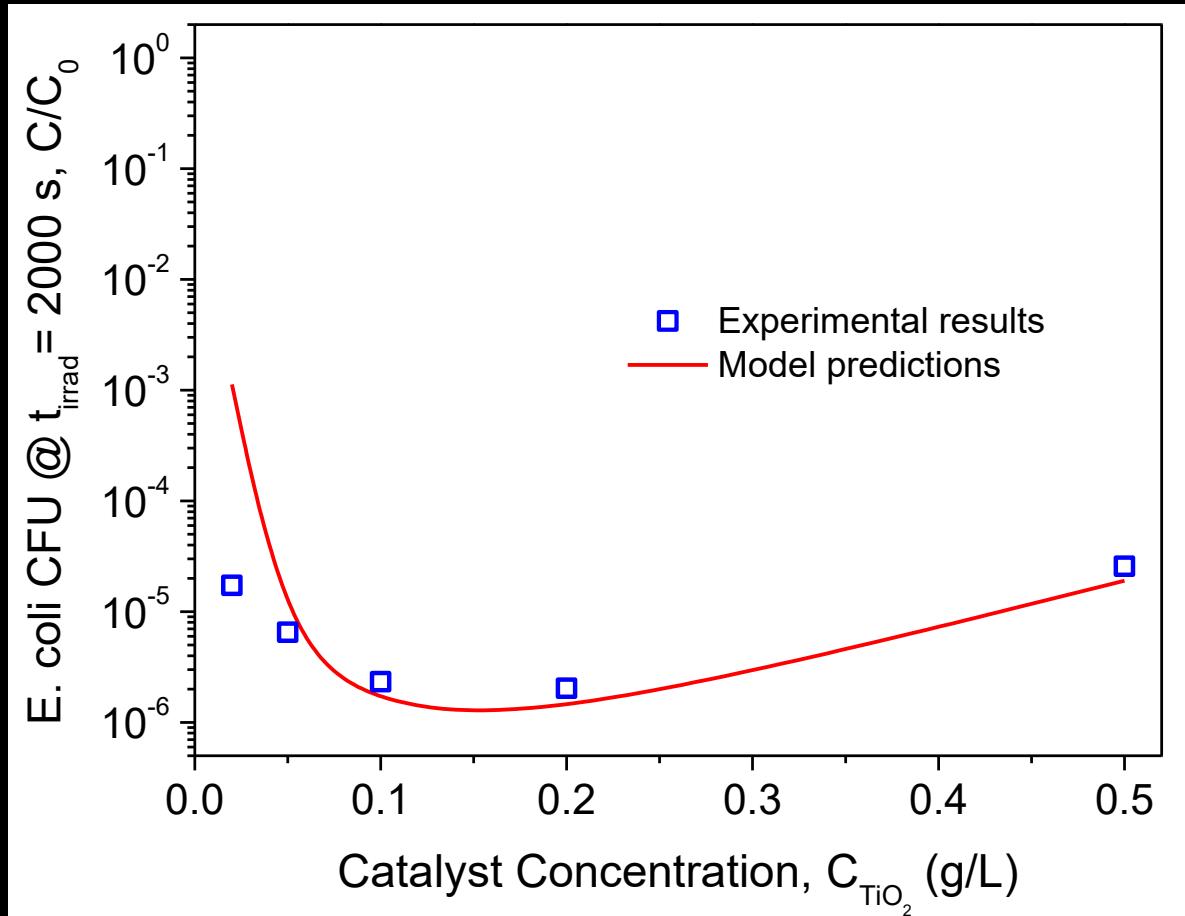
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- Mass Balance.
- **Scaling-Up Validation.**

Conclusions.



Perfil de Concentración (0.5 g/L)

OUTLINE

Introduction.

- The Problem.

Methodology.

- Proposed Scaling-Up Procedure.

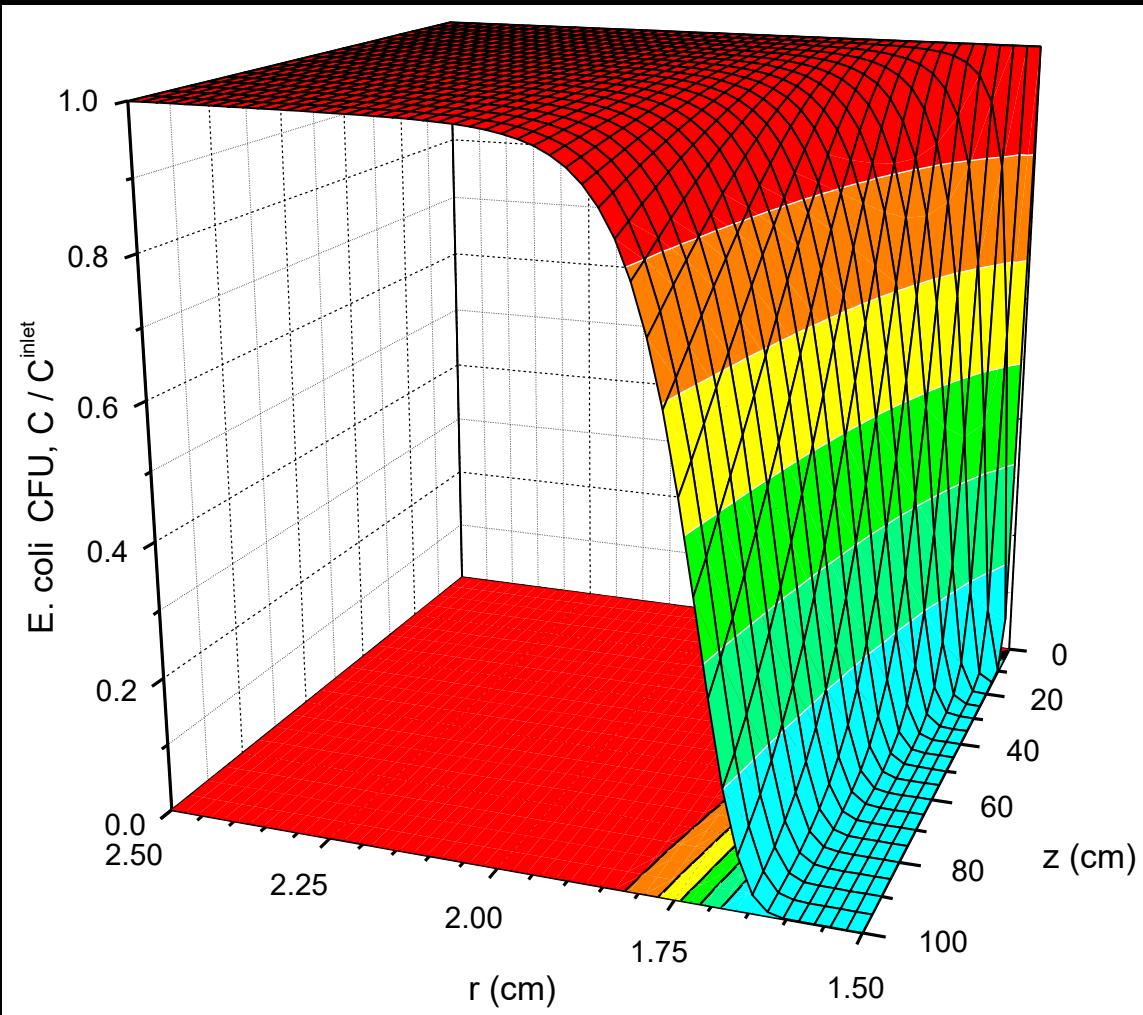
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Conclusions.



Optimum $[TiO_2]$: Bacteria vs Molecules

OUTLINE

Introduction.

- The Problem.

Methodology.

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Bench Scale.

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- Radiation Model.
- Kinetic Model.
- Mass Balance.
- Scaling-Up Validation.

Conclusions.

$$D_{CN^-}^0 = 1.25 \times 10^{-5} \text{ cm}^2 \text{s}^{-1}$$

Sun et al. (1996)
Metall. Mater. Trans.

$$D_{Ecoli}^0 = 9.2 \times 10^{-7} \text{ cm}^2 \text{s}^{-1}$$

Ford & Harvey. (2007)
Adv. Water Res.

Aqueous TiO_2 suspension

Bacterial concentration profiles

Bacterial diffusion

Radiation absorption profile and reaction rate



$\downarrow C_{cat}$

$\uparrow C_{cat}$

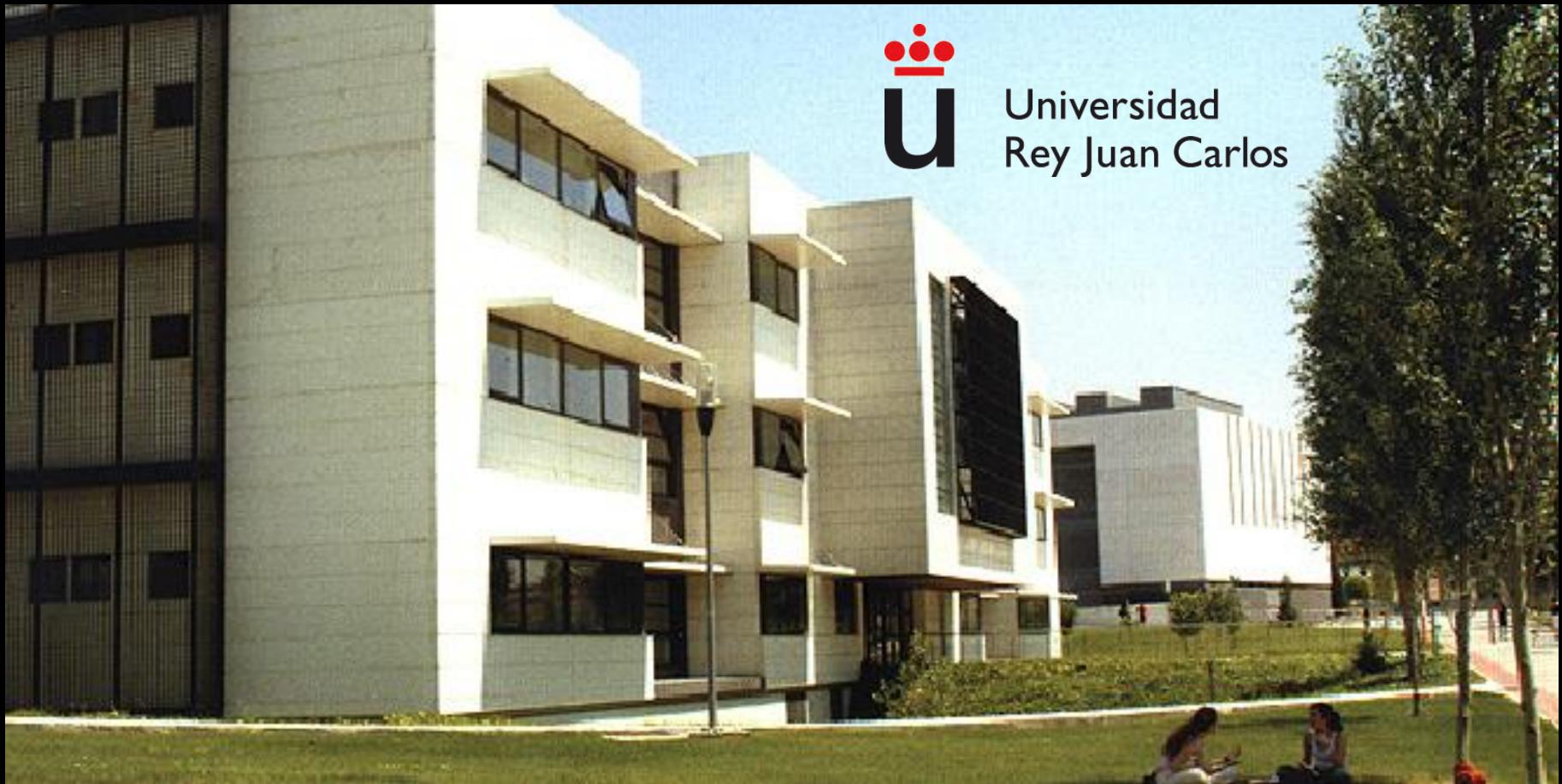
$\uparrow C_{cat}$

$\downarrow C_{cat}$

Conclusions

- The performance of large scale photocatalytic reactor has been simulated following an absolutely predictive procedure based on the intrinsic kinetics and the information about the geometry, irradiation source and operation conditions.
- The only experimental information required to be determined at laboratory scale is the intrinsic kinetics that describes the explicit dependence of the reaction rate with the LVRPA.
- The proposed method for the scaling-up of slurry reactors for the photocatalytic inactivation of *E. coli* with TiO₂ in suspension has been successfully validated in a ten times higher irradiated volume reactor, including the predicted optimum concentration of catalyst predicted by the model.

Thanks for your attention!



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SIMULATION AND DESIGN OF PHOTOREACTORS

Javier Marugán



Universidad
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AOPs PhD School

**Summer School 2017
Porto, 11th July 2017**